

Mo-V-Te-Nb-O mixed metal oxides – "diluted" and "undiluted"- prepared by Hydrothermal Synthesis for selective oxidation of propane to acrylic acid

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Introduction

- The selective oxidation of propane to acrylic acid has provoked a great interest due to the economical and environmental advantages.
- Nowadays the best catalyst for this reaction is the $Mo_1-V_{0.33}-Te_{0.23}-Nb_{0.125}-O$ mixed metal oxide developed by Mitsubishi Chemicals.
- Application of Hydrothermal Synthesis instead of the conventional method, "Slurry method", has the advantage of producing a material with higher crystallinity.
 - Preparation method as well as activation conditions are crucial for the catalytic performance.

<u>Objetives</u>

• type and concentration of Mo-starting material

Investigation of the influence of preparation

• addition of diluent



Experimental

Preparation of slurry-precursor



- AHM, VOSO₄, Te (OH)₆, C₁₀H₈N₂O₃₃Nb₂
- $Mo_1-V_{0.33}-Te_{0.23}-Nb_{0.125}$ / $Mo_1-V_{0.25}-Te_{0.13}-Nb_{0.124}$
- \bullet T_{synthesis} = 80°C
- diluent: Aerosil 300



• P = 13 bar

• T = 175 °C

• t _{synthesis} = 48 h

Hydrothermal Synthesis

Activation (heat treatment)



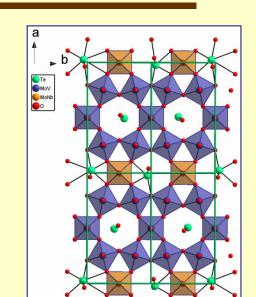
- calcination (air, T = 275 or 325°C)
- heat treatment (N₂, T = 600 or 650°C)

Structure

M1 phase (Ushikubo)¹⁾

parameters on structure and morphology of the materials

 $Te_2M_{20}O_{57}$ (M = Mo, V, Nb) = $Mo_{7.8}V_{1.2}NbTe_{0.937}O_{29.9}$



M2 phase (Ushikubo)¹⁾

 $Te_{0.33}MO_3 (M = Mo, V, Nb) = Mo_{4.31}Te_{1.81}V_{1.36}Nb_{0.33}O_{19.81}$

Present working hypotheses:

- □ M1 is the active phase²⁾
- □ phase cooperation between M1 and M2³)

Results

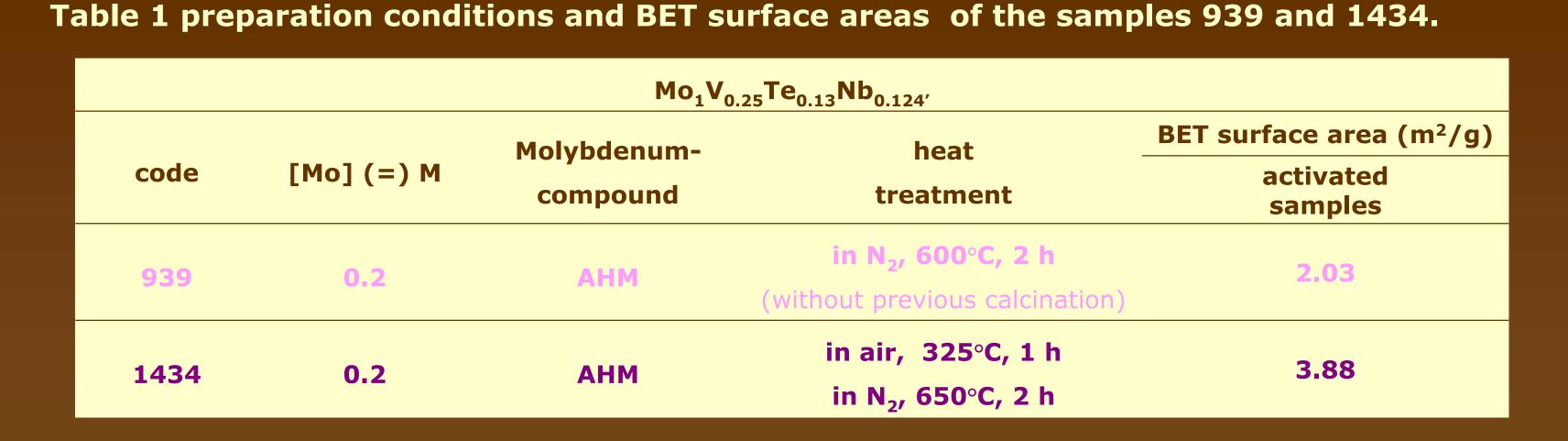
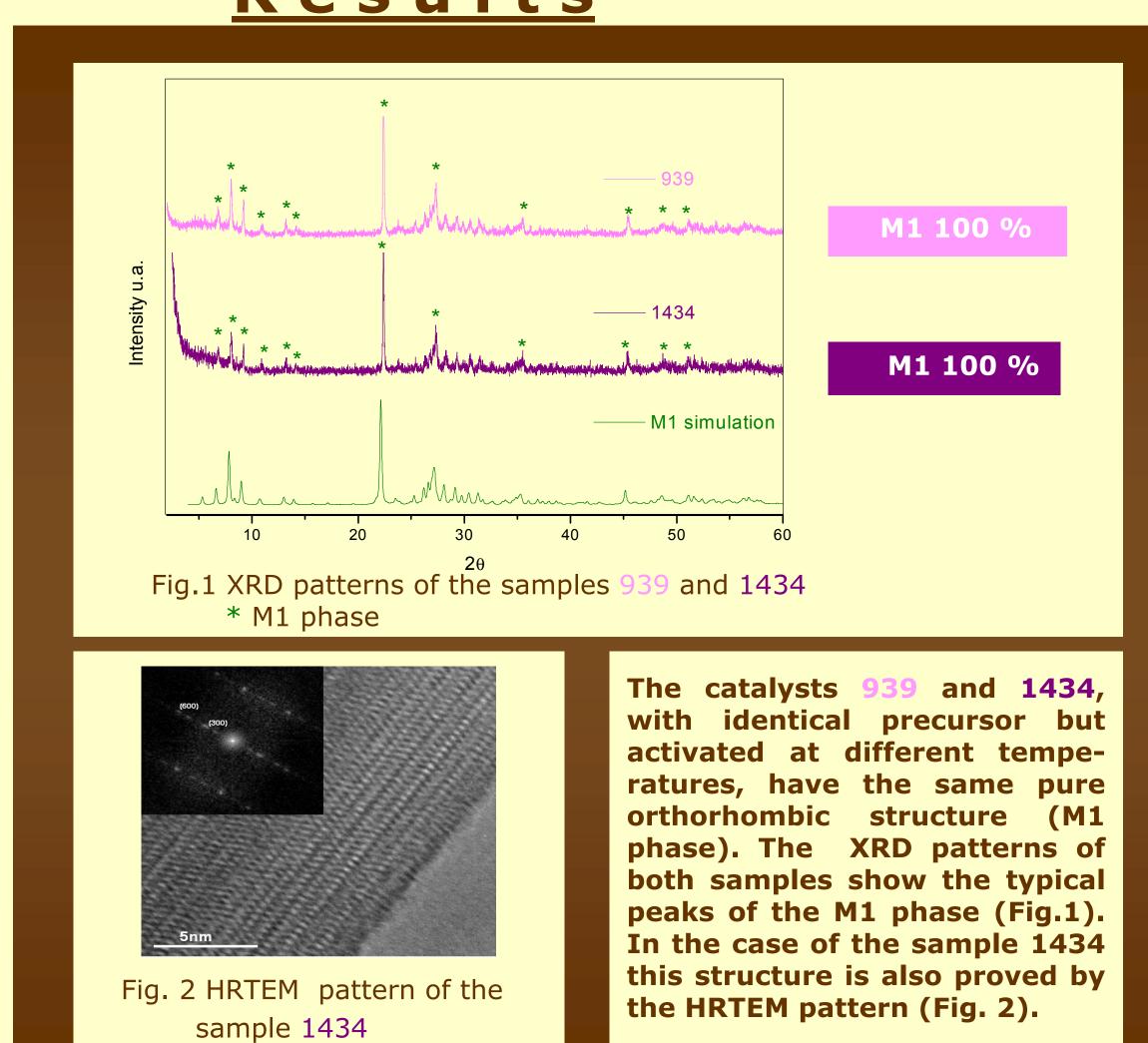


Table 2 preparation conditions and BET surface areas of the samples 1525, 1464 y 1419.

$Mo_1V_{0.33Te_{0.23}Nb_{0.125}}$									
	[Mo] (=) M	Molybdenum- compound	diluent	BET surface area (m²/g)					
code				no activated	activated				
				samples	samples				
1525	0.2	Mo ₃₆ O ₁₁₂ 8-	-	143.2	11.61				
1464	0.4	АНМ	-	63	5.11				
1419	0.2	AHM	SiO ₂ 300	102.5	96.9				



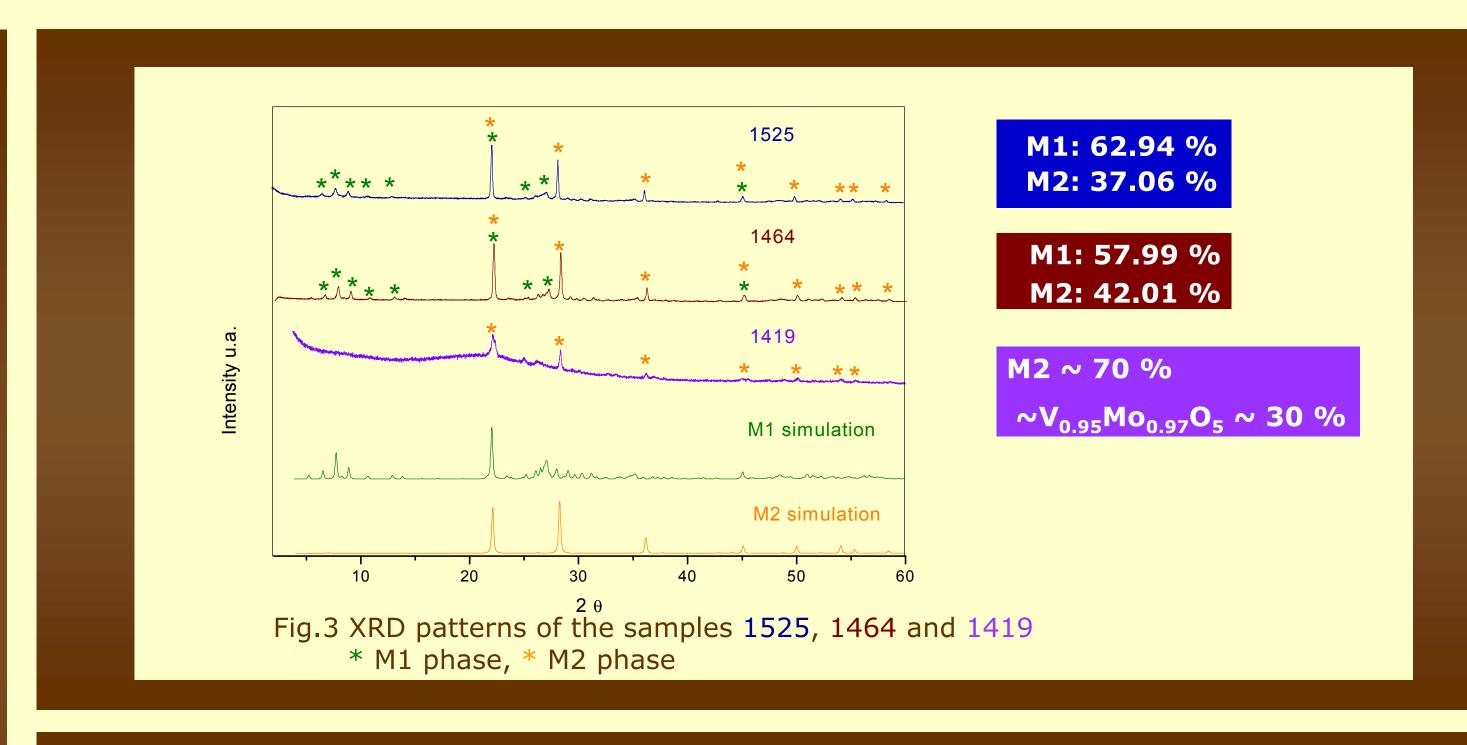


Table 3 catalytic test at 400 °C and GHSV = $1200 h^{-1}$.								
code	C ₃ :O ₂ :N ₂ :steam (% molar)	Хсзна	S _{AA}	Y _{AA}				
1525	0.85:1.9:15.2:12	56	10	6				
1464	0.85:1.9:15.2:12	61	47	29				
1419	0.85:1.9:15.2:12	11	55	6				
939	0.85:1.9:15.2:12	38	73	28				
1434	0.85:1.9:15.2:12	52	79	41				

Conclusions

- Pure orthorhombic structure (M1 phase) has been formed in the case of the catalysts with stoichiometry $Mo_1V_{0.25}Te_{0.13}Nb_{0.124}$, independently of the different temperatures of the heat treatment (600 or 650°C).

- The heat treatment of the samples has a big influence on their catalytic activity. For catalysts identically synthesized (939, 1434), the one activated at higher temperature shows higher catalytic performance.
- With different preparative parameters (Mo₃₆O₁₁₂8- as starting molybdenum-compound, higher metal concentrations, addition of a diluent) the BET surface area of the activated samples increases but a mixture of M1 and M2 phase (pseudo-hexagonal structure) is formed instead of the pure M1 phase.

¹⁾ T. Ushikubo, K. Oshima, A. Kayou, M. Hatano, Stud. Surf. Sci. Catal. 112 (1997) 473.

²⁾ D. Vitry, Y. Morikawa, J. L. Dubois, W. Ueda, Applied Catalysis A: General 251 (2003) 411-424

³⁾ Robert K. Grasselli, Topics in Catalysis Vol.23 nos 1-4 2003