

Complex Metal Oxides as Heterogeneous Catalysts

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Scope and Acknowledgements



Function of catalysts and structure-function correlations as basis for rational design efforts.

Full analysis of structural complexity by in-situ observation with complementary techniques.

Thanks to the group leaders:

M. Behrens, (R. Horn), A. Knop-Gericke, J. Tornow, A. Trunschke, M. Willinger

Taylor model

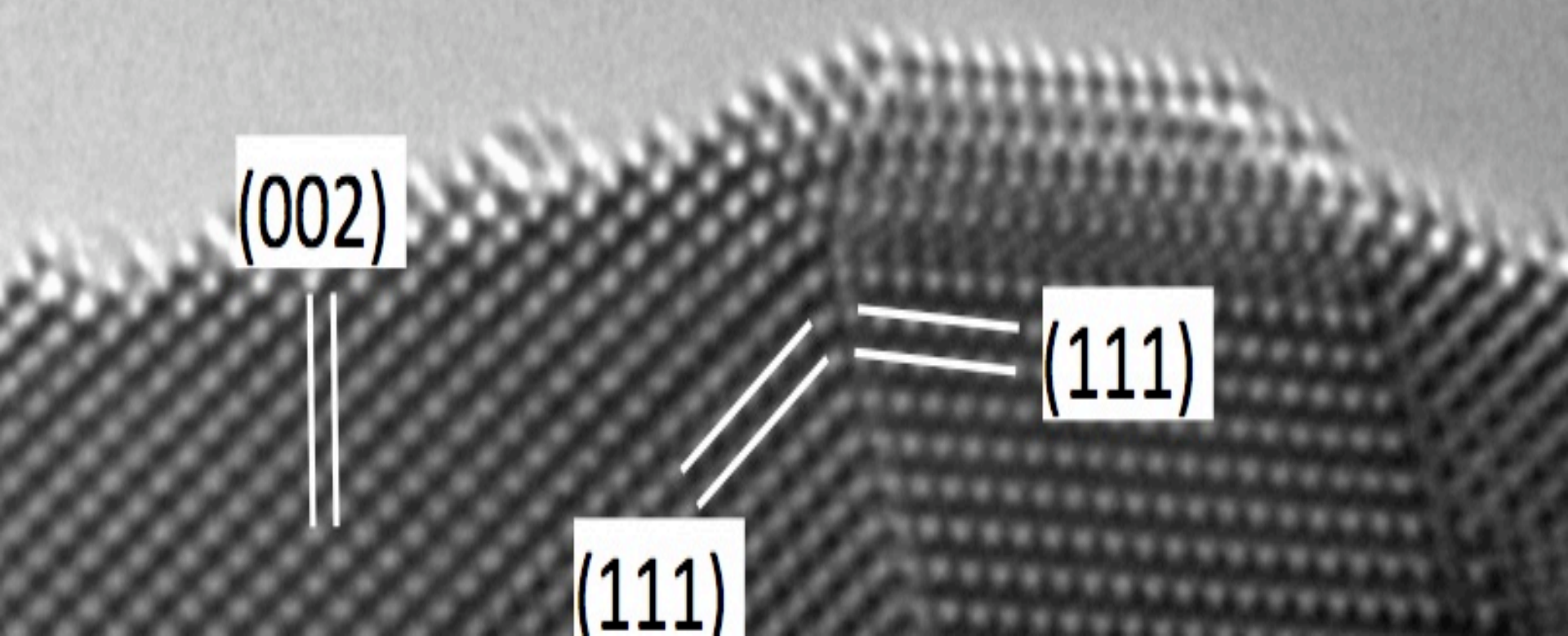
The ordinary general, inorganic, and organic chemistry of substances is concerned with the reactions and properties of many million millions of examples of such atoms or molecules, and the result given is a statistical average covering all the cases. The properties of the contact agent, especially in catalytic reactions difficultly achieved, are those of the aristocracy of the atomic or molecular species concerned, and are as different from the statistical average behavior of the crowd as the actions of an educated minority of people should be different from that of an indiscriminately collected mob.

J. Phys. Chem, Vol 30, (1926)



Taylor model

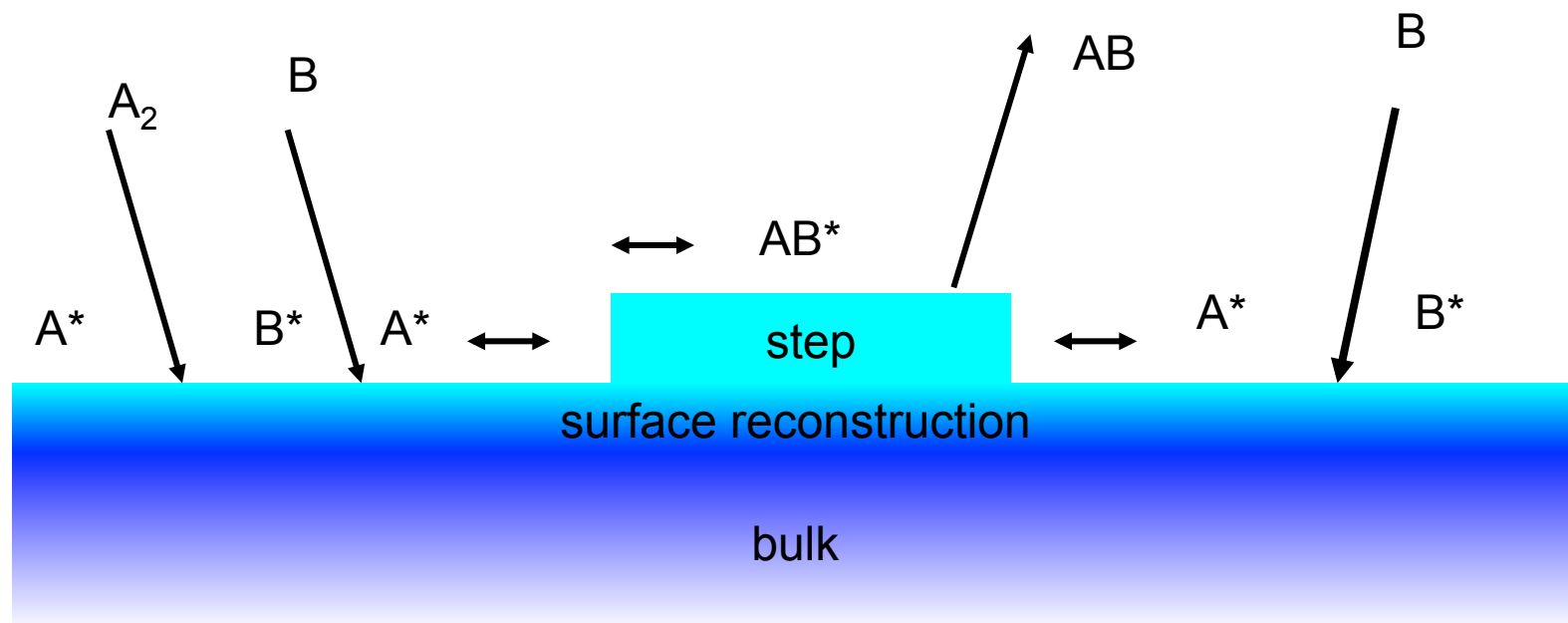
2 nm



Standard model of heterogeneous catalysis

deep understanding, limited function

system is close to equilibrium
theory finds minimal energy configurations



Adsorbate structures dynamical (chemical waves)
Bulk is "irrelevant", no chemical transformations sub-surface

Works well for adsorbate-controlled reactions (are only few)

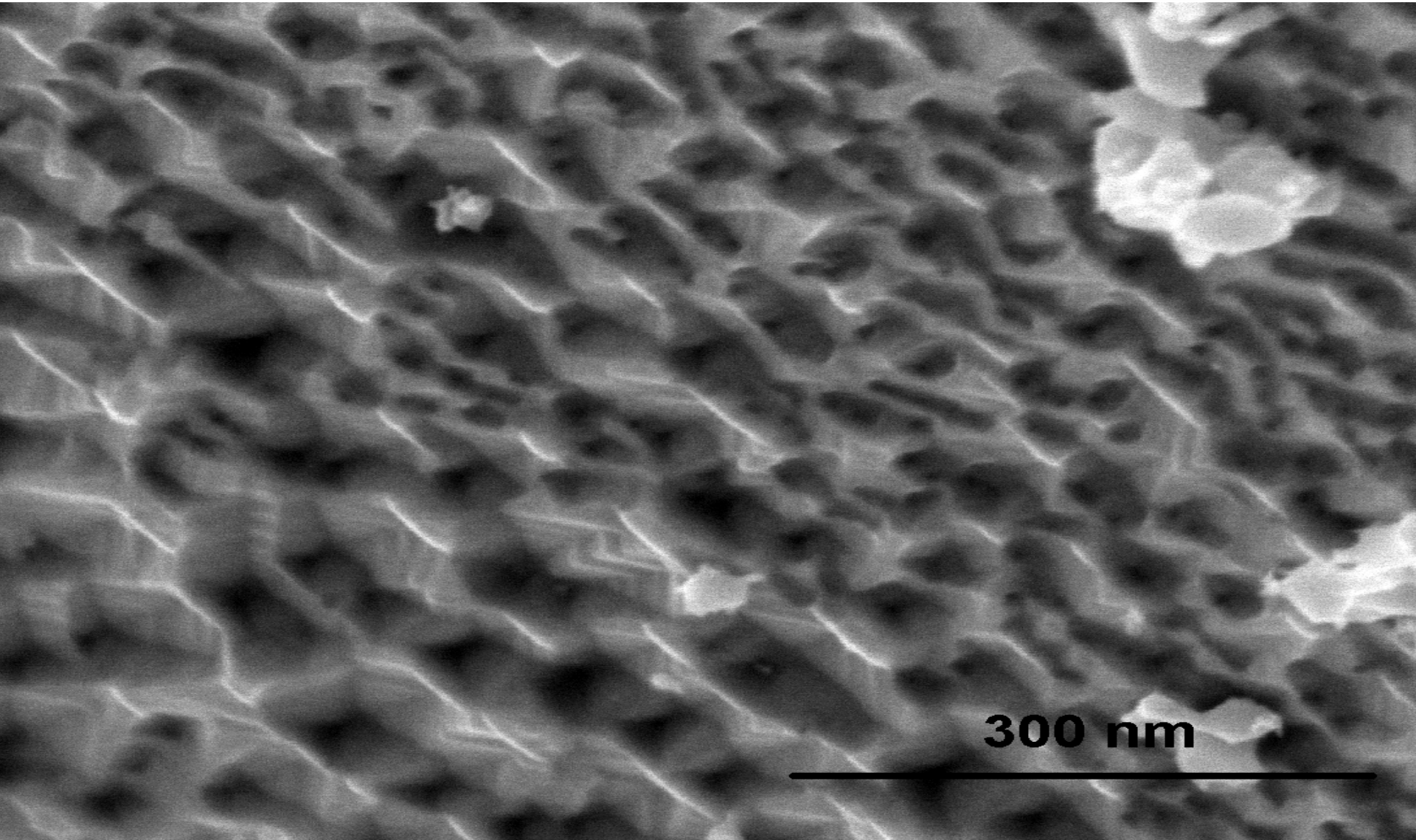


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Standard model of heterogeneous catalysis deep understanding, limited function

HZB Helmholtz
Zentrum Berlin

unicat
Unifying Concepts in Catalysis



300 nm



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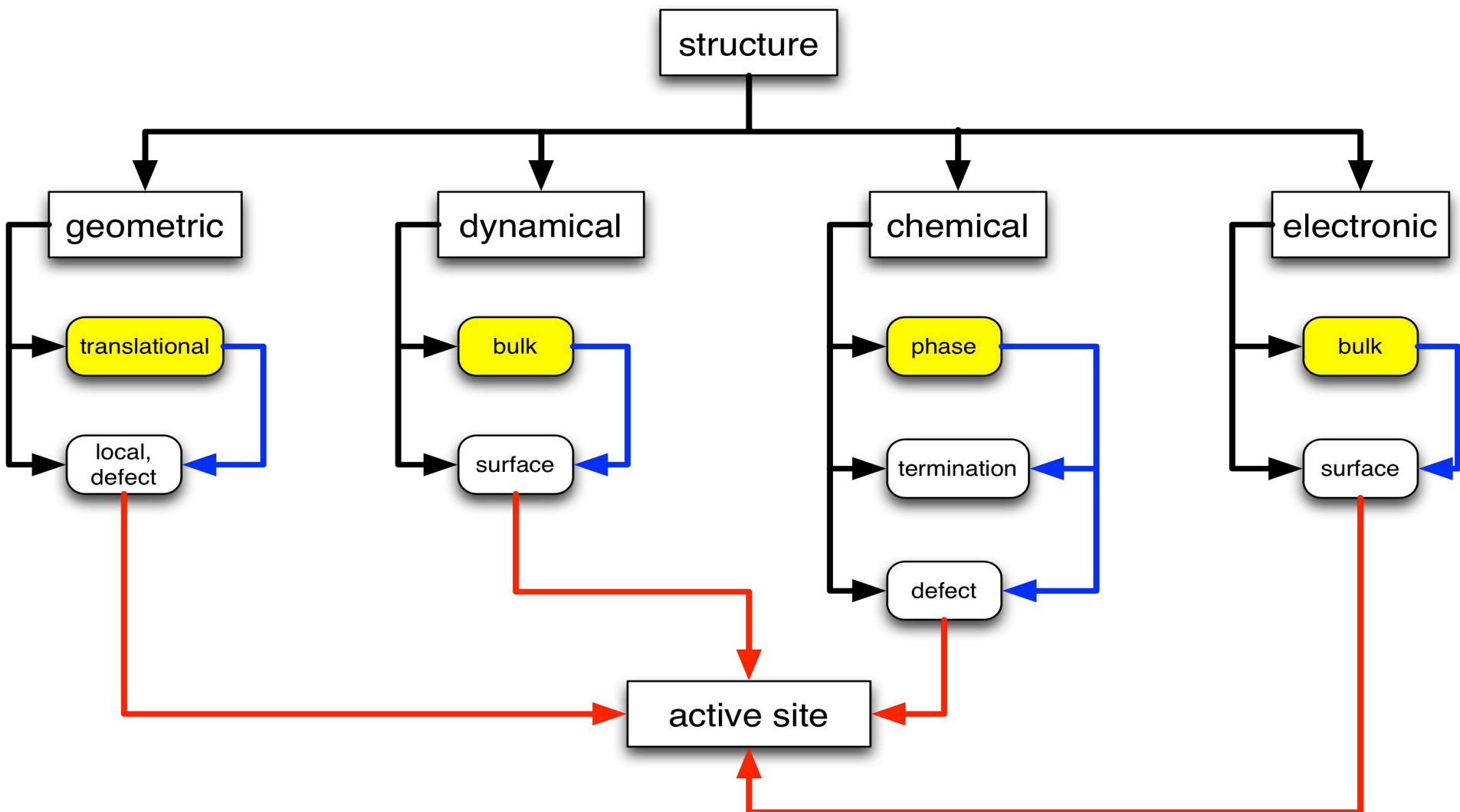
More complexity: Active sites In-situ analysis

HZB Helmholtz
Zentrum Berlin

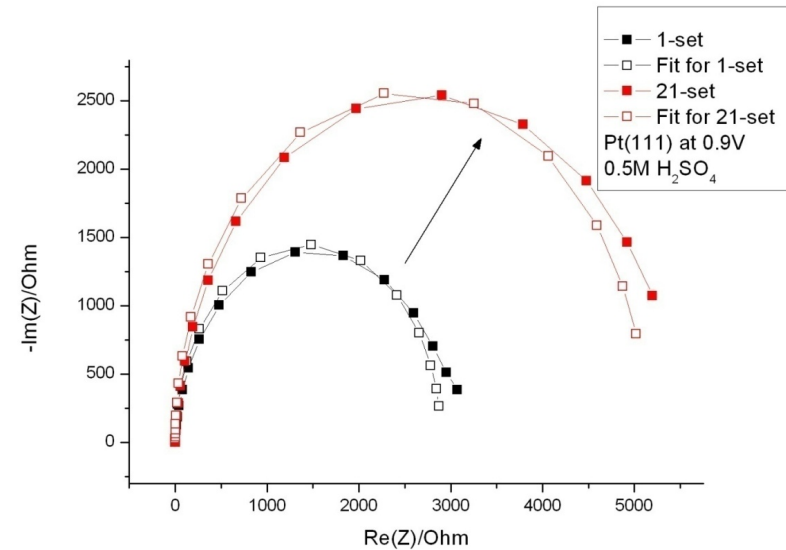
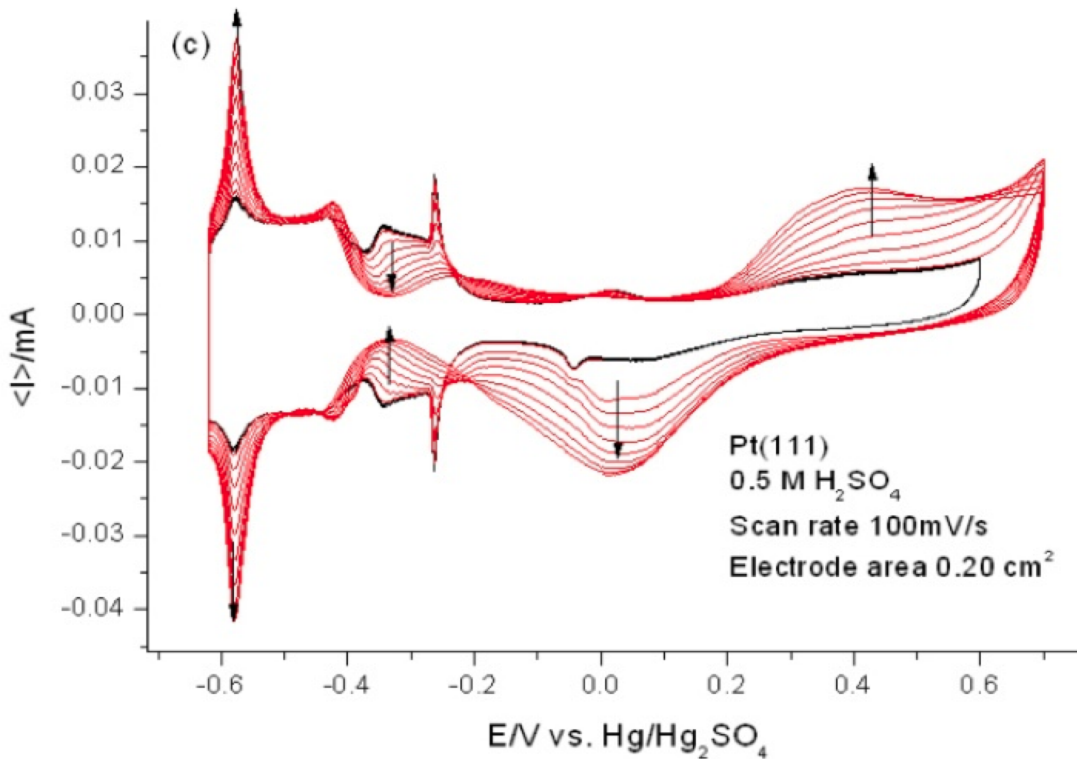
unicat
Unifying Concepts in Catalysis

- The central concept in all types of catalysis.
- Act as coordination centres allowing to exchange adsorbates (fragments) and electrons (oxidation state).
- Are modified during chemical bond rearrangement.
- In a catalytic cycle they are regenerated in to their most active initial state.
- Adaptivity required as mostly the reaction product is more reactive than the starting species: selectivity through autogenous partial deactivation.

Catalyst structure: A variable target

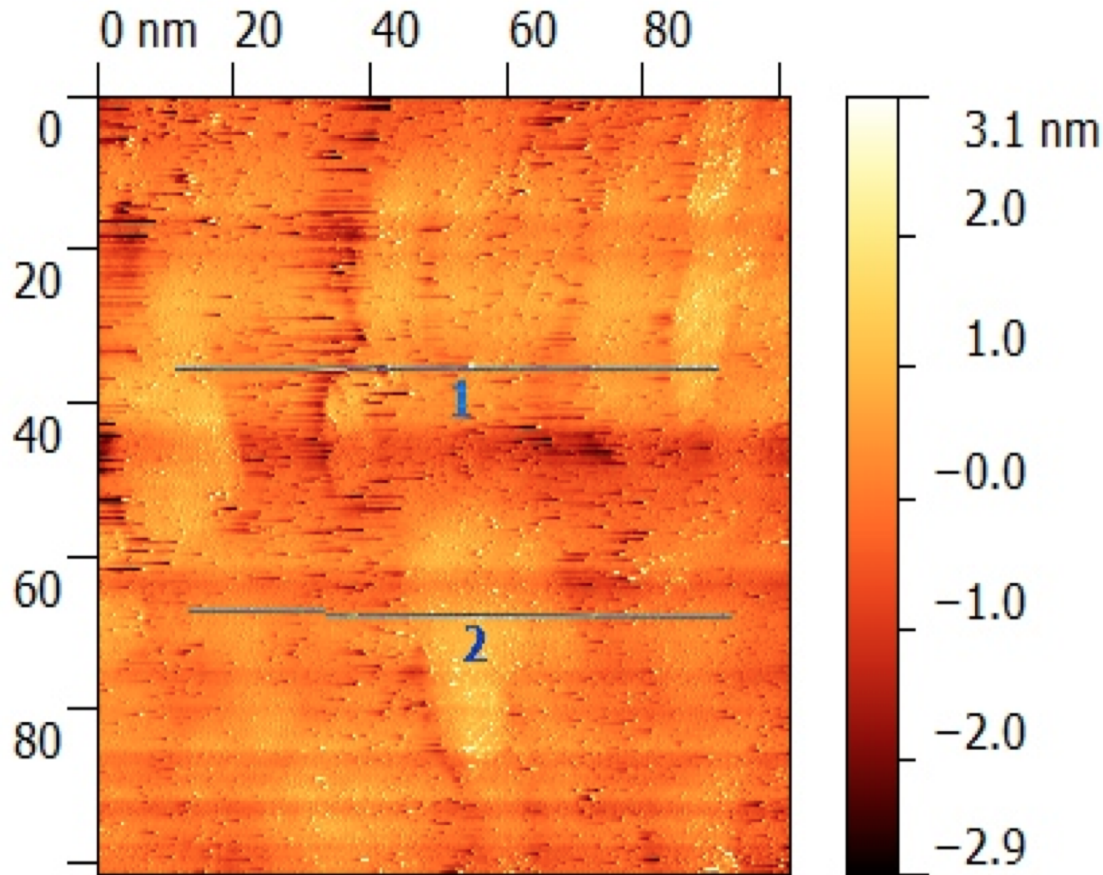


Excursion: Dynamics of Pt in OER

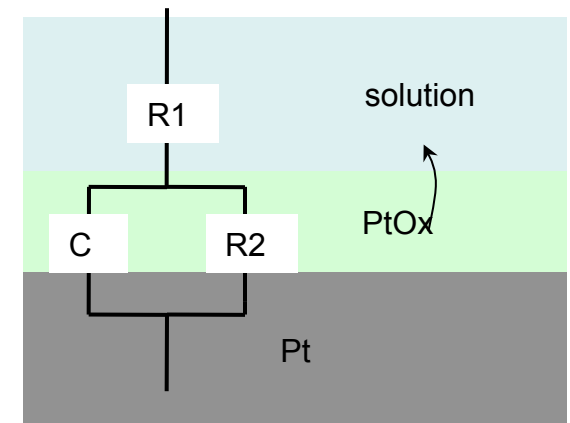


Irreversible roughening
 Enhanced hydrogen production
 Oxidic overlayer pre-requisite for OER

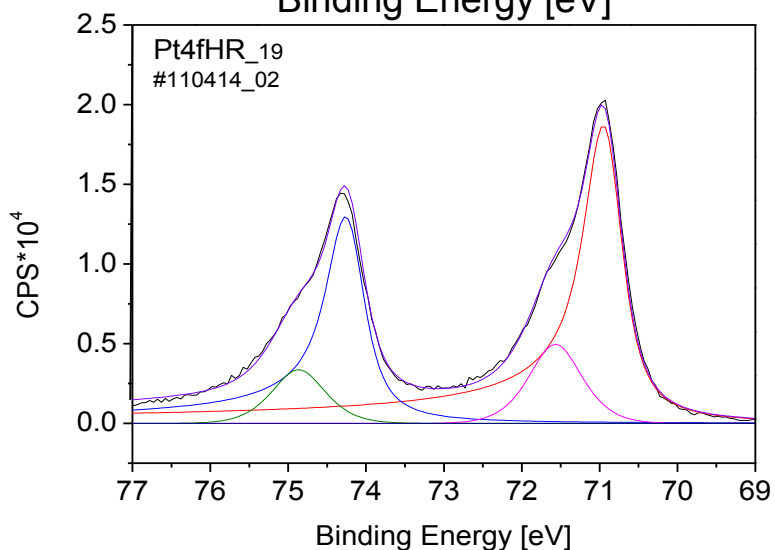
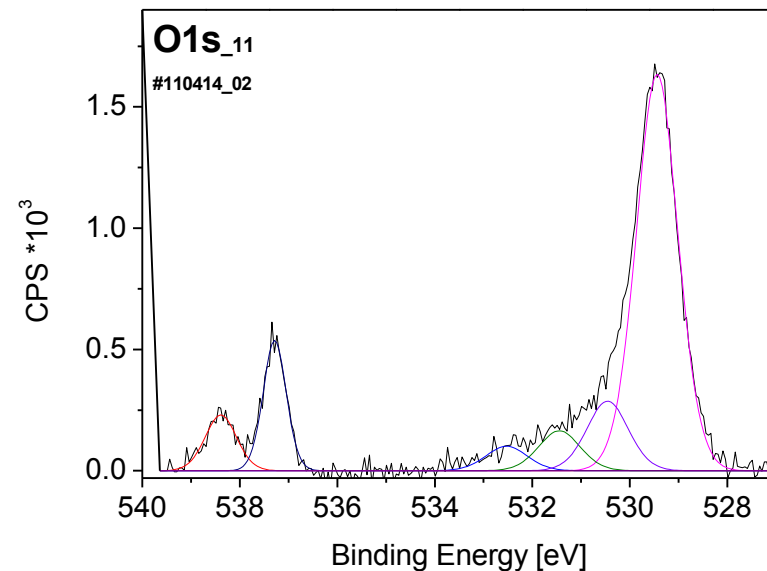
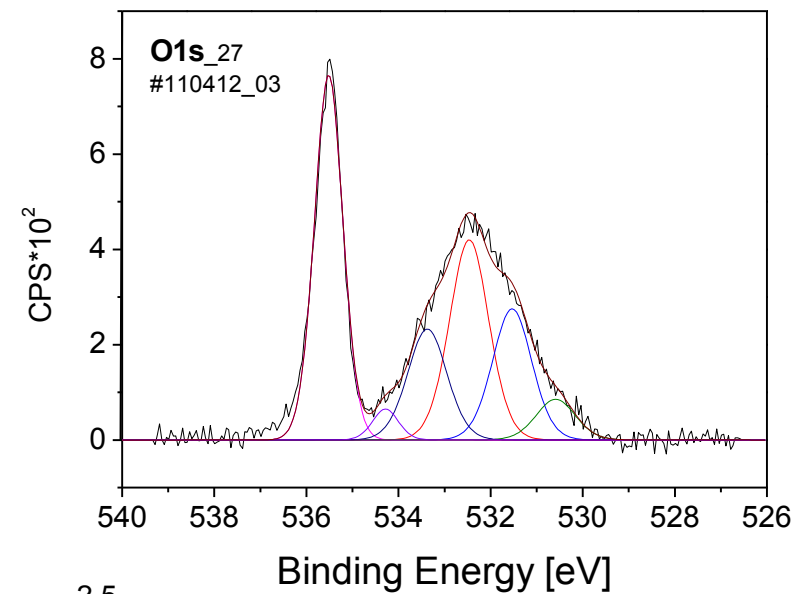
Excursion: Dynamics of Pt in OER



	R1+C2/R2	1-Set	21-set
R1 ($\Omega \cdot \text{cm}^2$)		1.68	1.69
C2 ($\mu\text{F}/\text{cm}^2$)		51	48.9
R2 ($\Omega \cdot \text{cm}^2$)		2901	5 151



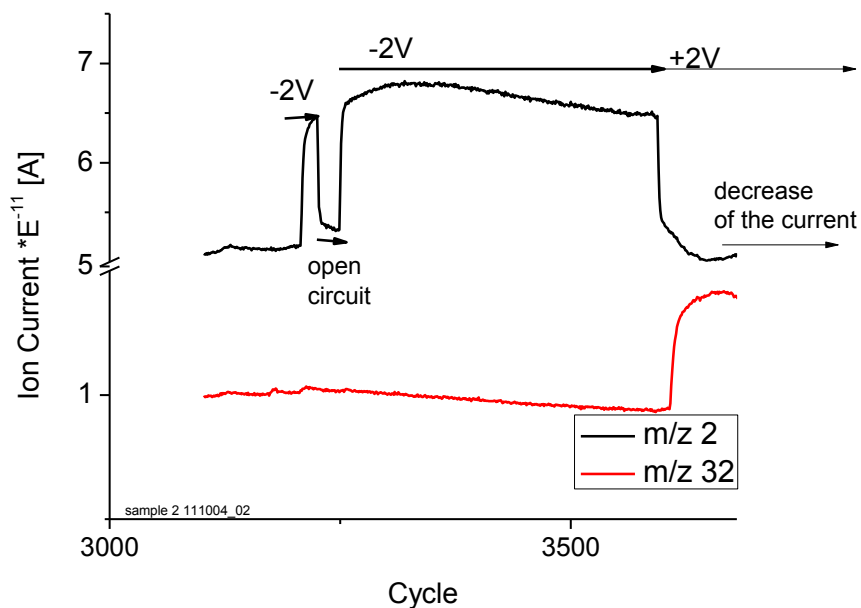
Nature of the Pt “rust” film



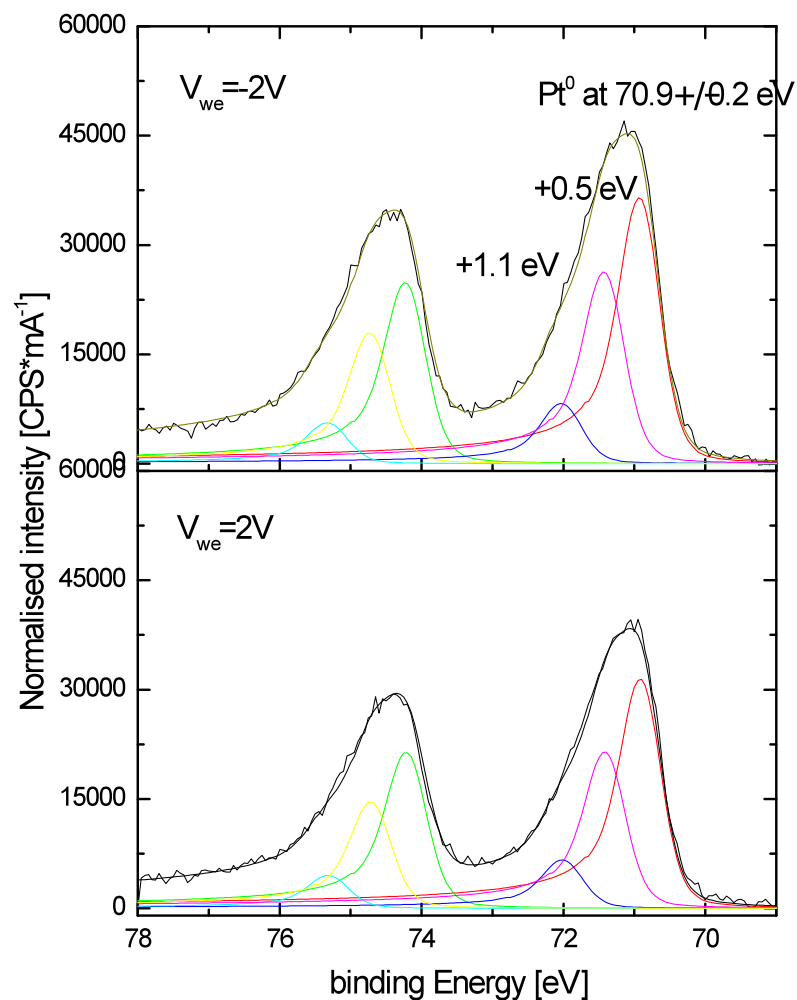
Ambient pressure XPS at very high resolution and extreme surface sensitivity:

Pt is covering with a one monolayer film of hydroxide in water leaving divalent Pt.

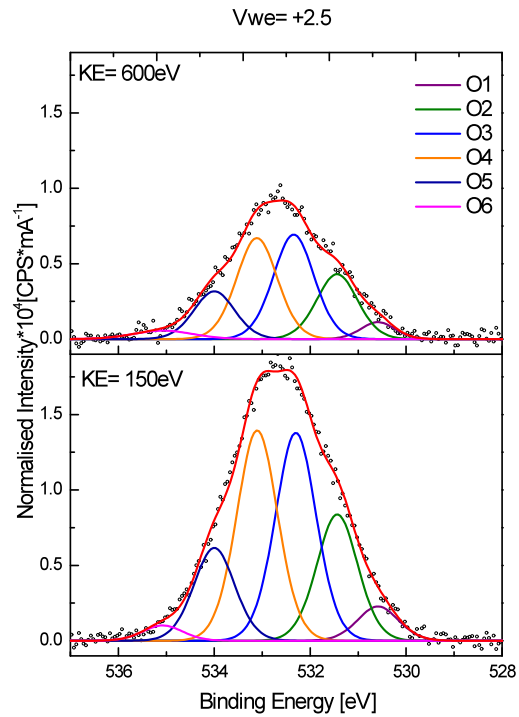
In-situ observation



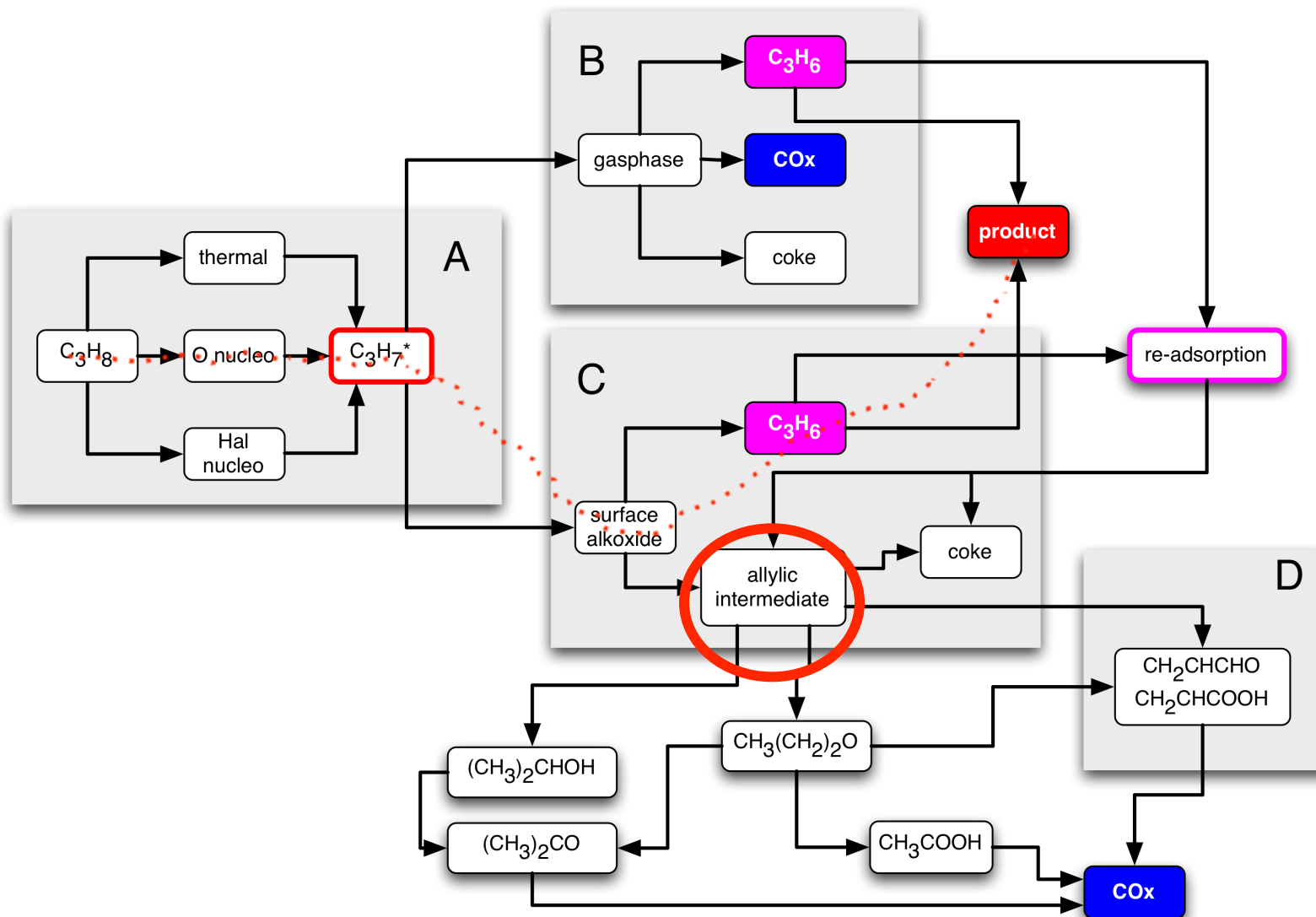
Pt forms a mixture of sub-surface oxygen species converting gradually into Pt O (OH)



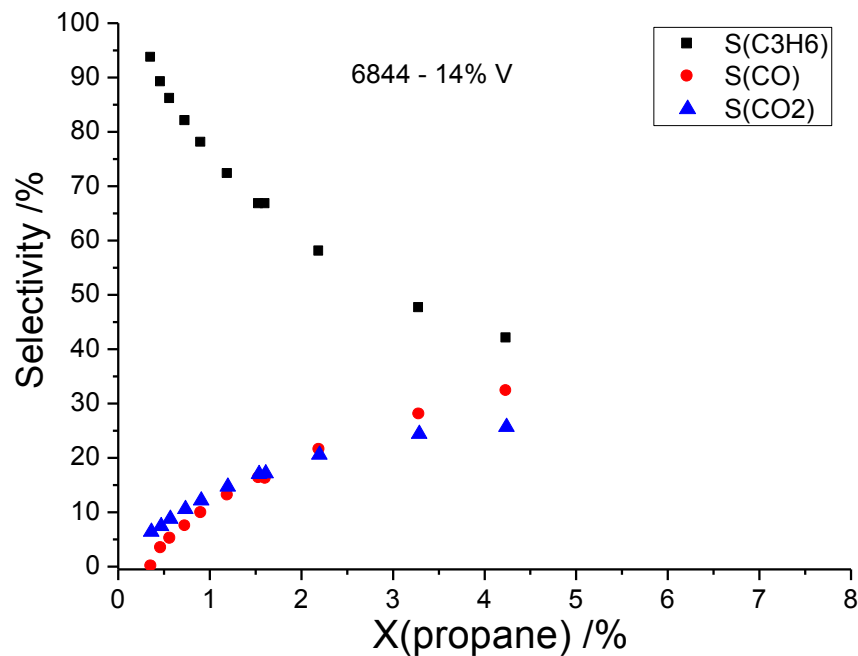
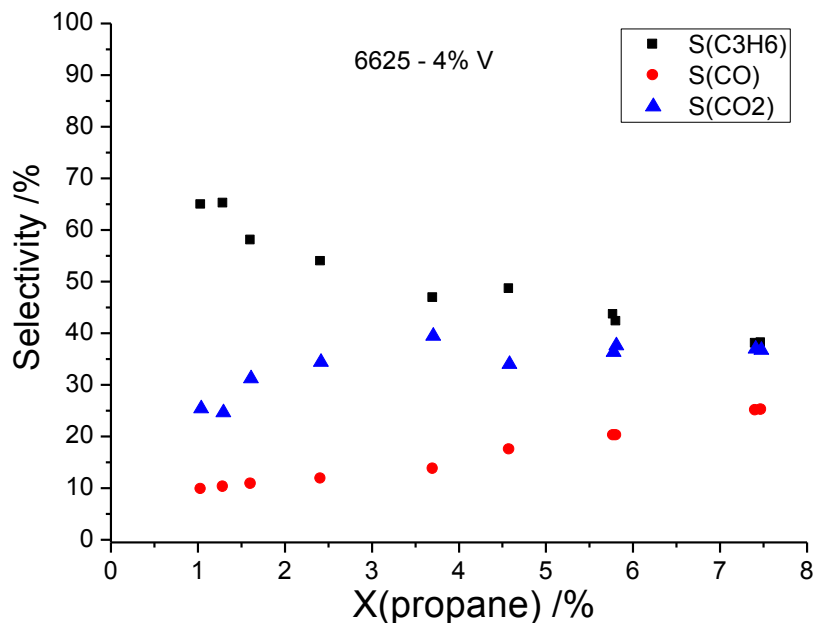
In-situ observation



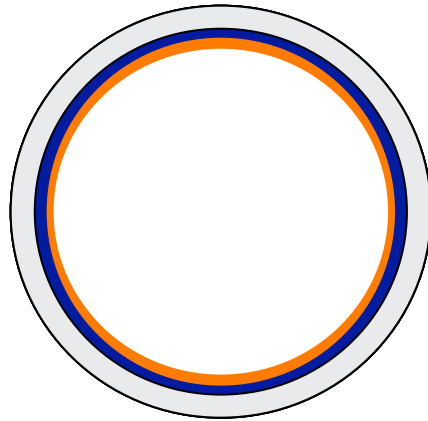
C3 oxidation: C_3H_8 to C_3H_6 a “simple” reaction network



C3 oxidation: C_3H_8 to C_3H_6 a “simple” reaction network



An oxide model system monolayers in a bottle



V-Ti/SiO₂

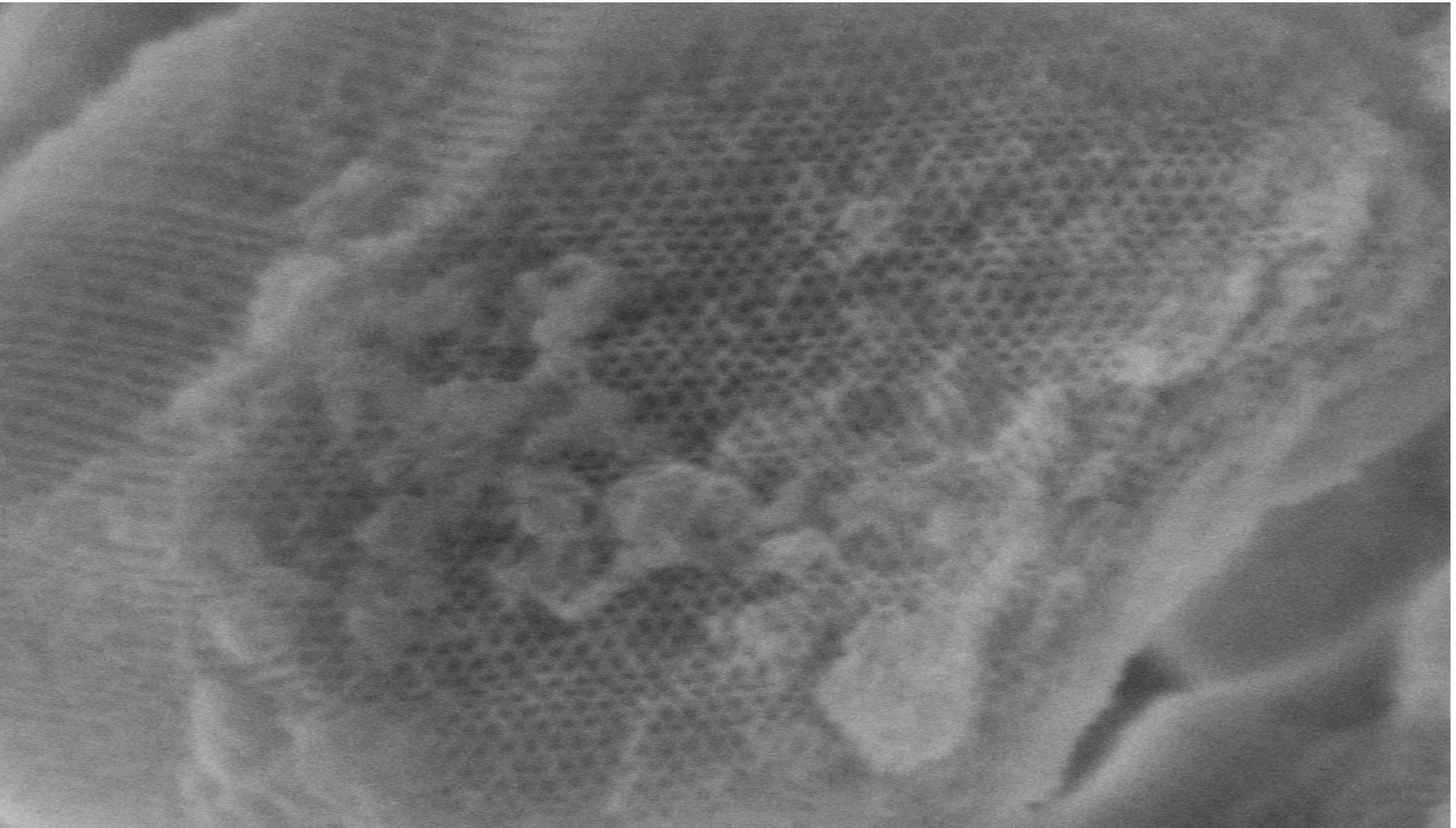
Why SBA-15?

- Regular pore structure allows the application of an extended number of physico-chemical methods
- High surface density of silanol groups available for anchorage of metal oxide species = high number of exposed V species
- V/SBA-15 is an efficient catalyst for oxidative dehydrogenation of propane (STY_{max} (FHI) = 1.5 g C₃H₆ /g_{cat} / h)

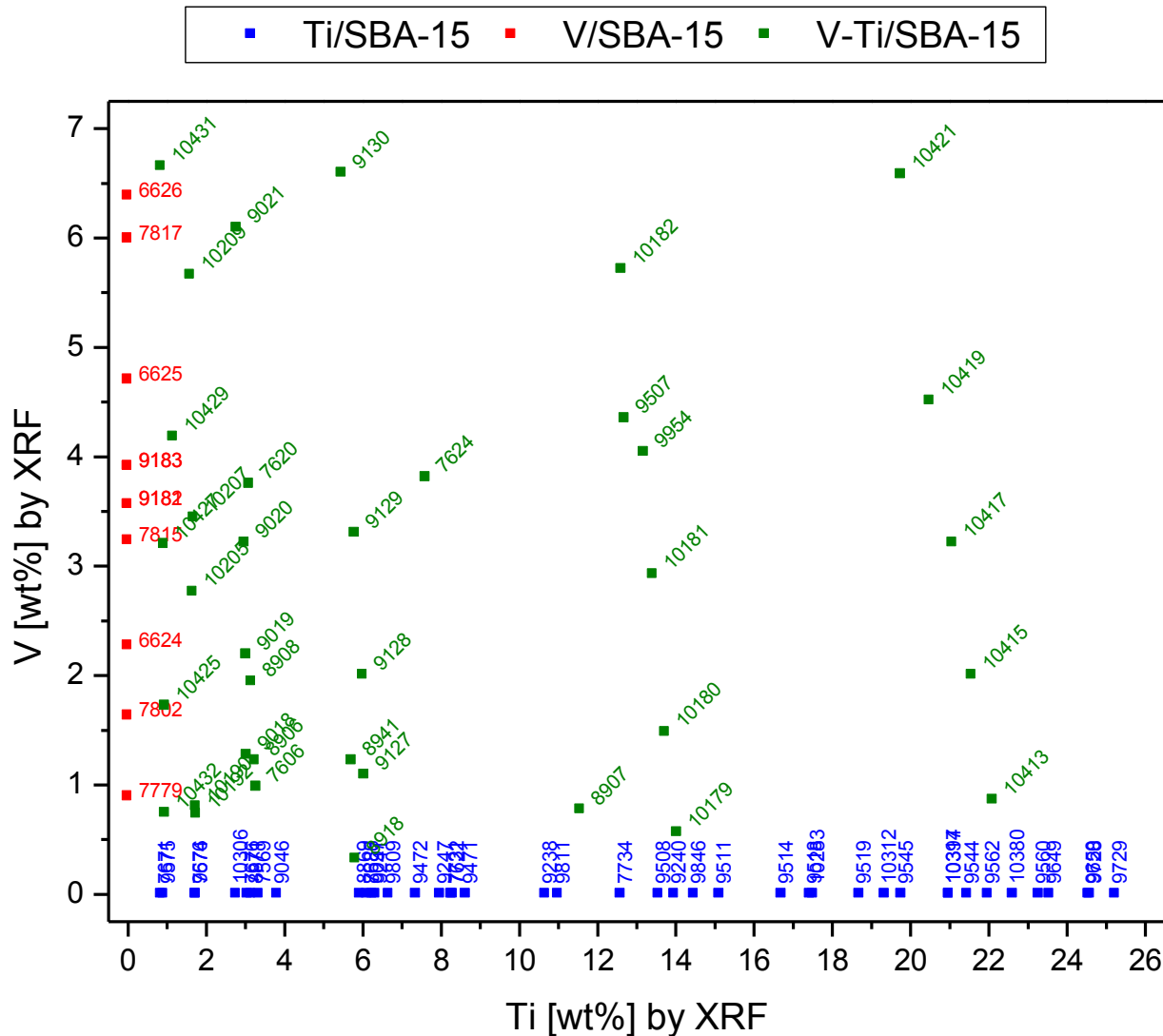


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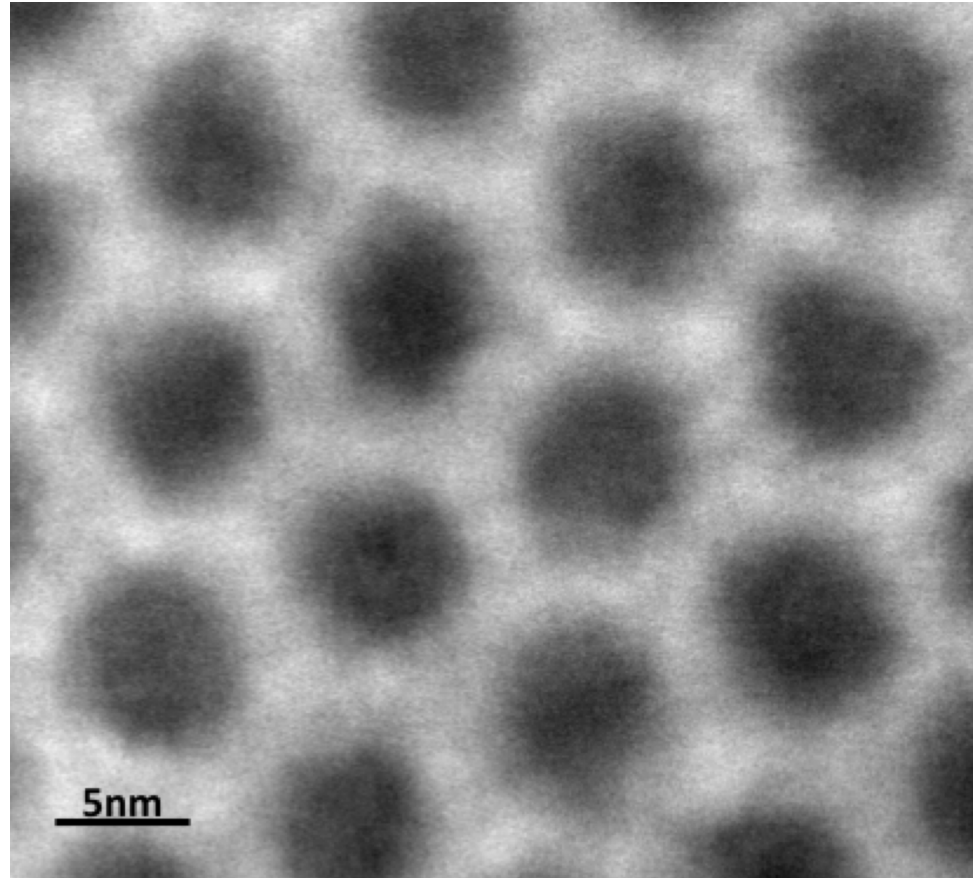
An oxide model system monolayers in a bottle



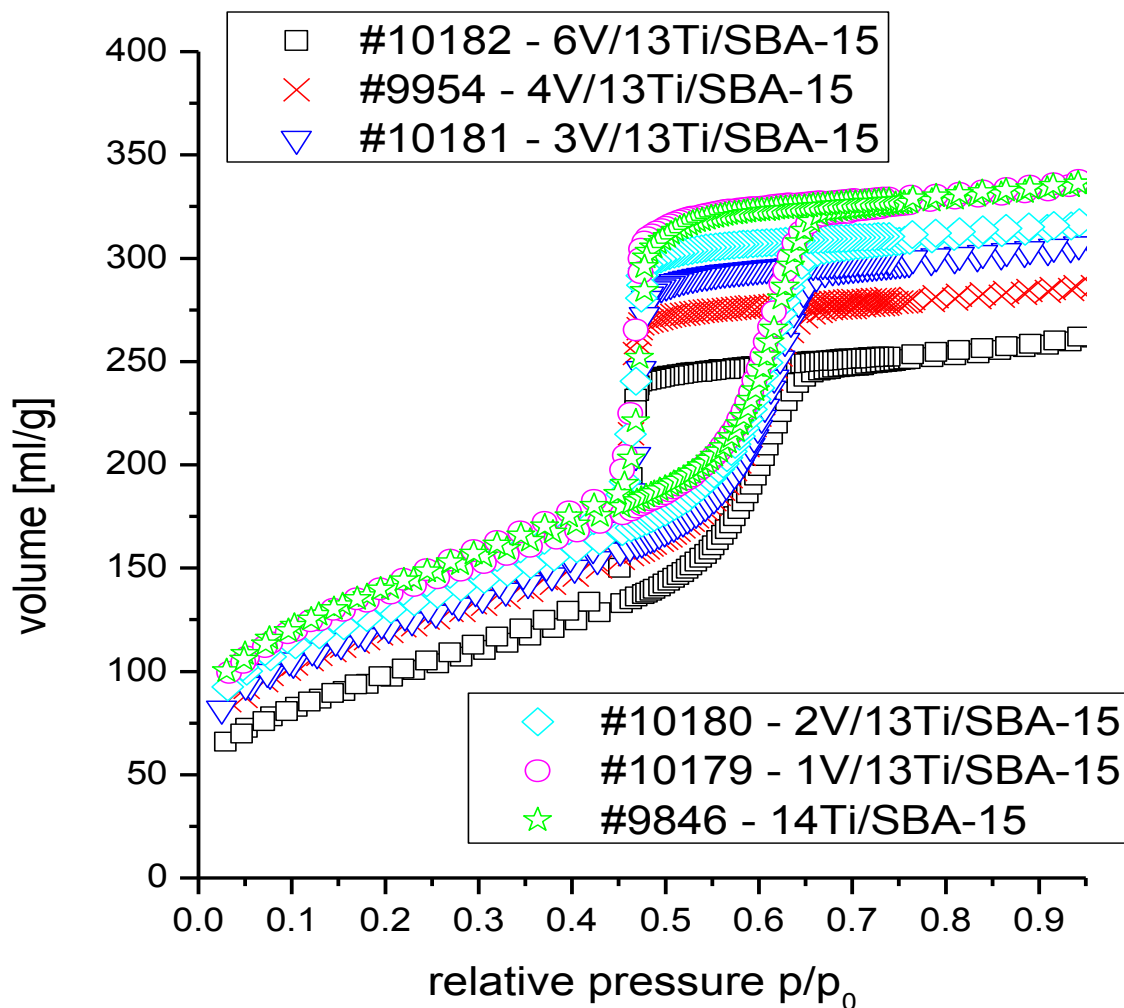
A catalyst library based on a common structure



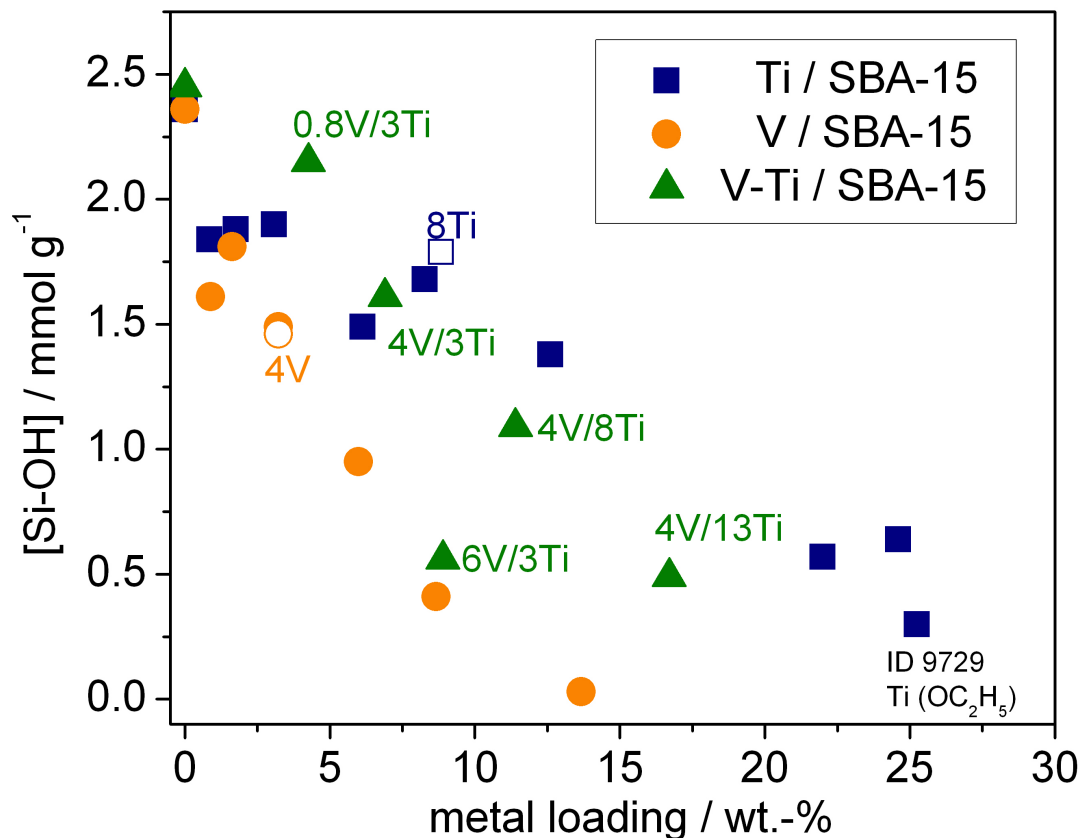
A catalyst library based on a common structure



A catalyst library based on a common structure



The design concept of a homogeneous library



V locates on mixed systems both in pores of SBA and on Ti:

V-Si dominated by V-V interactions (homodimer)

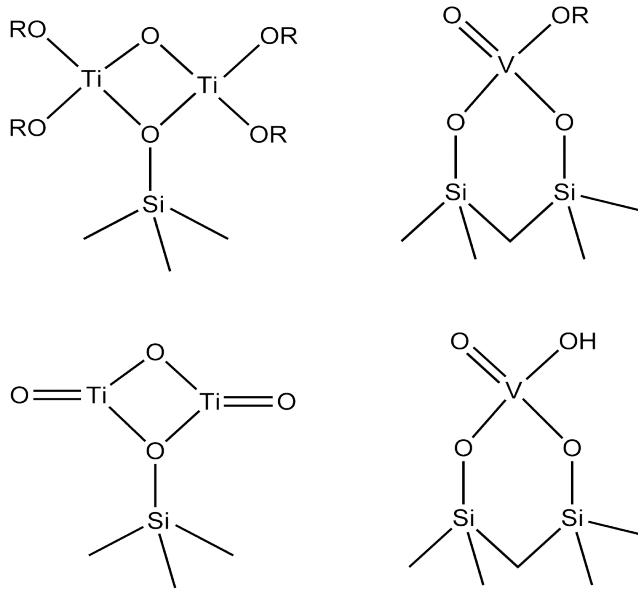
V-Ti dominated by V-Ti bonds (heterodimer)

V seems to require exactly twice as many silanol groups than Ti

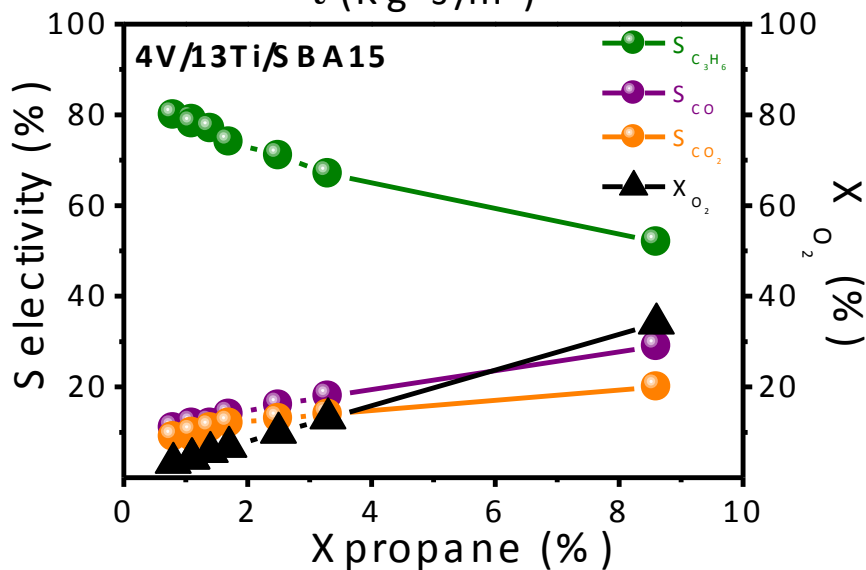
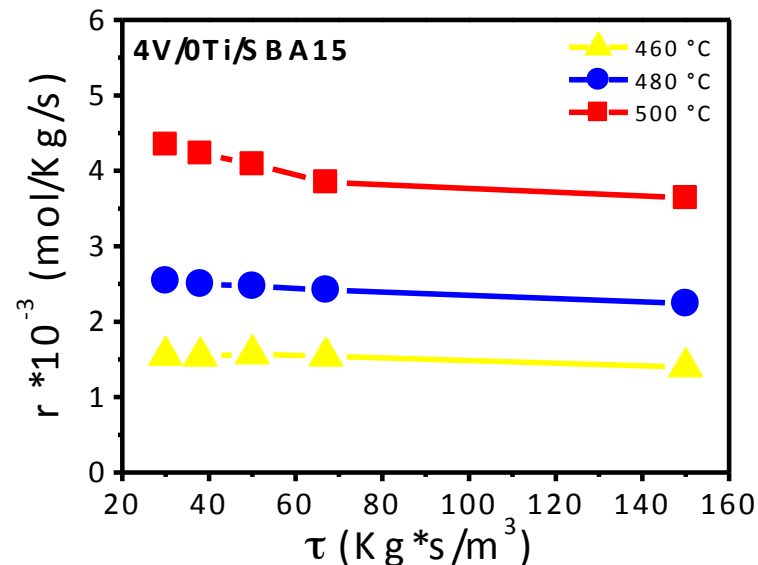
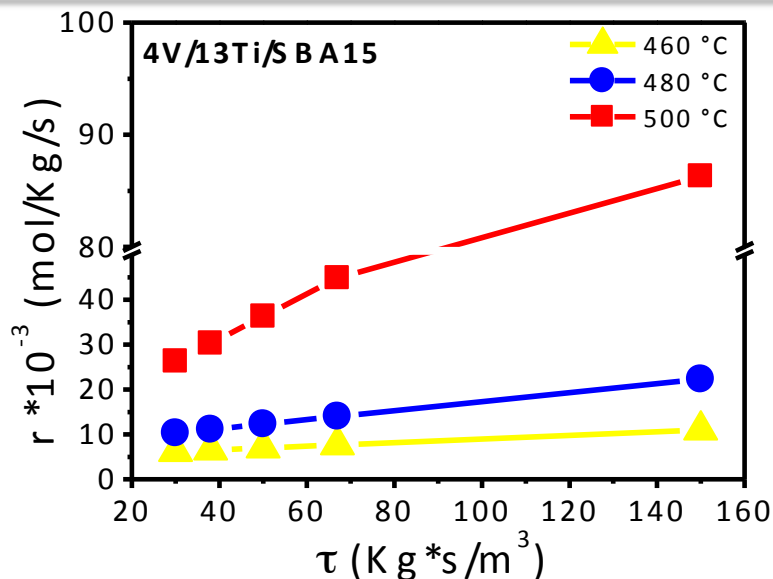
Only V introduces Brønsted OH into the system, Ti exhibits no free OH
 As Ti liberates 2 alkoxide per molecule, dimer structure as long as sufficient space

The design concept of a homogeneous library

Hydrolysis

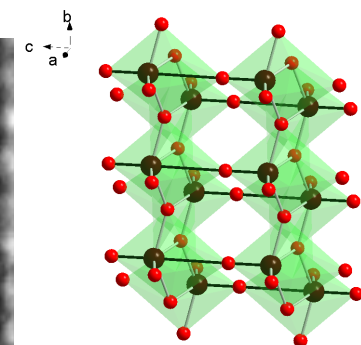
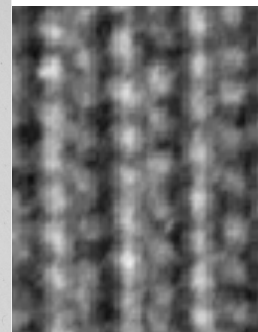
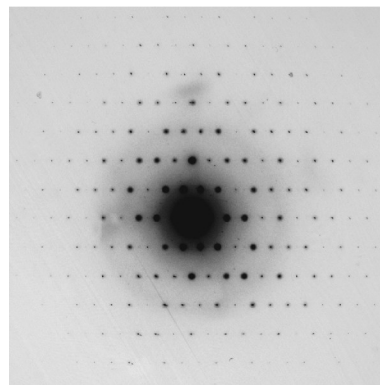
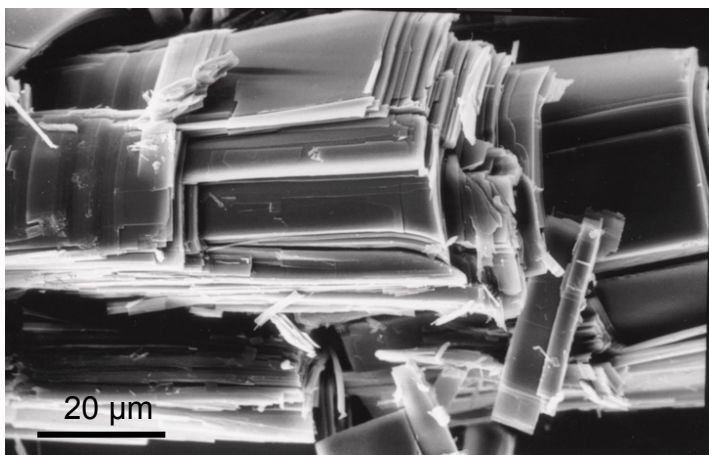
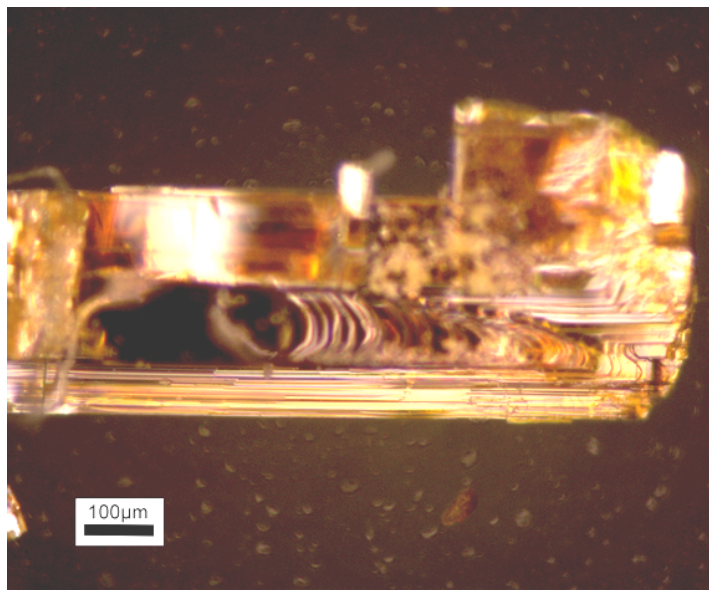



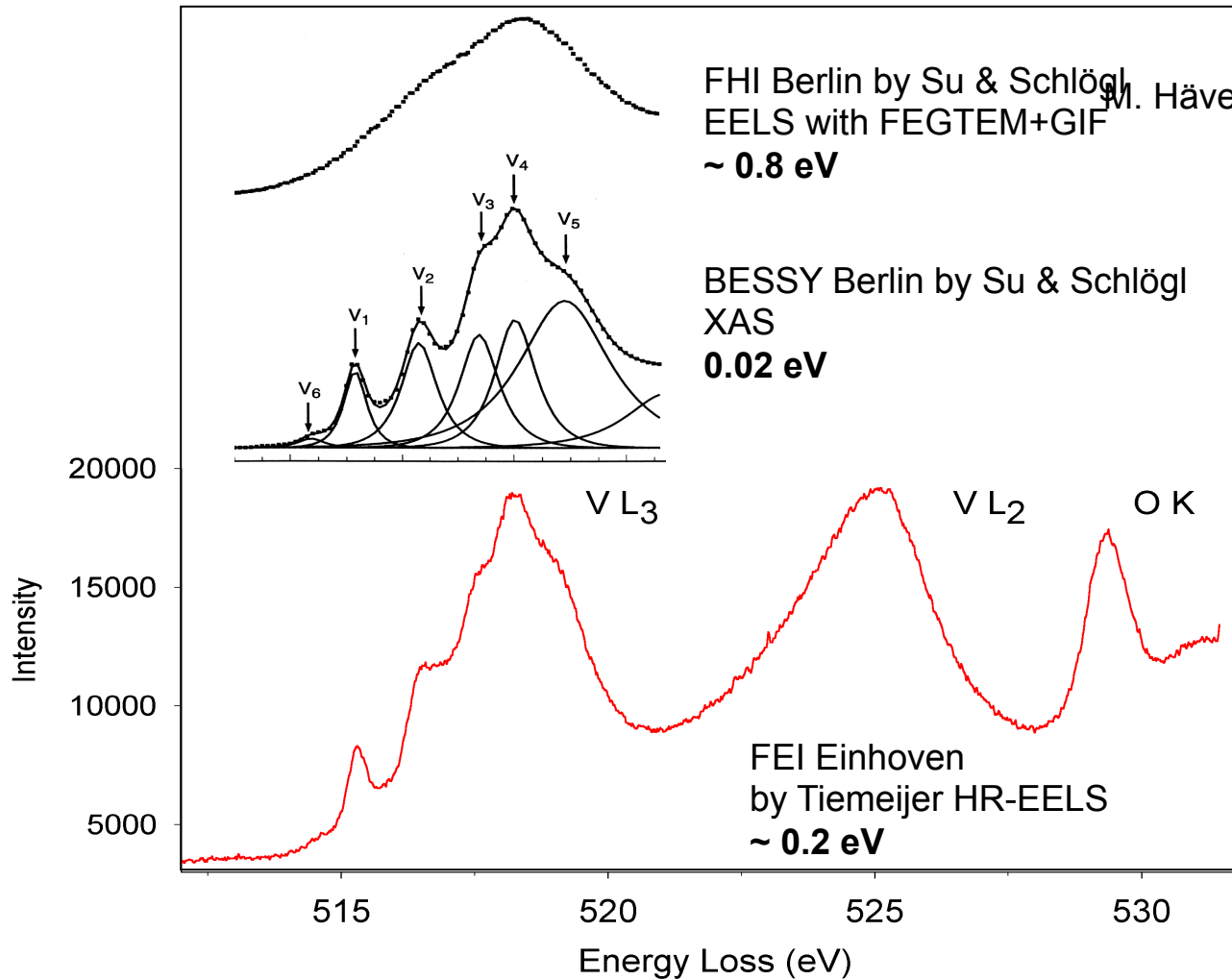
Is this good?



Catalysis:
Massive improvement of
performance when V is deposited on
Ti that is sufficiently covered to
minimize O_2^-
Gold standard:
 10^{-2} mol/kg/h

V_2O_5 the parent reference



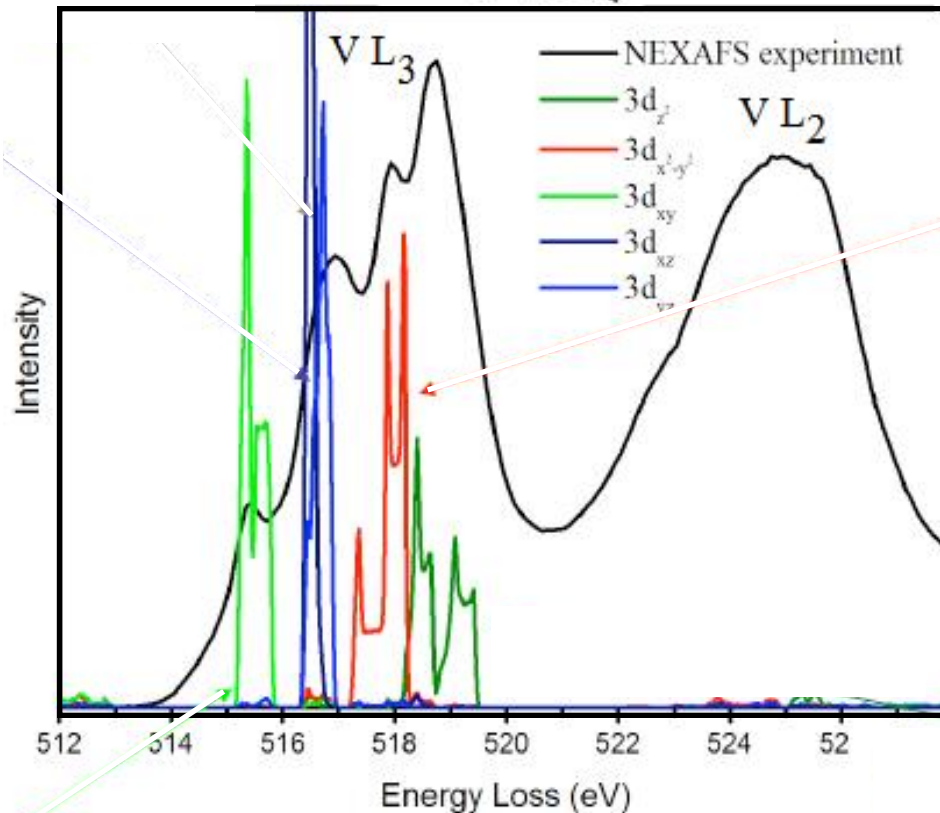


FHI Berlin by Su & Schlögl, M. Hävecker, F. Neese et al 2012
EELS with FEGTEM+GIF
~ **0.8 eV**

BESSY Berlin by Su & Schlögl
XAS
0.02 eV

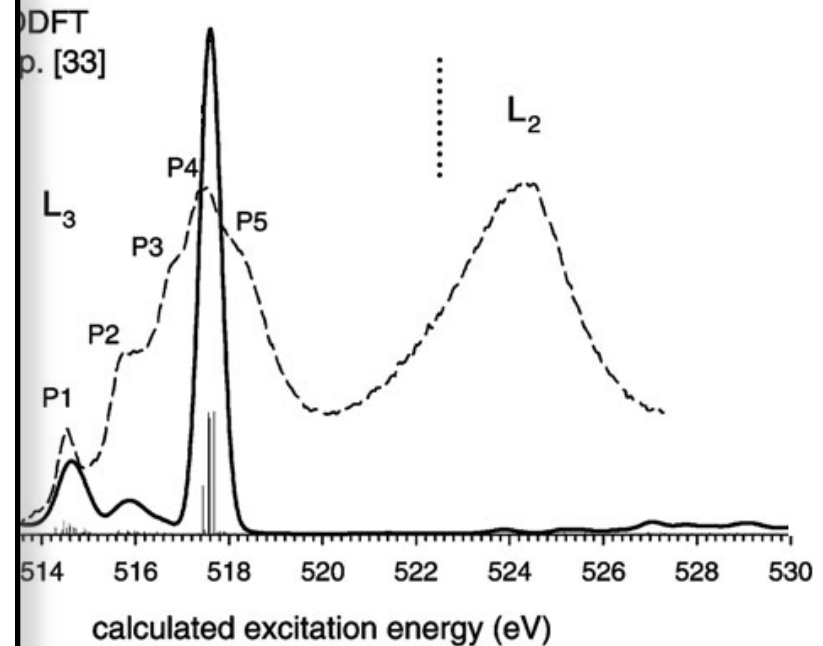
FEI Eindhoven
by Tiemeijer HR-EELS
~ **0.2 eV**

Ligand Field Multiplet

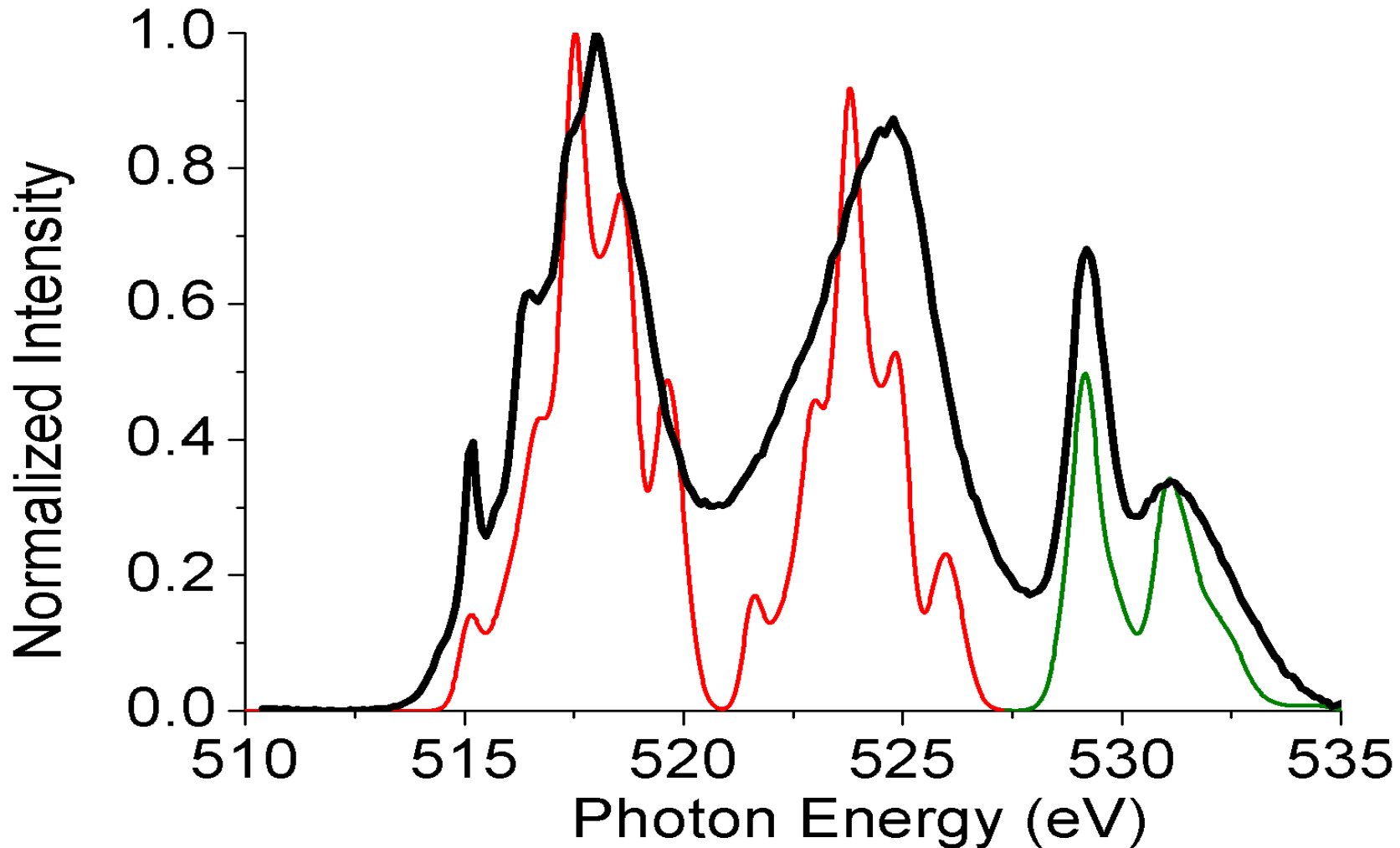


(M. Willinger et al, 2006.)

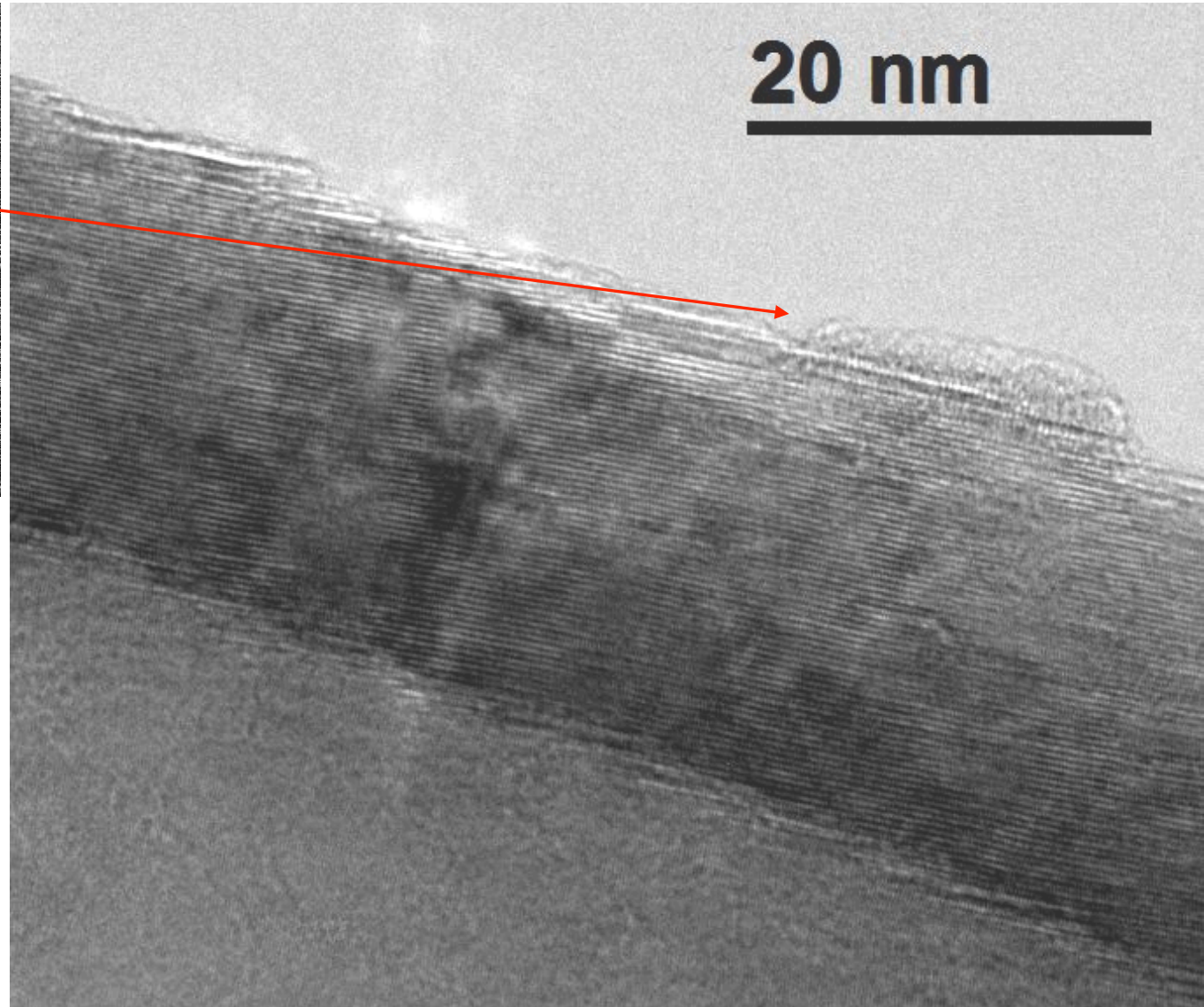
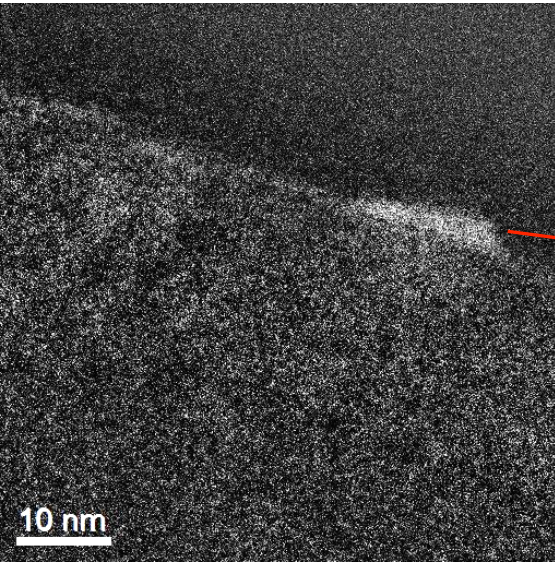
TD-DFT



o, R.; Stener, M.; Causa, M.; Toffoli, D.; Fronzoni, *Chemistry Chemical Physics* **2006**, *8*, 4300.

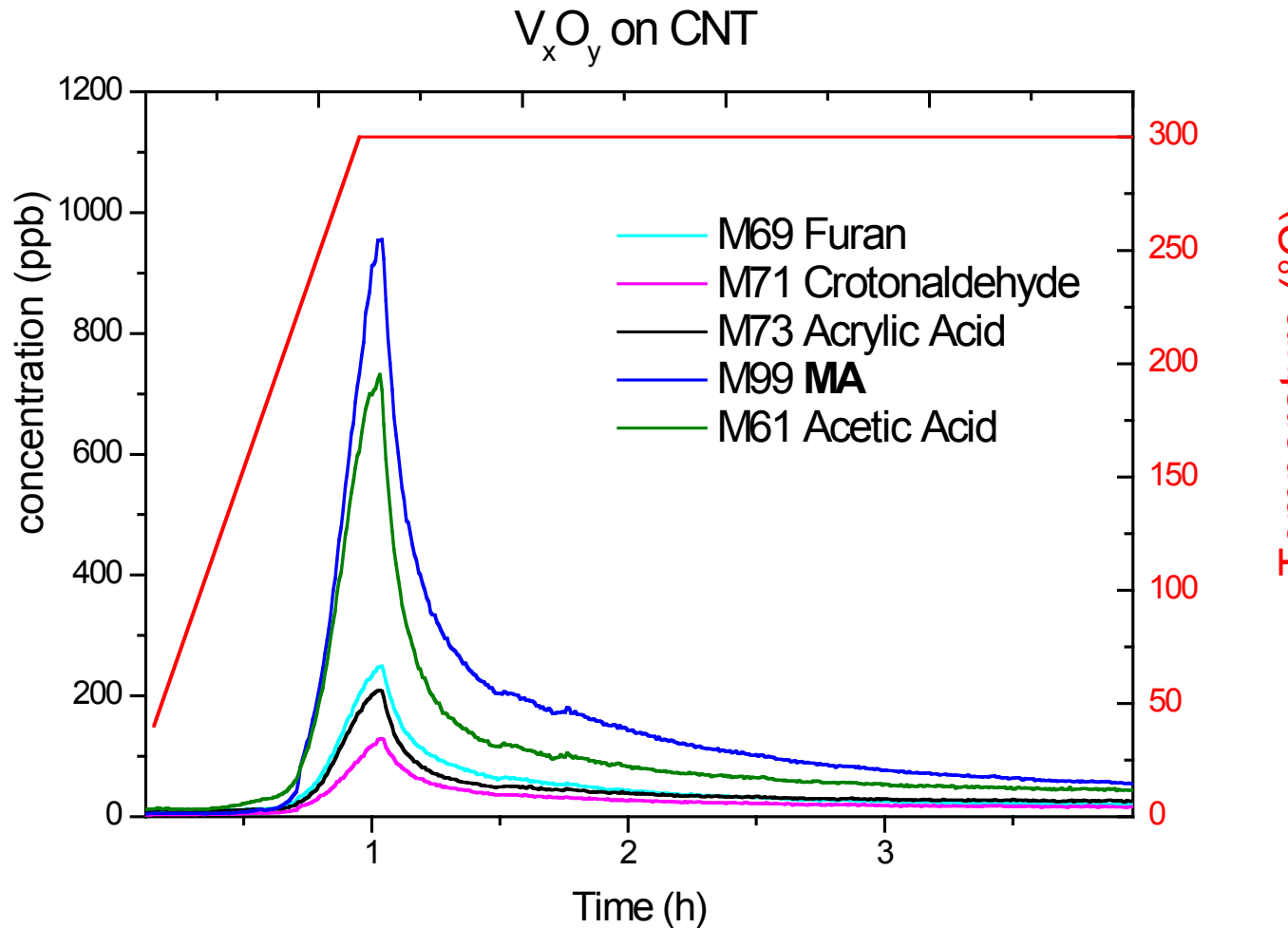


CNT supported $VxOy$ reactivity vs. structural dynamics



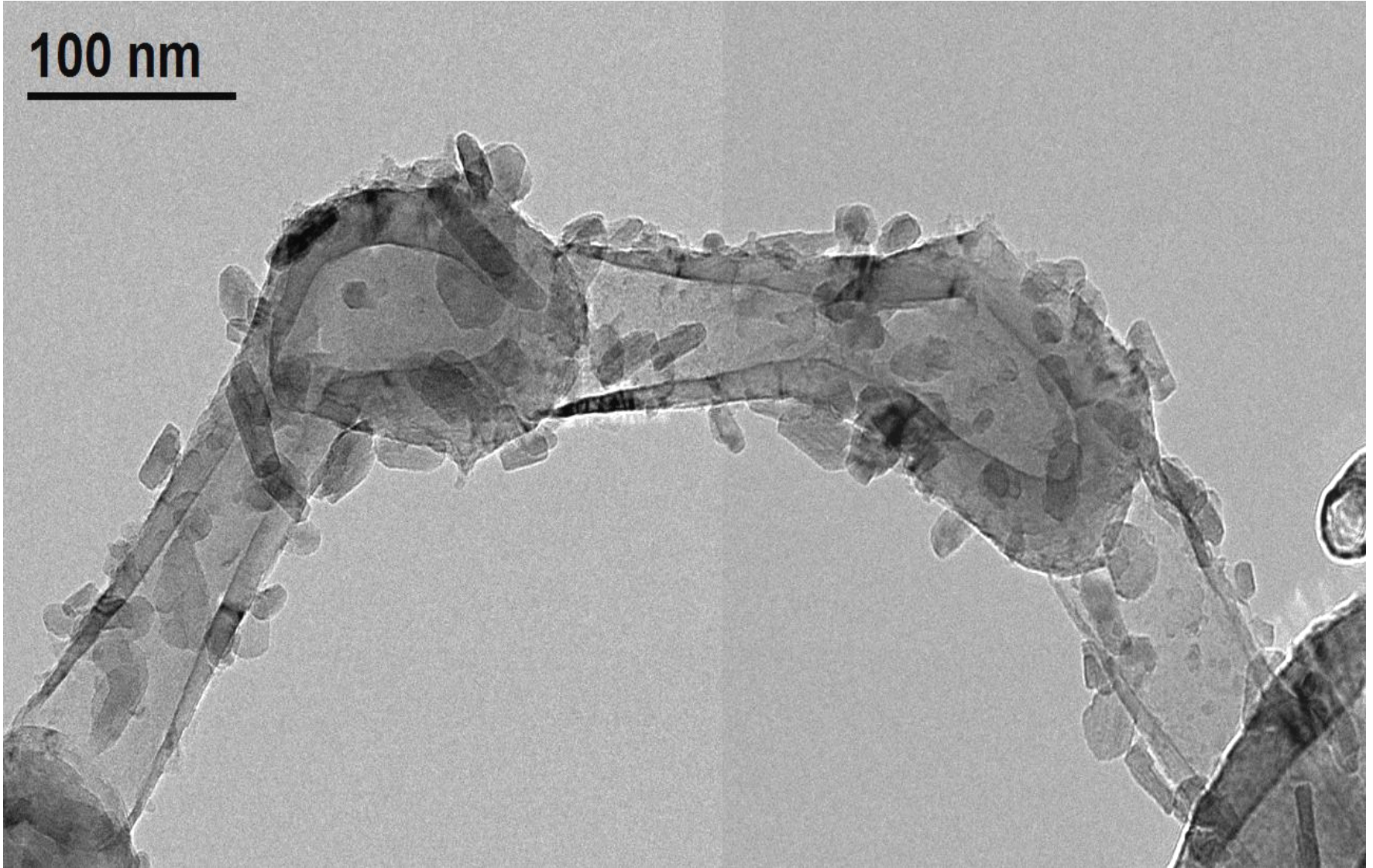
Vanadium map

CNT supported V_xO_y reactivity vs. structural dynamics

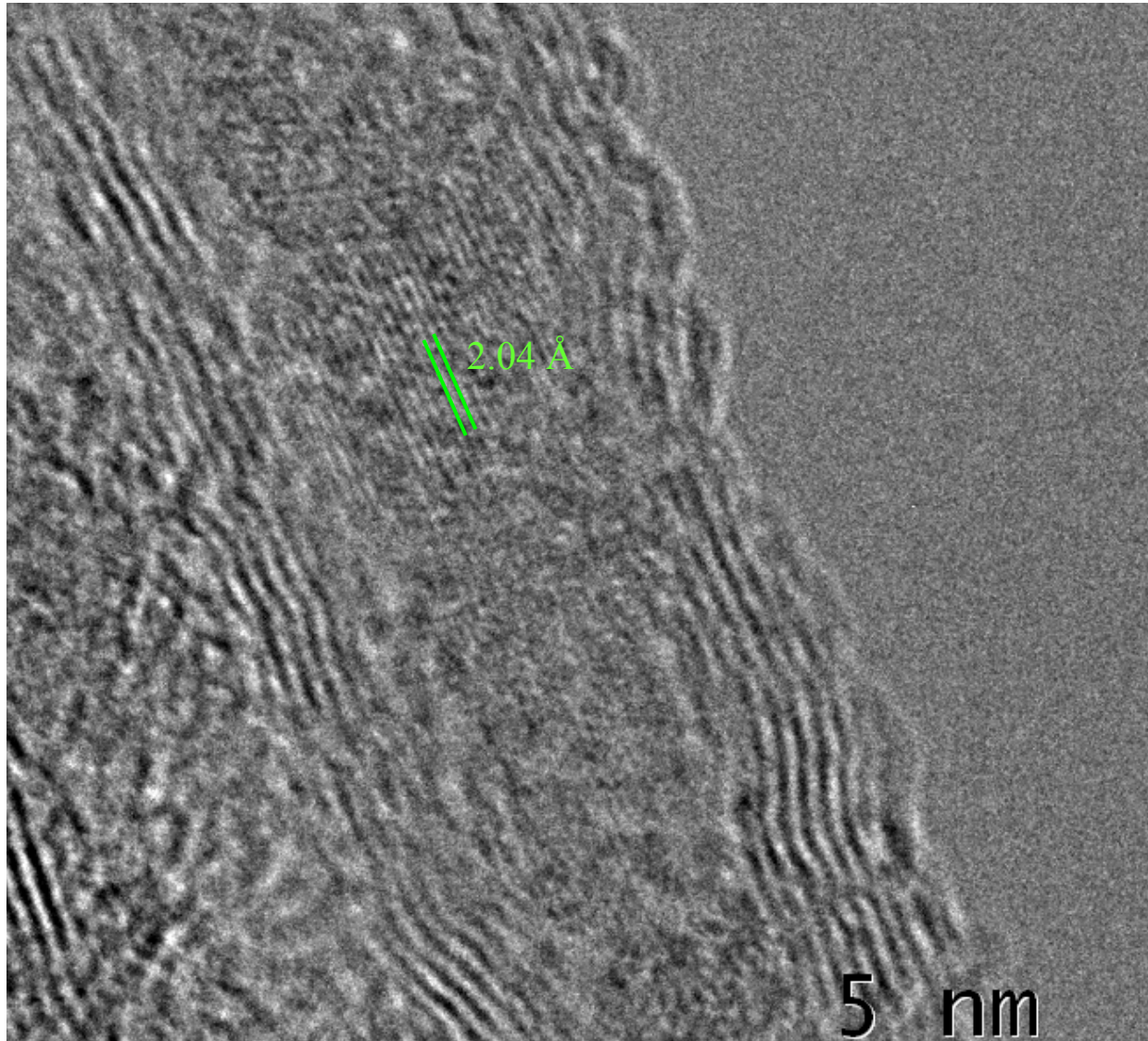


CNT supported V_xO_y reactivity vs. structural dynamics

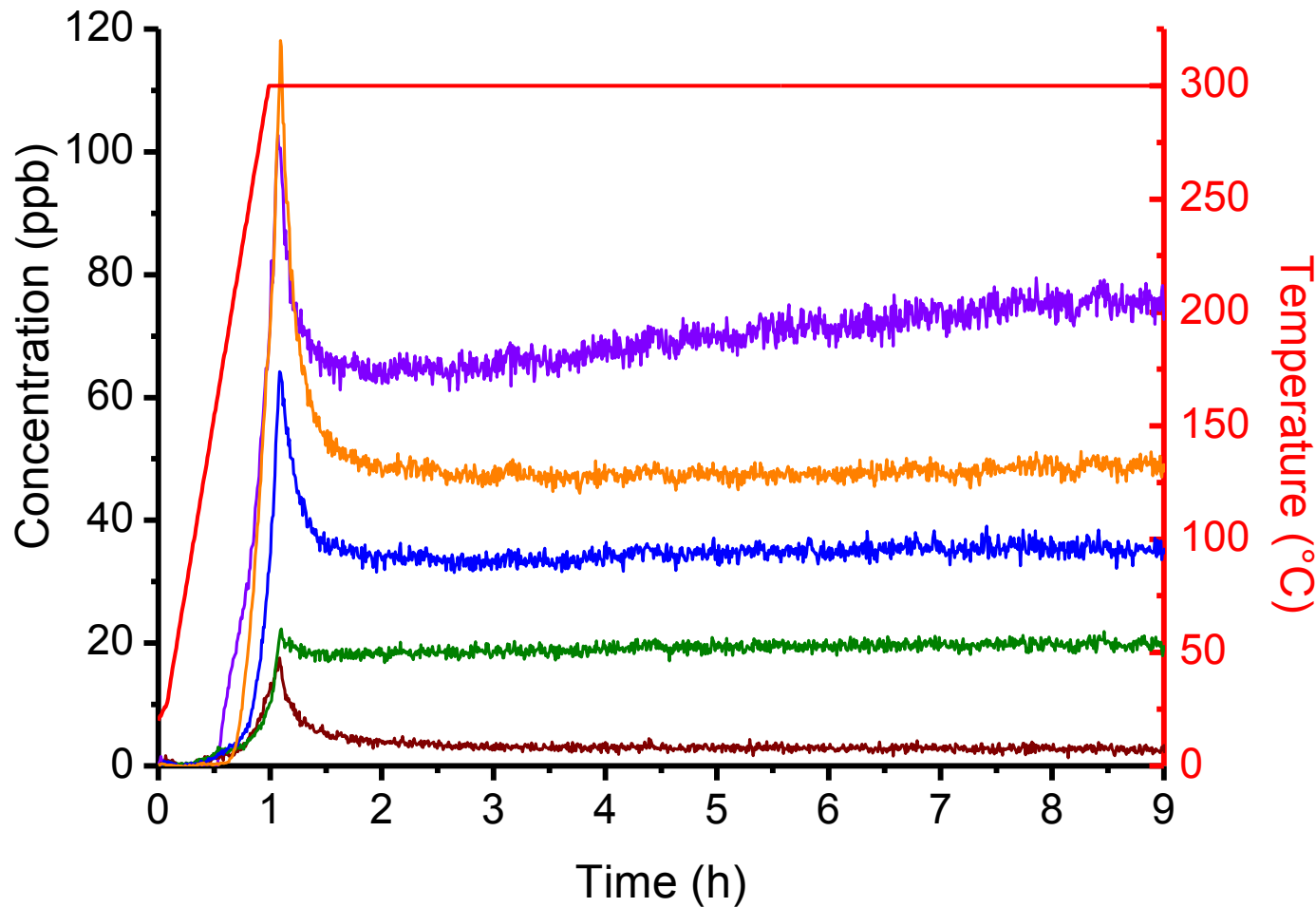
100 nm



CNT supported V_xO_y reactivity vs. structural dynamics



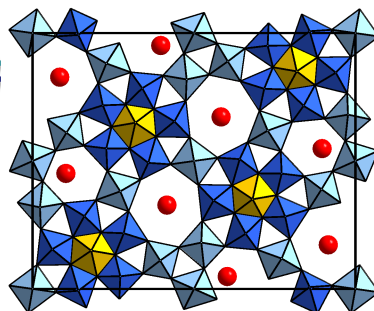
CNT supported VxOy reactivity vs. structural dynamics



C3 oxidation II

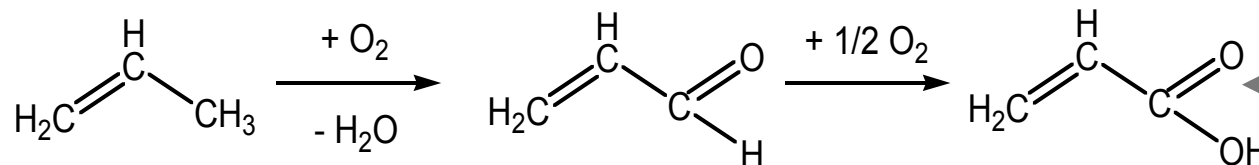
- MoVTeNb oxide
- polycrystalline
- M1/M2 phases

M1



- Y < 55 %
- stability is an issue

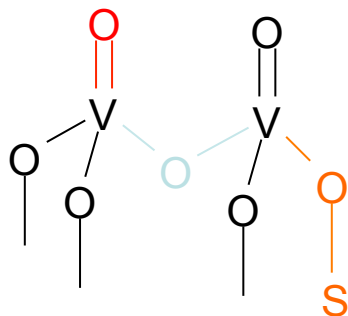
MoVTeNb



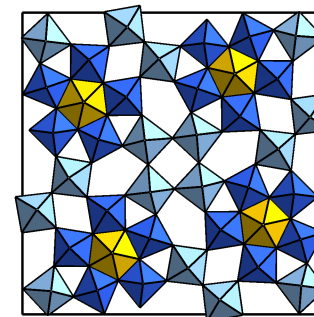
V

MoBi

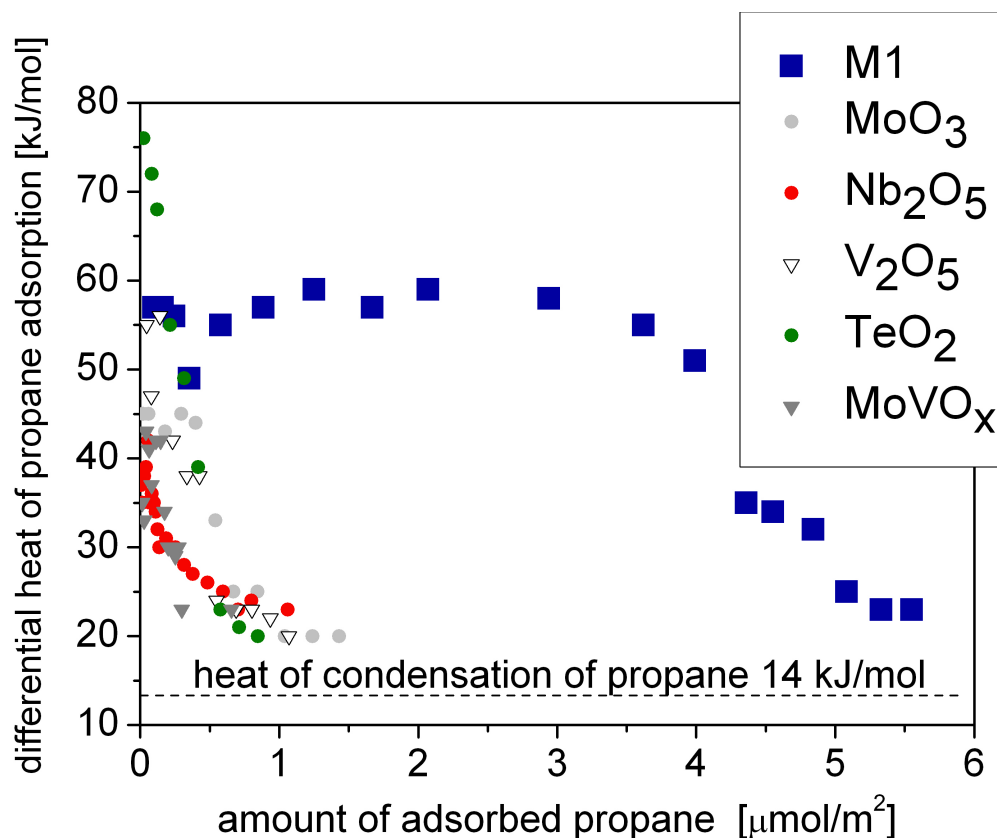
MoVW



(Mo,Nb,V)₅O₁₄

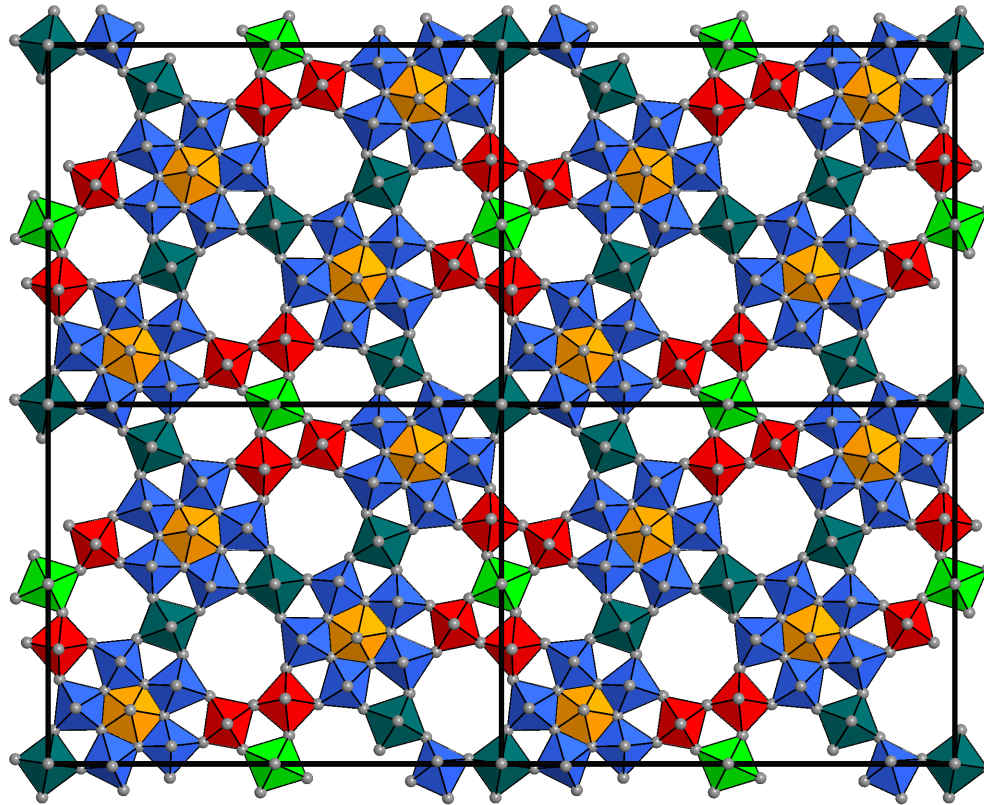


Synergy: adsorption as probe

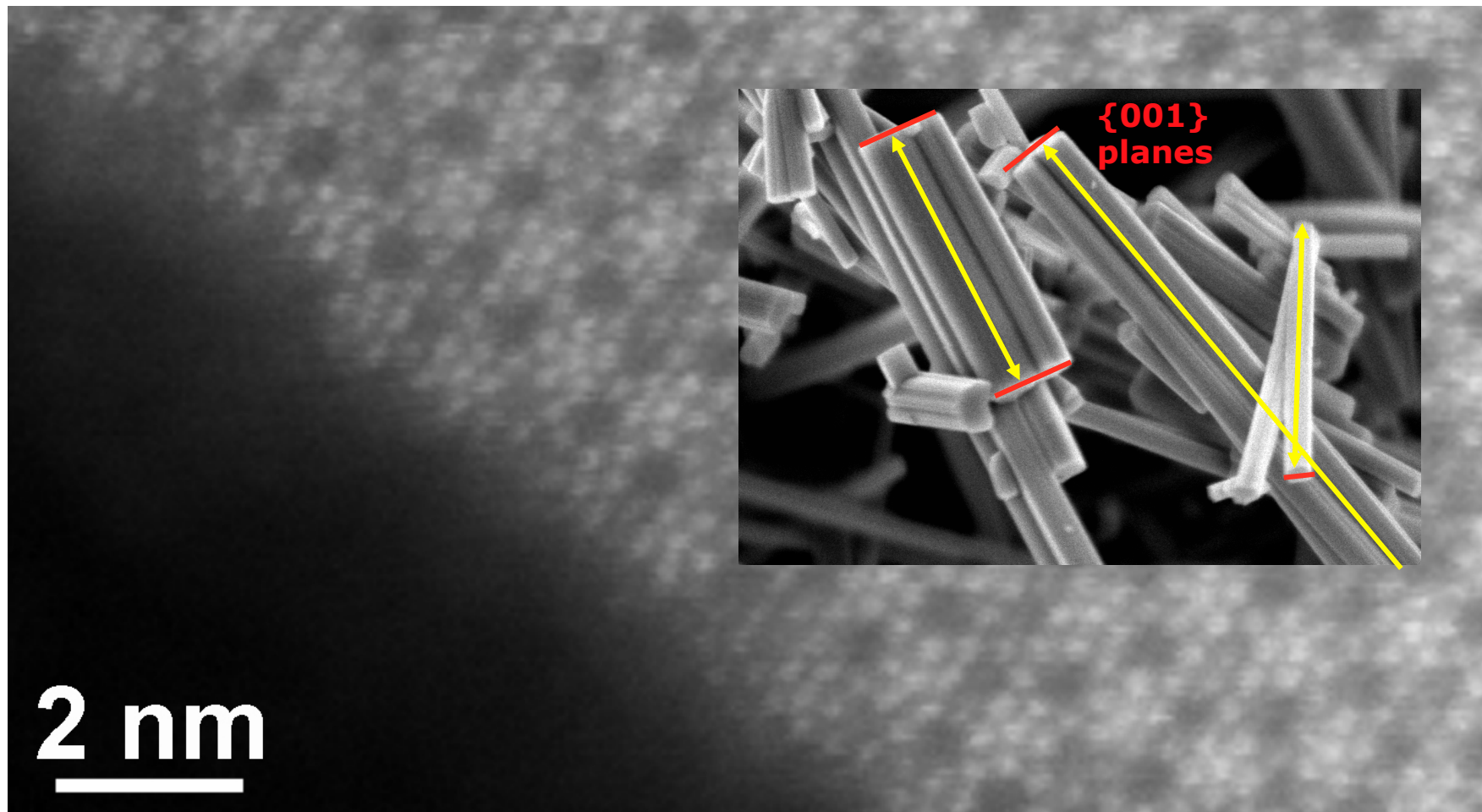


- Propane is strongly adsorbed on tellurium oxide
- High density of energetically homogeneous adsorption sites on M1

Termination of the prismatic faces

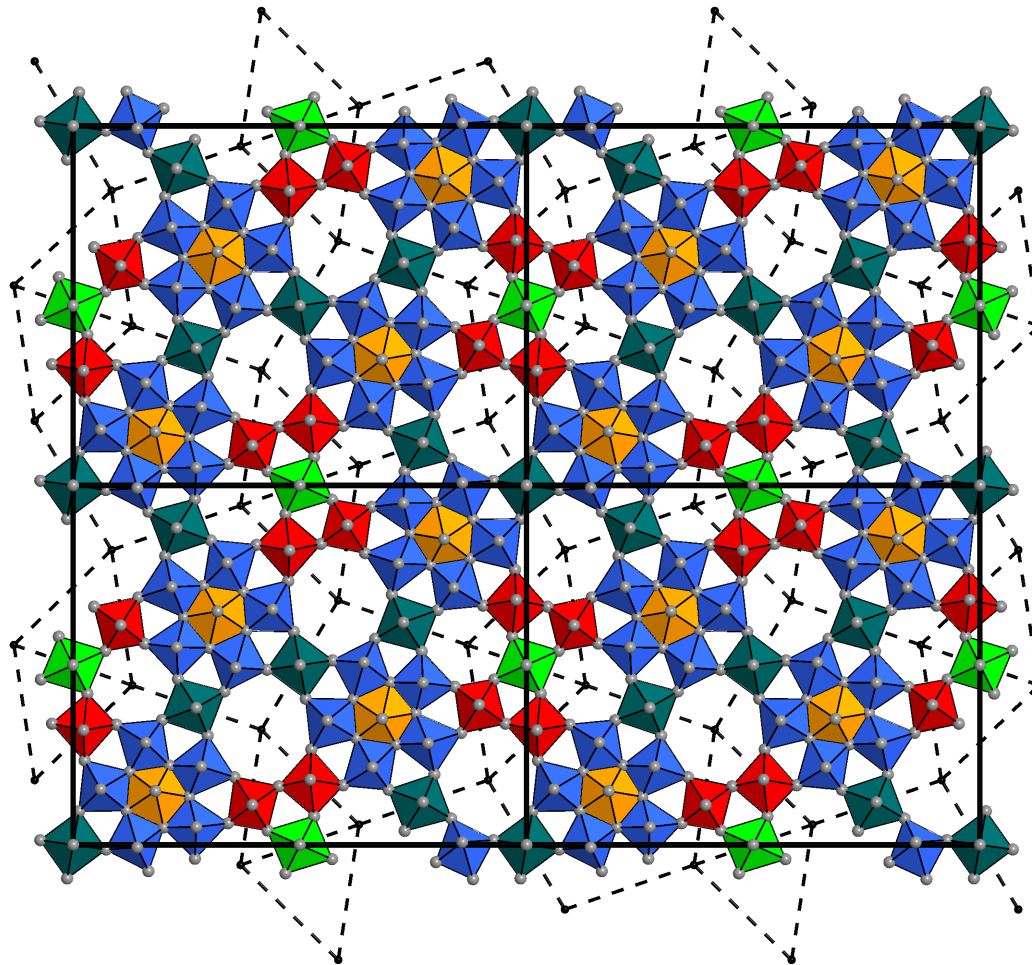


Termination of the prismatic faces



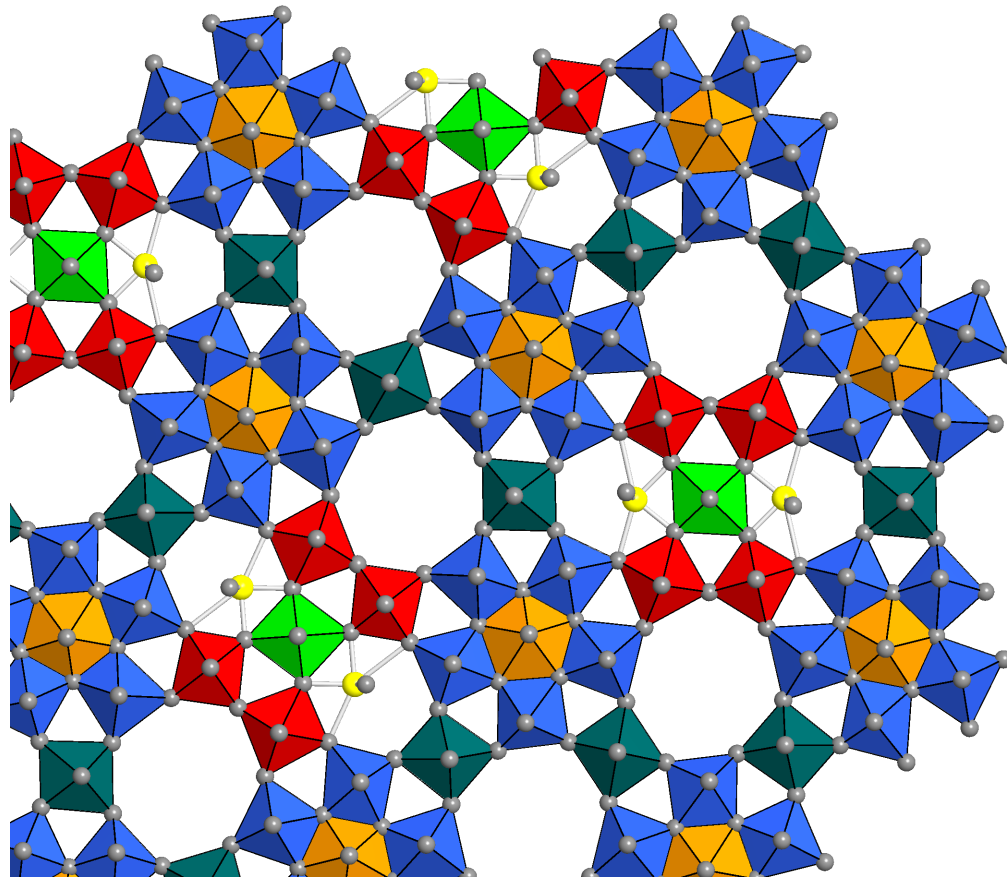
The active site feature

Kinetics of synthesis decides over activity



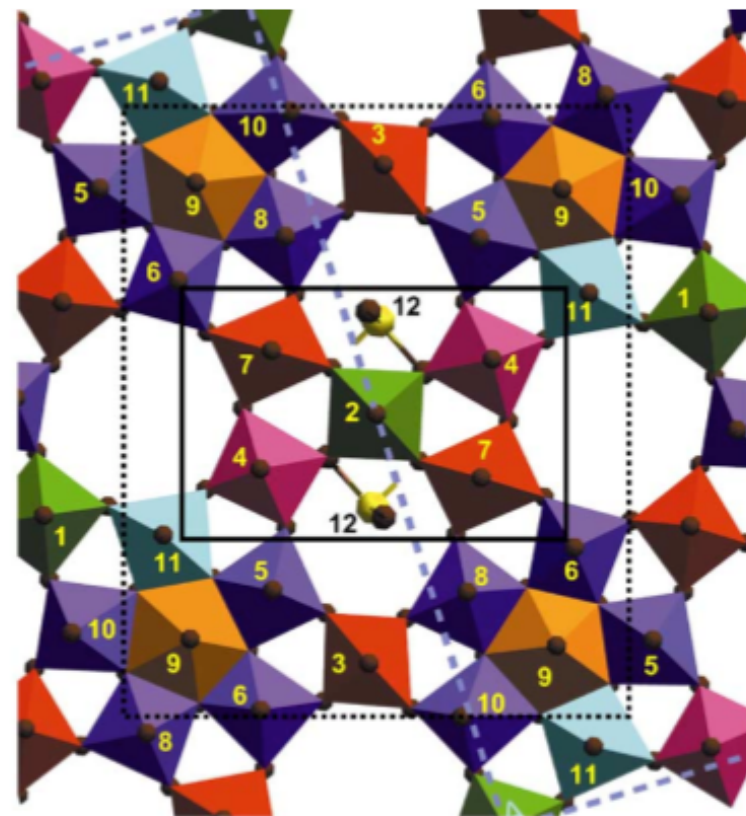
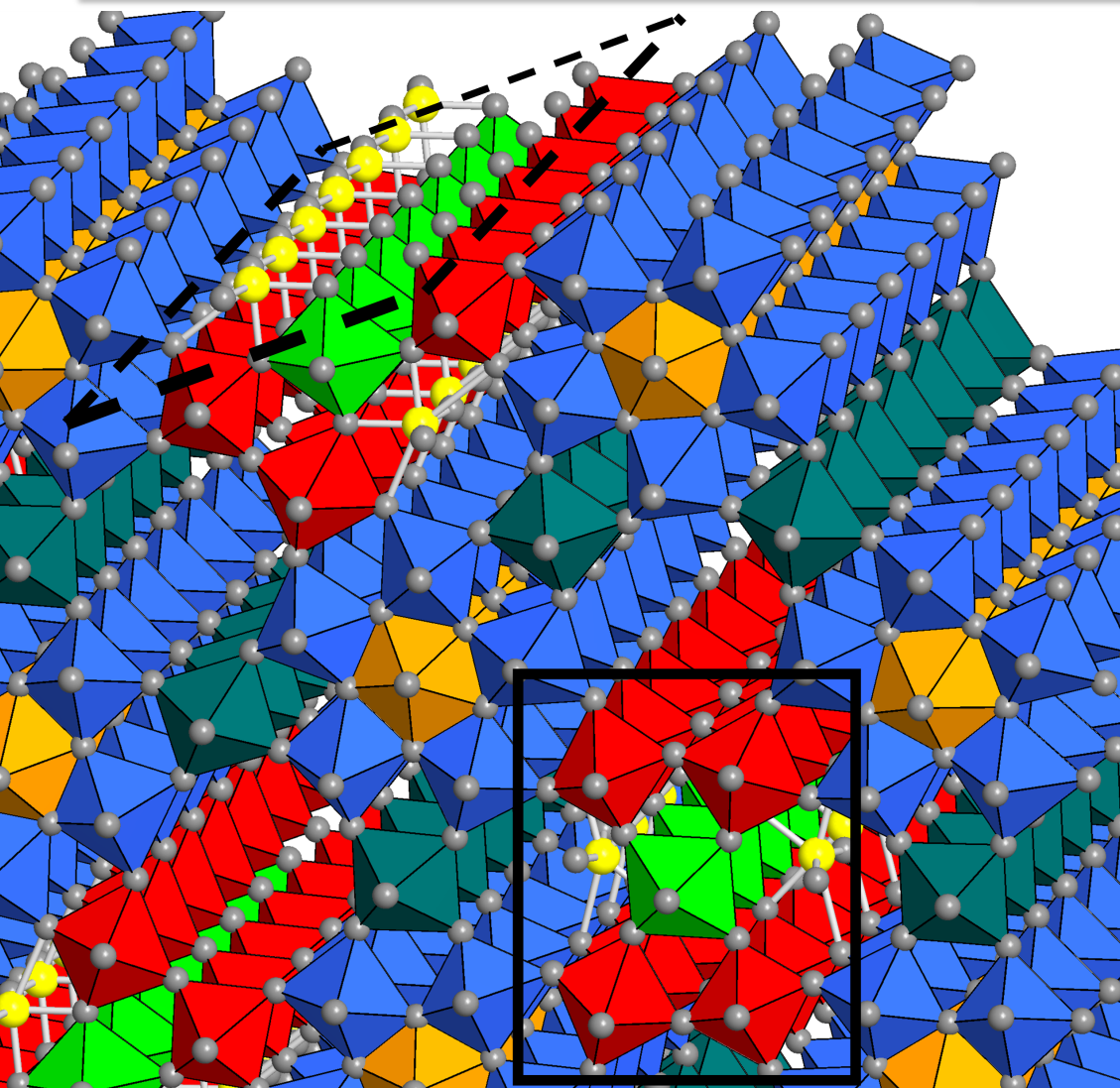
The active site feature

Kinetics of synthesis decides over activity



The active site feature

Kinetics of synthesis decides over activity

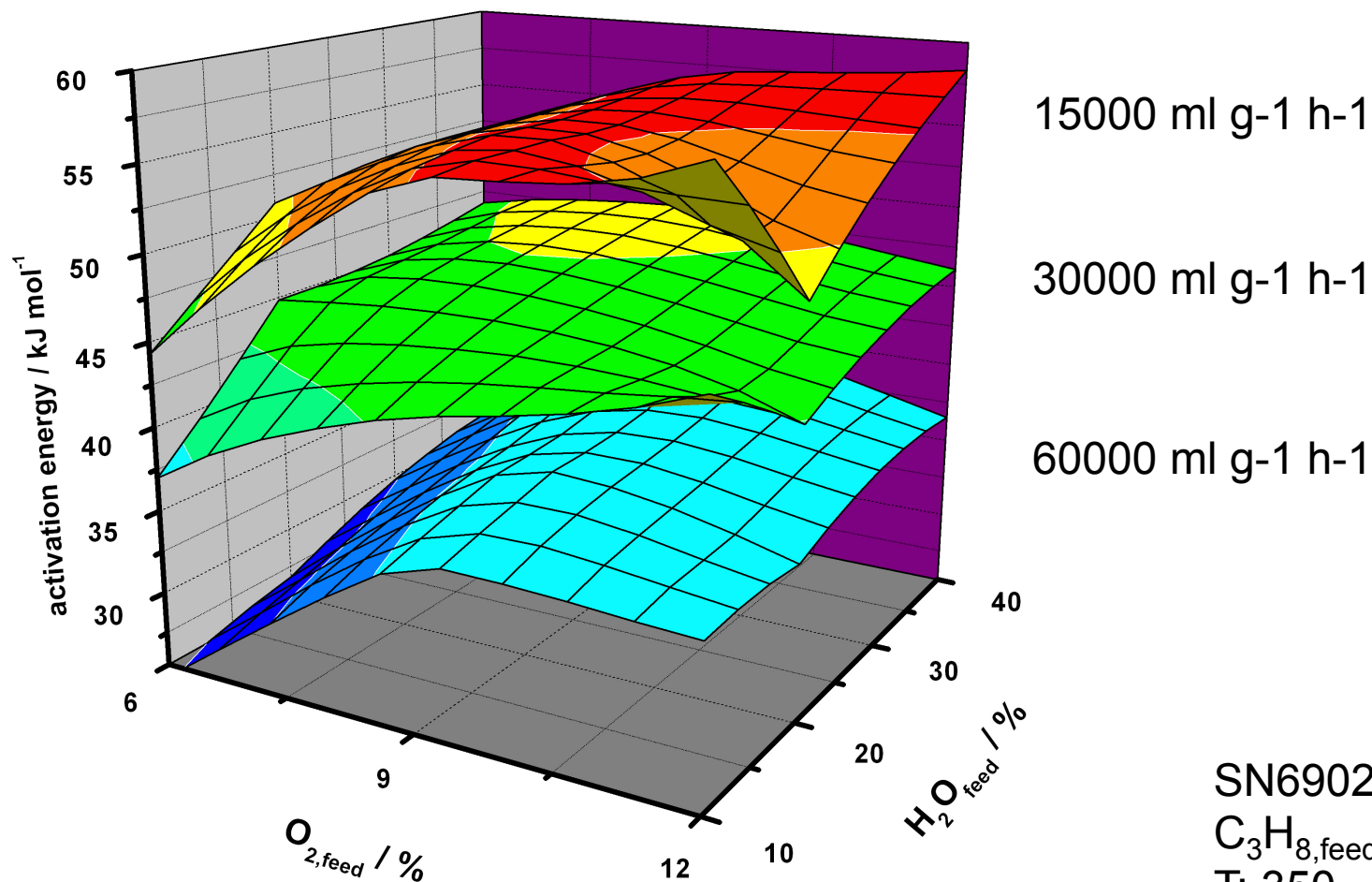


M1: $V^{4+}_{0.26} / Mo^{5+}_{0.74}$	M4: $Mo^{6+}_{0.5} / Mo^{5+}_{0.5}$	M9: $Nb^{5+}_{1.0}$
M2: $V^{4+}_{0.62} / Mo^{5+}_{0.38}$	M5, 6, 8, 10: $Mo^{6+}_{1.0}$	M11: $Mo^{5+}_{1.0}$
M3: $V^{5+}_{0.42} / Mo^{6+}_{0.58}$	M7: $V^{5+}_{0.32} / Mo^{6+}_{0.68}$	M12: $Te^{4+}_{0.94}$

- Catalysts terminate different from their bulk.
- Termination controlled by (chemical) nanostructure.
- A low-dimensional active structure with fast kinetics of structural transformation: dynamics
- Allowing facile reaction with reactants: “activation”.
- Suitable for adaptive active sites.
- Difficult to detect at low performance condition of typical analysis.
- Stable systems are not dynamical and thus not active in suitable times: activity and stability are counteracting!

Dynamics vs stability

Activation energy for propane consumption

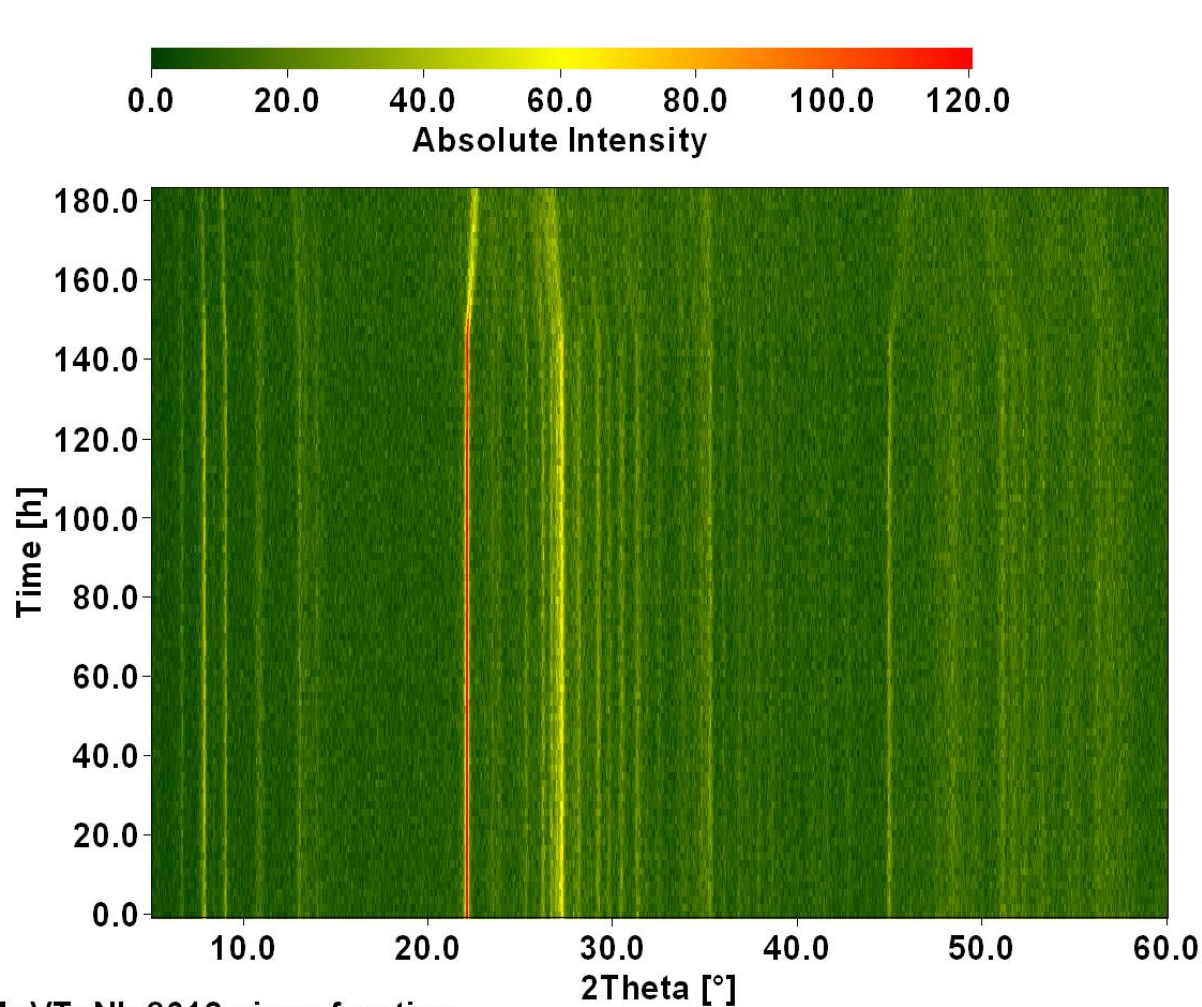


SN6902

C₃H_{8,feed}: 3 %

T: 350 - 390°C

Dynamics vs stability



H₂O / O₂ / propane

0 / 0 / 3

5 / 0 / 3

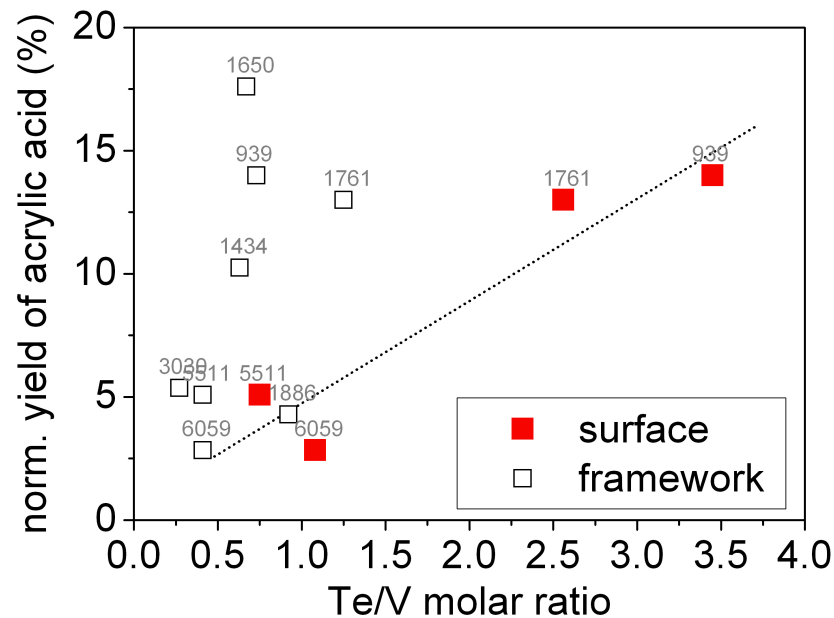
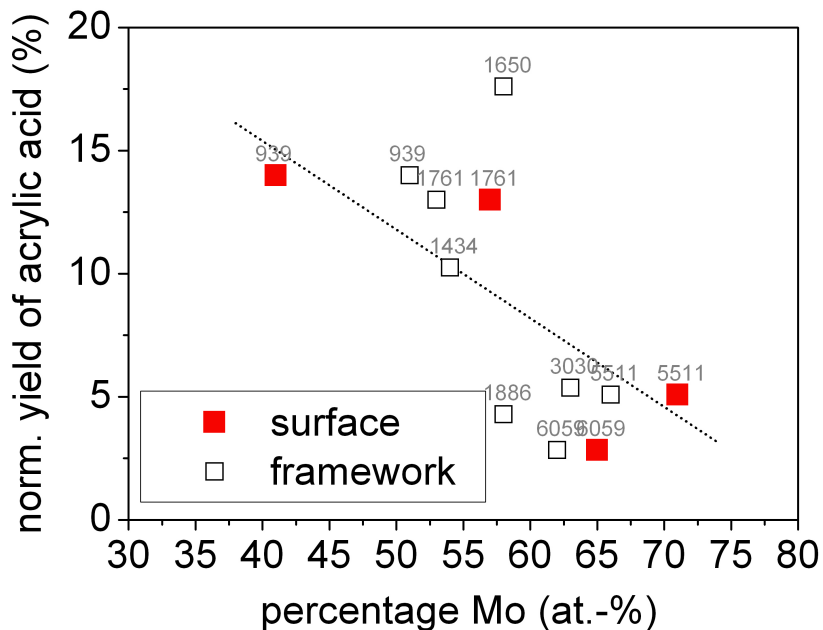
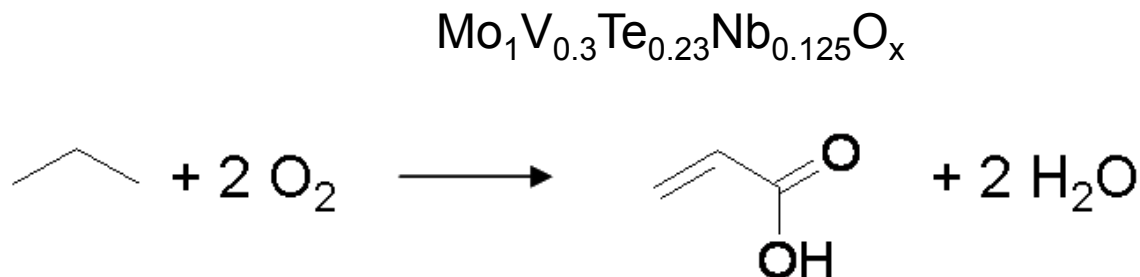
5 / 12 / 3

0 / 12 / 3

MoVTaNb 8612 sieve fraction

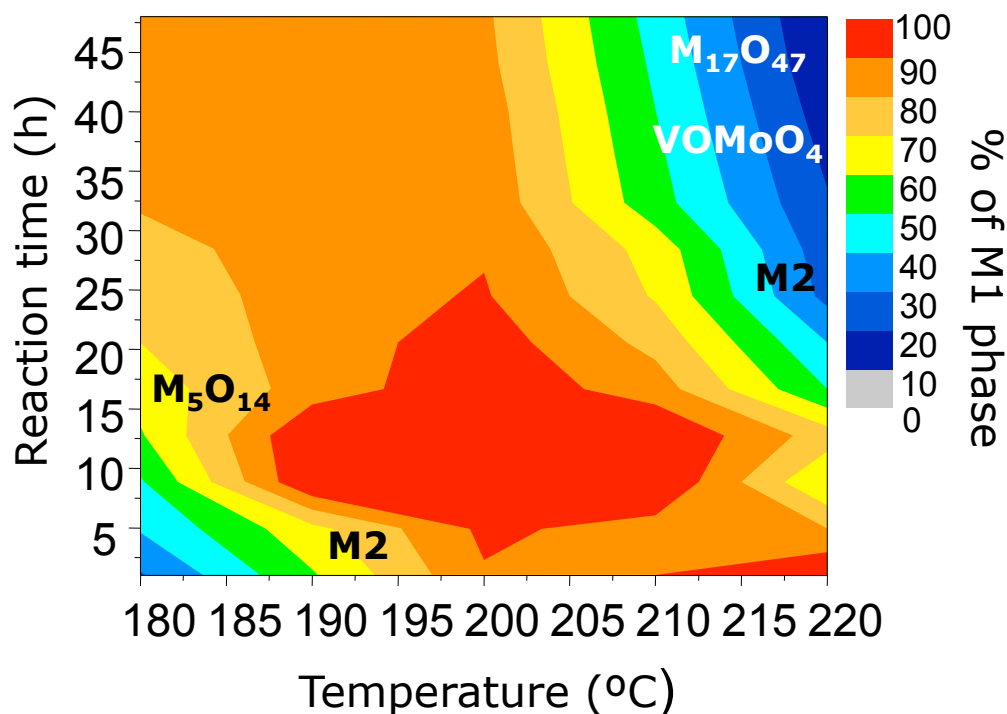
GHSV=5000h⁻¹
T=673K

A dynamical oxide



Synthesis of a complex catalyst catalysis by itself?

Nominal stoichiometry: $\text{MoV}_{0,25}\text{Te}_{0,23}\text{Nb}_{0,124}$

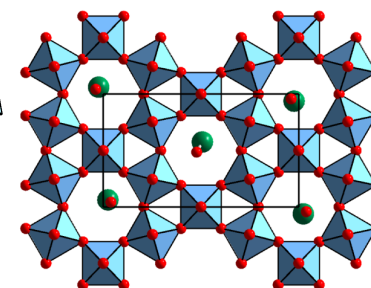
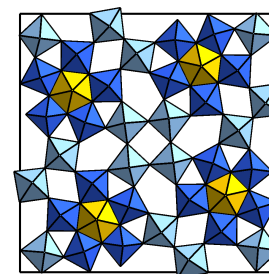


Secondary phases

Intermediates

M_5O_{14}

M_2

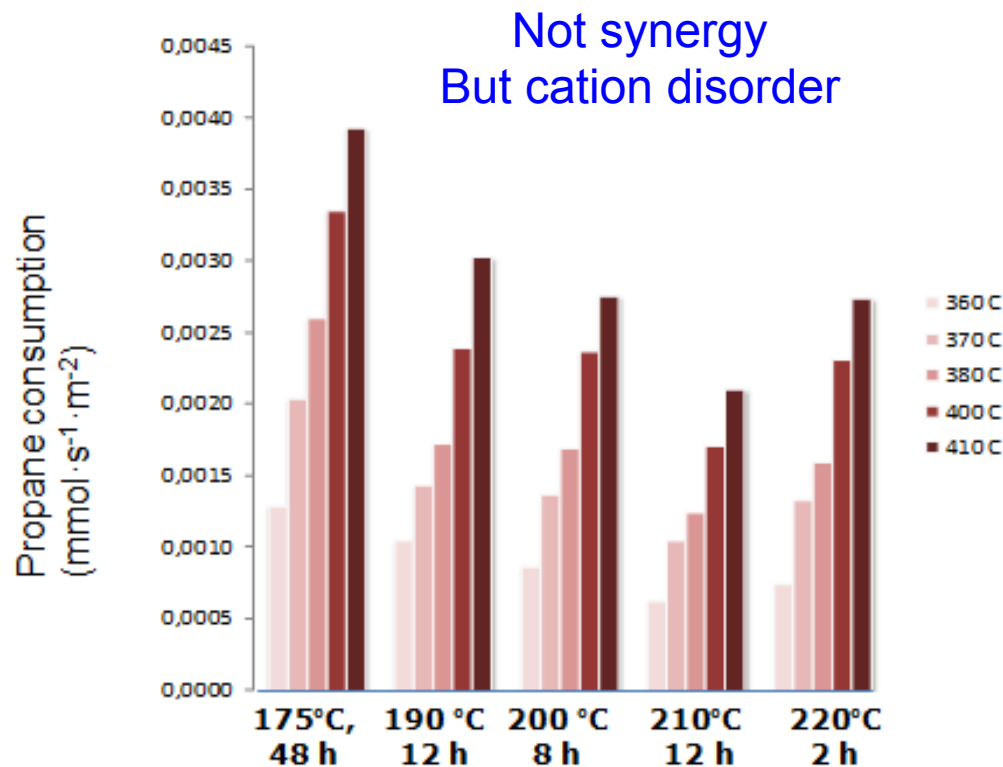


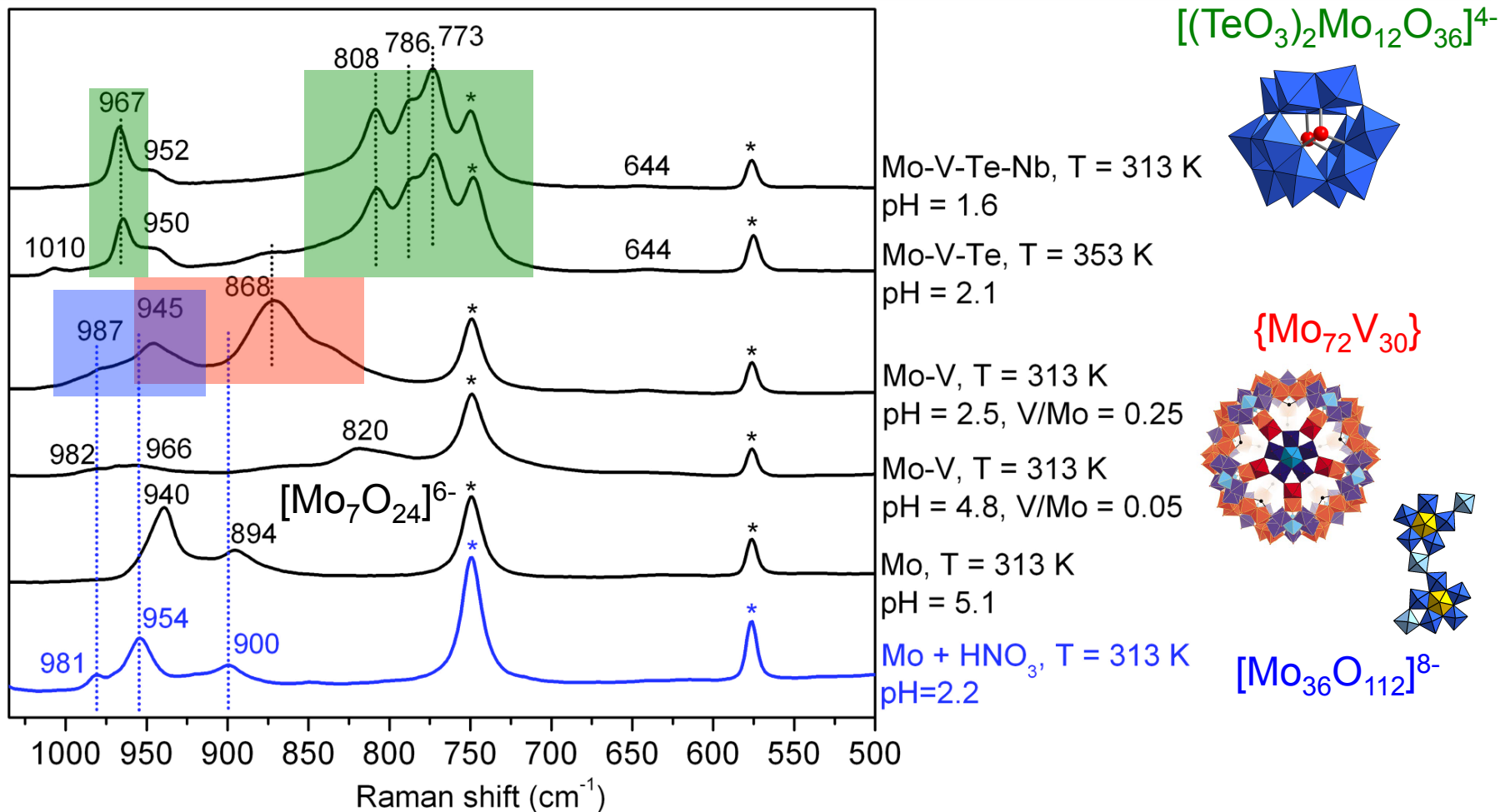
decomposition products

$\text{M}_{17}\text{O}_{47}$, VOMoO_4 , M_2

- At higher T and longer reaction times, thermodynamically favoured products are formed
- Optimum conditions: 190-200°C, 6-12 h
- At lower T and much longer times still better catalysts.

Synthesis of a complex catalyst catalysis by itself?

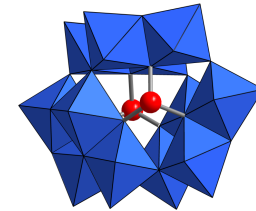
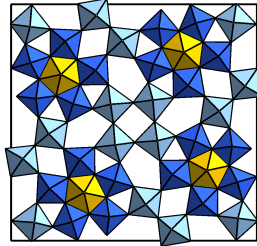




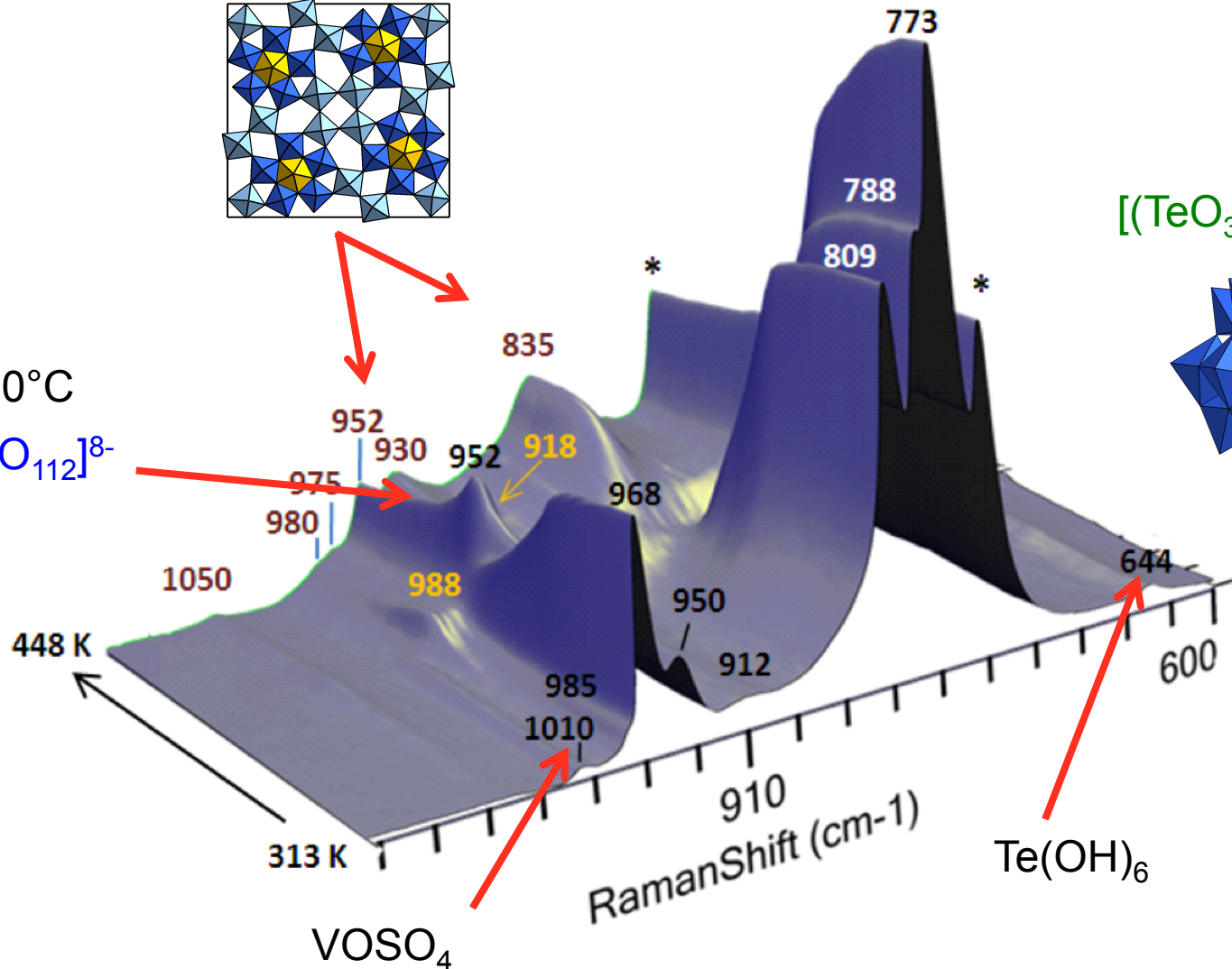
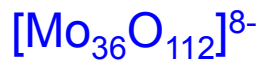
- Initially formed (M)M5 building blocks are decomposed by reaction with tellurium

Destruction-reconstruction during heating: where is the active phase?

M_5O_{14} intermediate



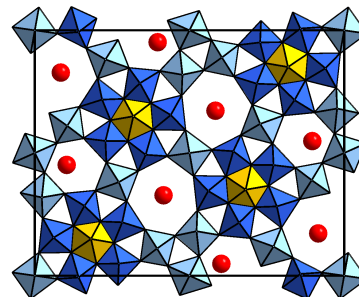
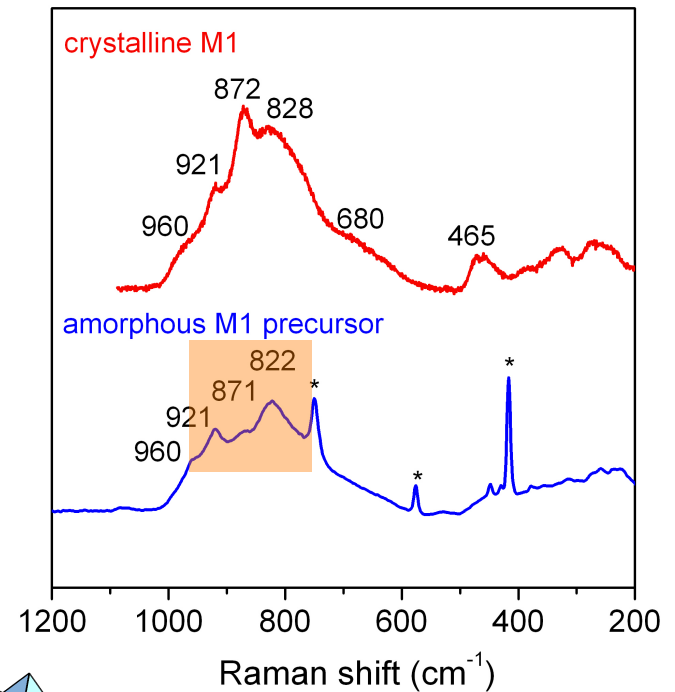
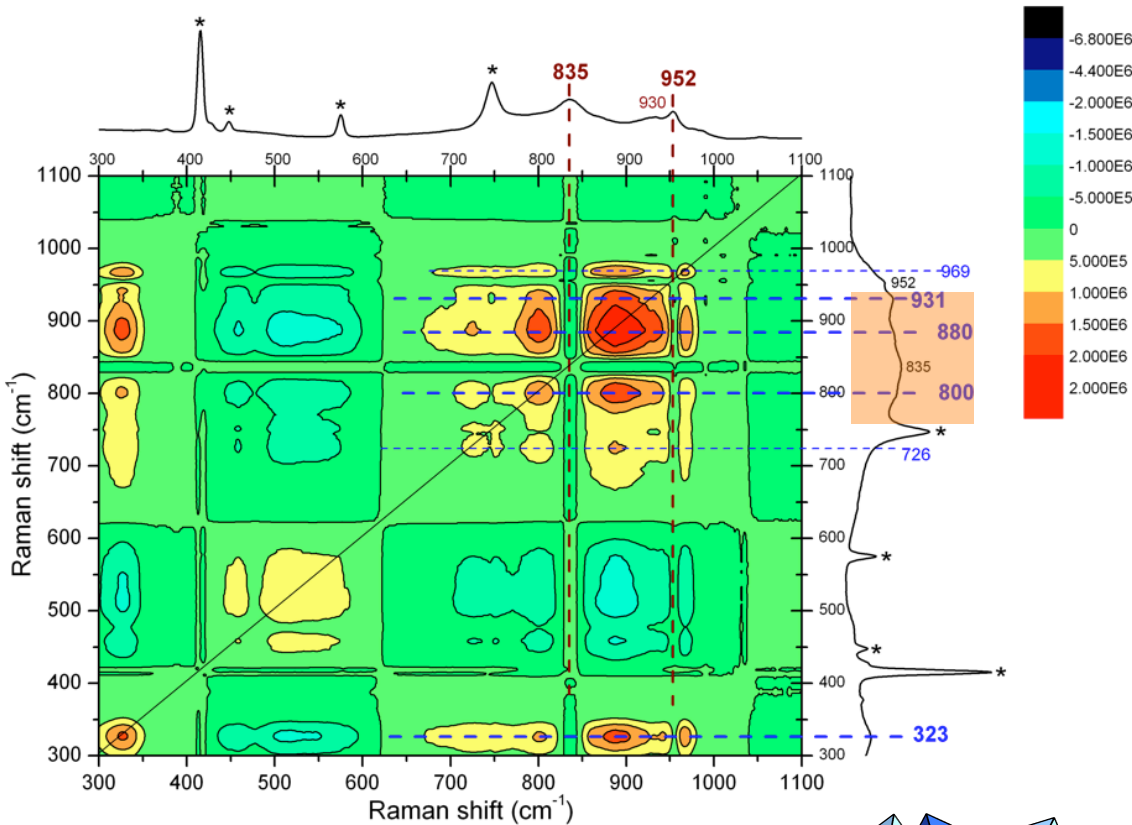
$T > 120^\circ C$

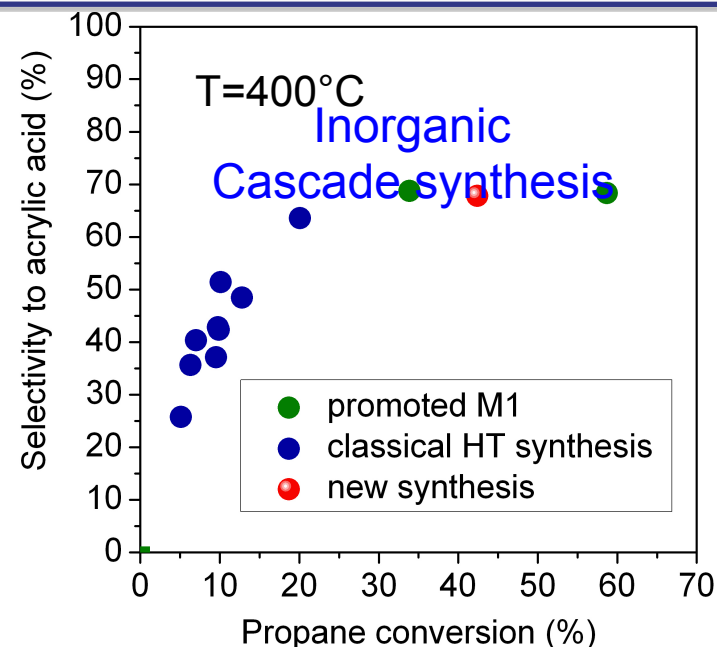
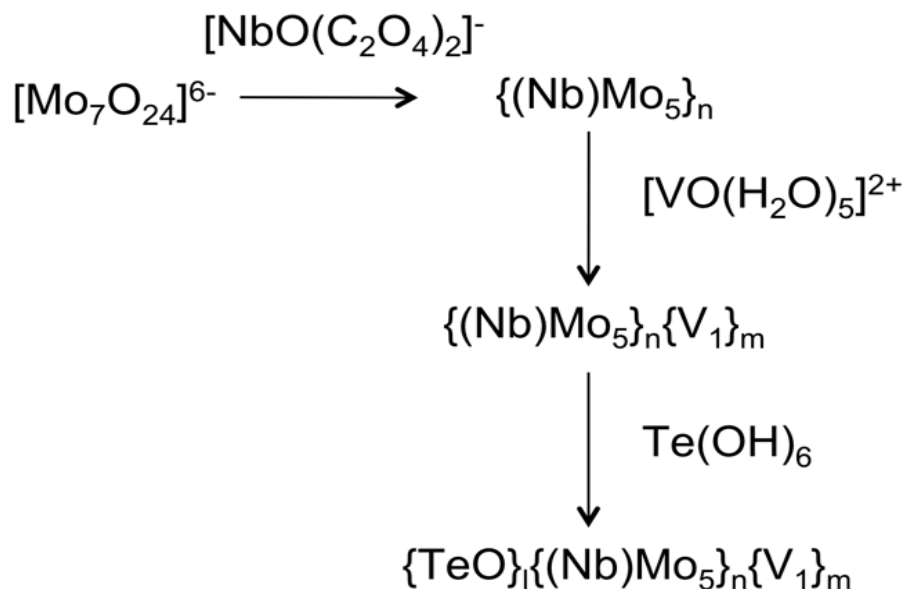


$VOSO_4$

$Te(OH)_6$

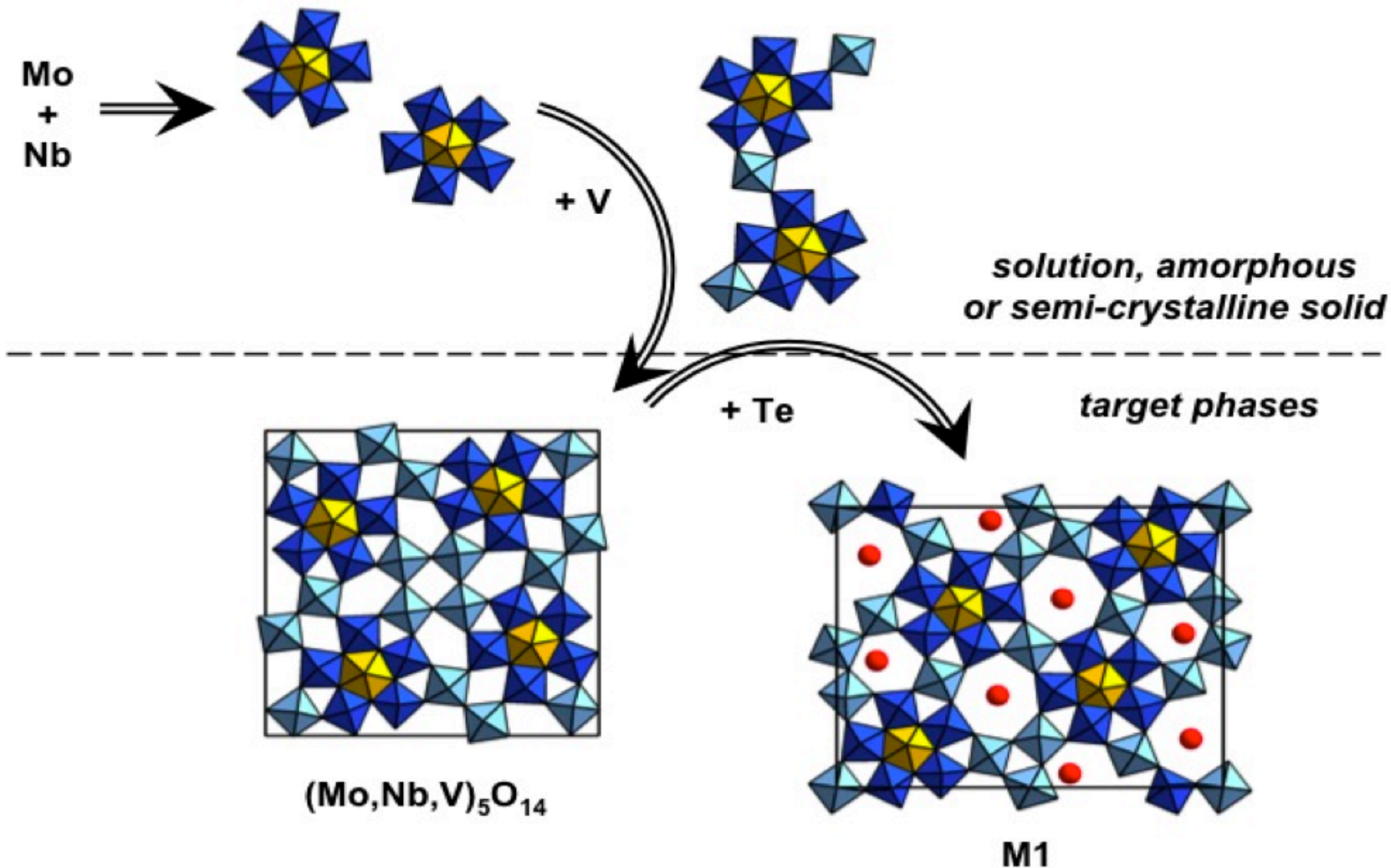
The active sites grow during ageing: cation distribution





	Classical M1 synthesis (catalyst ID 11811) T=190°C t = 12 h	Novel, step-wise M1 synthesis (catalyst ID 12639) T=175°C t = 2 h
Formulation normalized to Mo (XRF)	MoV _{0.228} Te _{0.267} Nb _{0.318}	MoV _{0.207} Te _{0.180} Nb _{0.207}
S _{BET} [m ² /g]	1.5	4.7
E _a [kJ/mol]	72	55
Space time yield [mg _{aa} /g _{cat} h] at 673 K	9.3	48.8 50

The practical use of the synthesis knowledge rational design



- Oxides are highly versatile catalysts for a variety of reaction families.
- They exhibit complex terminations, “simple” oxides terminate often passivated.
- High performing systems exhibit a “monolayer” active phase stabilized by a bulk withstanding the chemical potential of the reaction environment.
- Semiconducting properties relevant.
- This causes complex crystal structures to be functional, also as storage phase for the active component.

Dem Anwenden muss das Erkennen vorausgehen

Max Planck



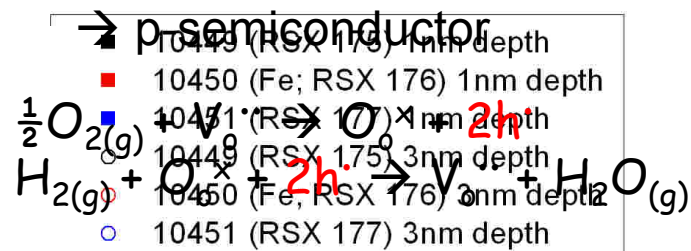
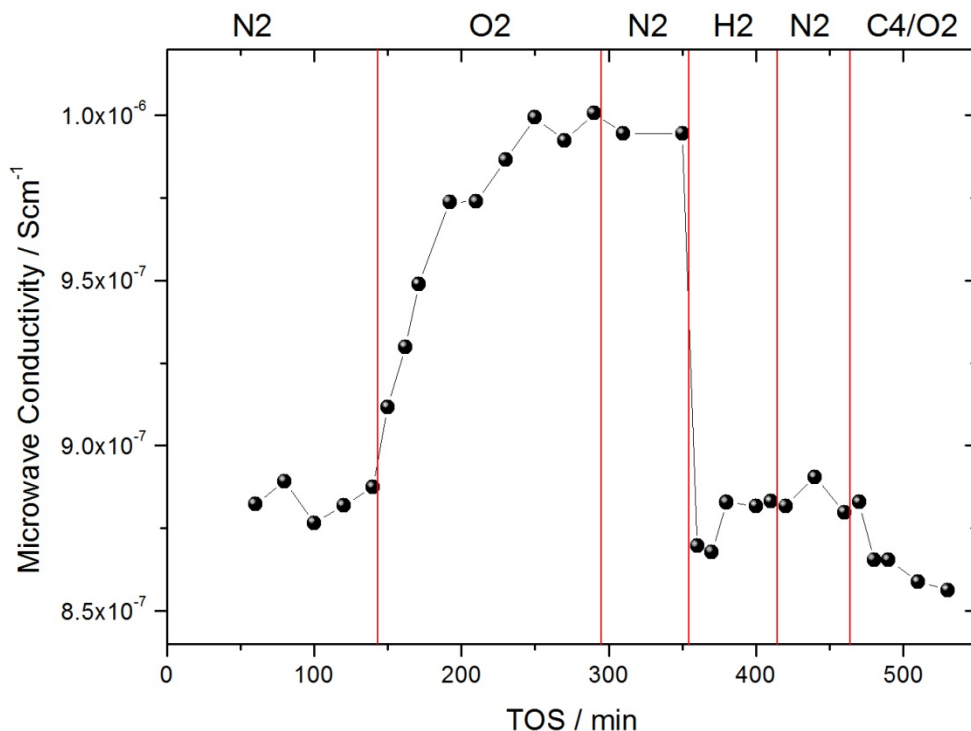
Thank You

VPP in MA synthesis: well-known here active species across pressure gap

www.fhi-berlin.mpg.de

GHSV: 3540 h⁻¹; N₂: 100% N₂; O₂: 20% O₂; H₂: 14% H₂; C₄/O₂: 2% n-butane, 20% O₂; residual gas always N₂; 0.5-1 mm split

12829 (RSX 600)



AP-PES

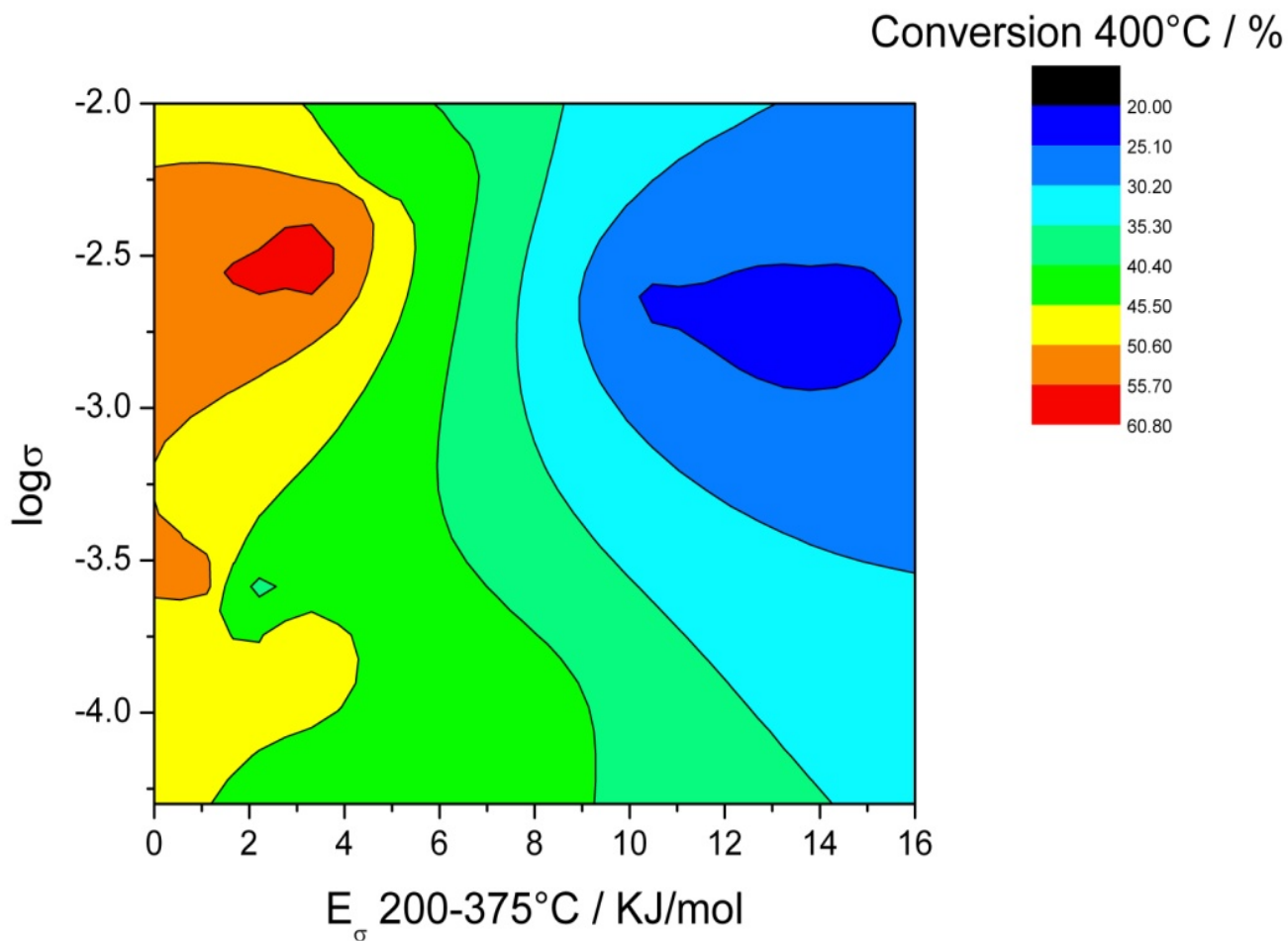
Strong variation of the
“oxidation state” (surface
structure) with chemical
potential.

But only in the top few nm

How at atmospheric
pressure with surface
sensitivity?

Contactless microwave frequency perturbation

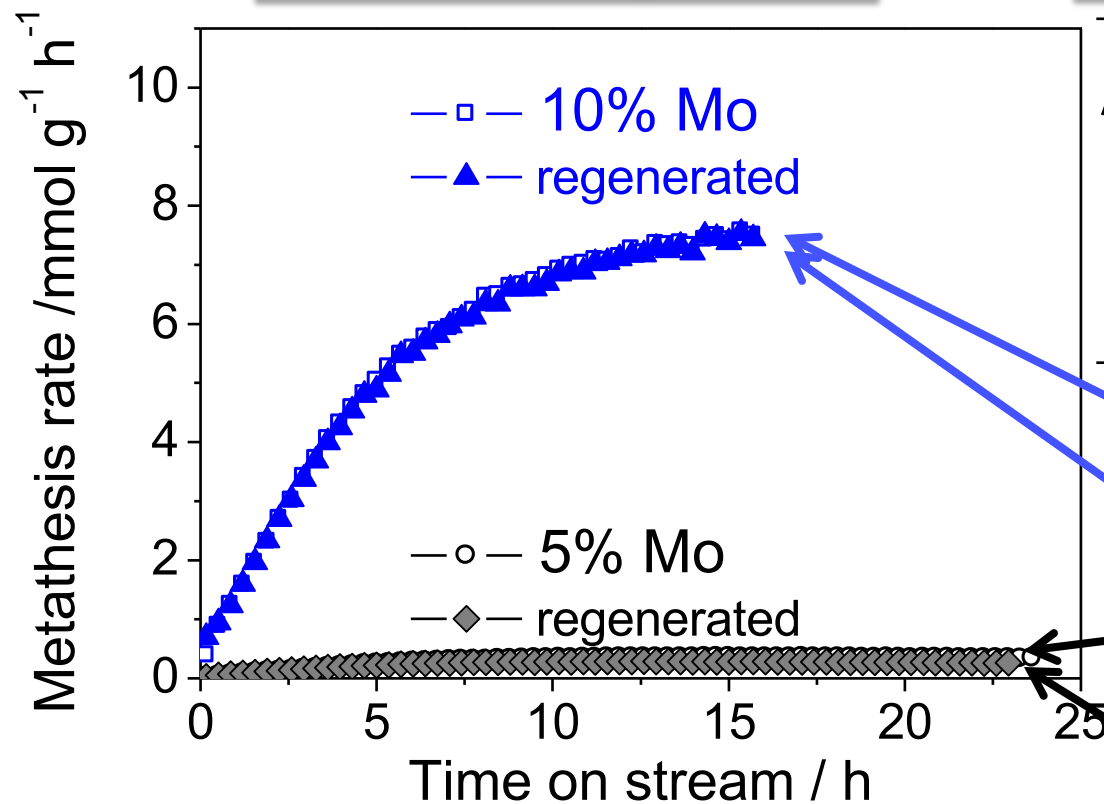
Physics of site isolation correlation to performance



Few sites are highly active

Activity of MoO_x/SBA-15

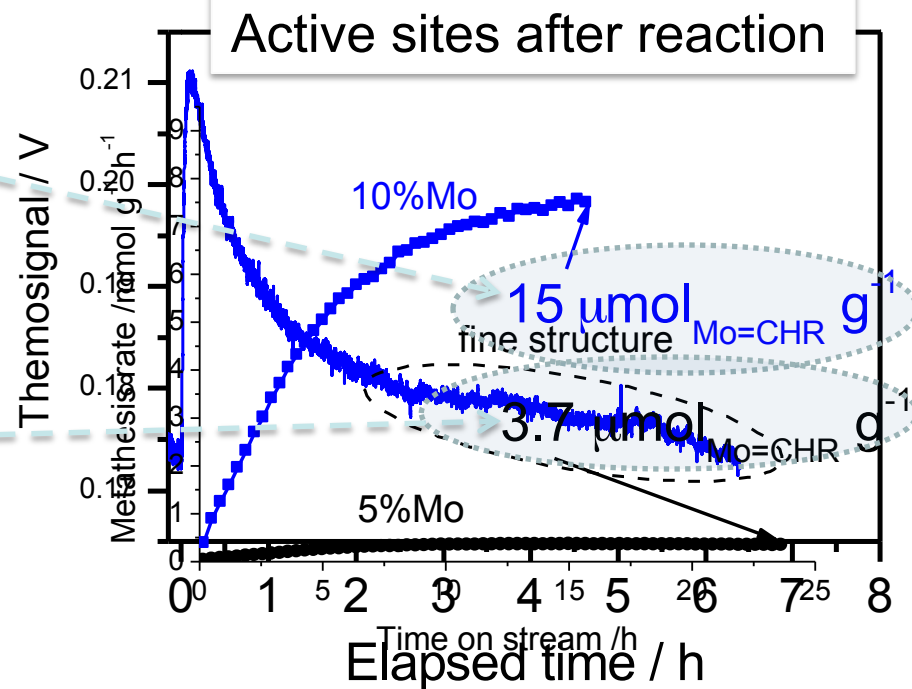
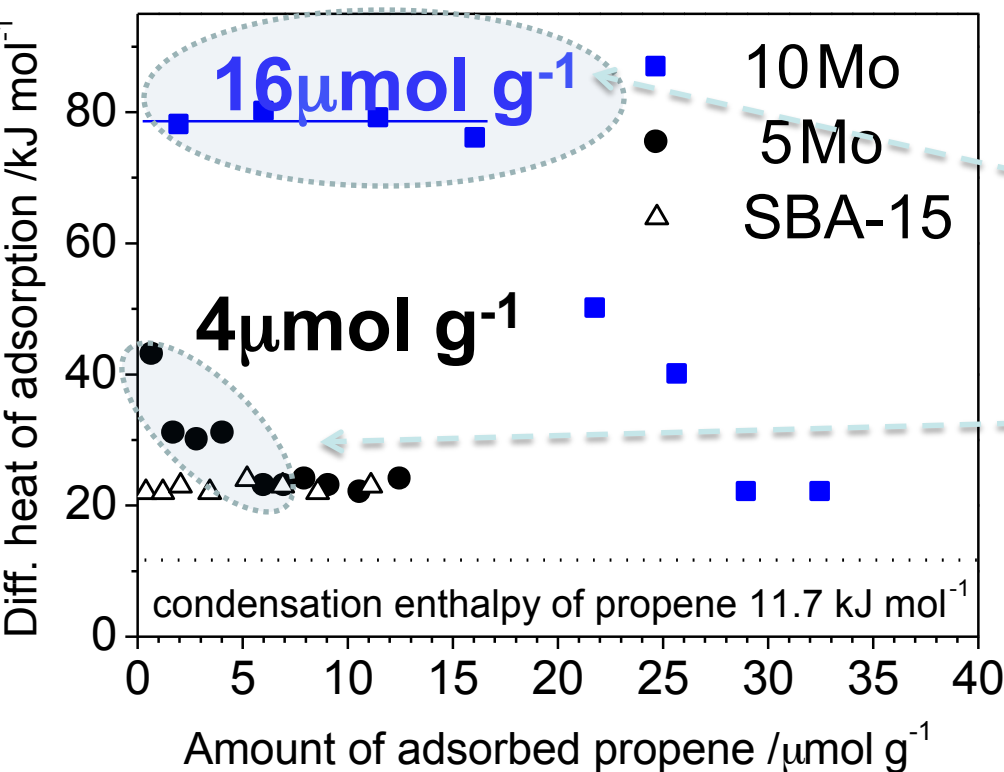
post-reaction carbene titration



Active site density ($\mu\text{mol g}^{-1}$)	Active site fraction (atom-%)	Intrinsic activity (h^{-1})
15	1.5	500
14	1.4	530
3.7	0.7	90
2.2	0.4	120

Activity not proportional to loading: structural variations

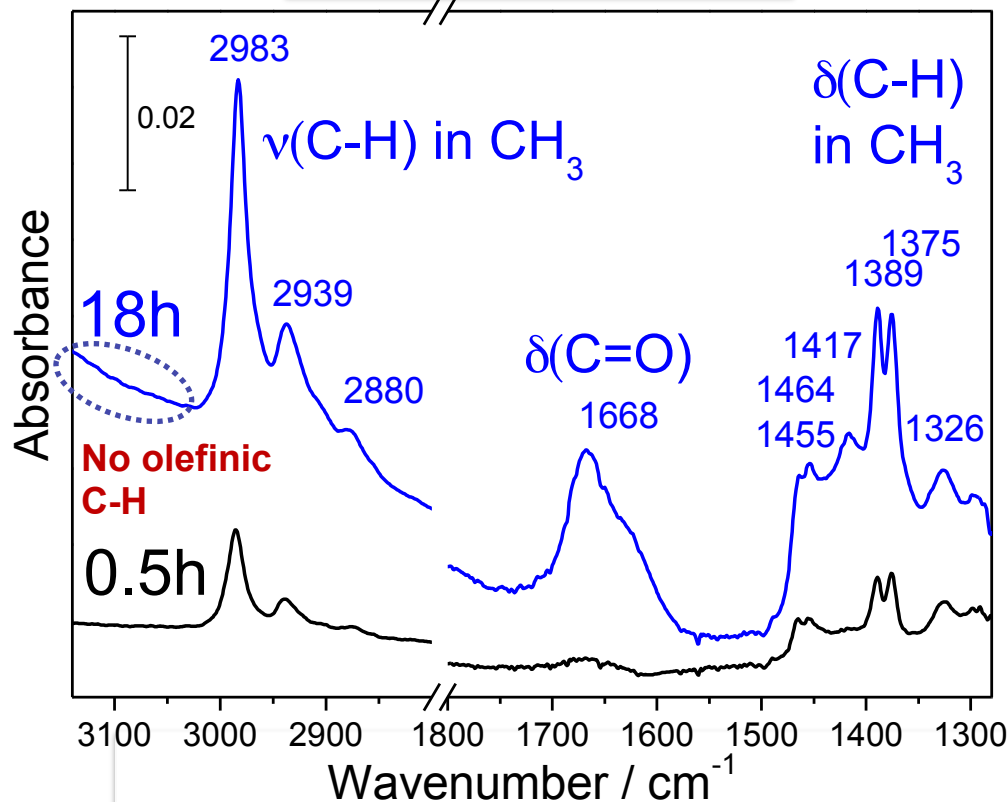
C₃H₆ Calorimetry



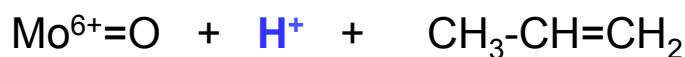
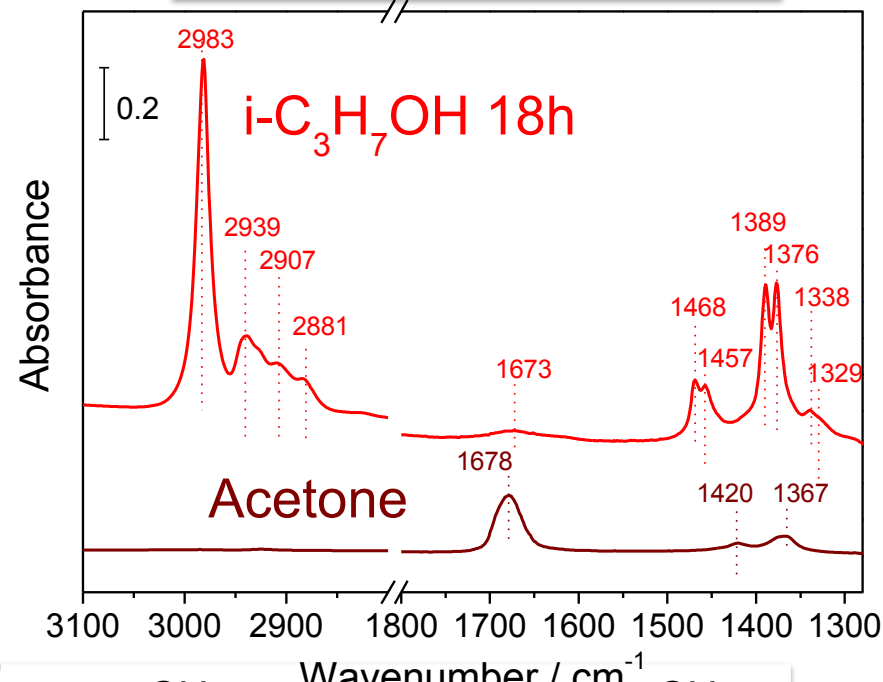
The site densities of strong and irreversible adsorption coincide with the carbene site densities measured by the post-reaction titration.

In-situ formation of active species: selective oxidation

Propene (3 hPa, 323K)



Reference : i-C₃H₇OH, C₃H₆O



Brønsted acid

