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In Situ Vibrational Spectroscopy of Reactants and Probe Molecules on Oxide Catalysts

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CECAM WORKSHOP In situ atomic scale characterization of surfaces under high pressures: recent advances in experiment and theory

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- 1. Introduction and classical probe molecule spectroscopy Sites and probe molecules, vibrational spectroscopy
- 2. Developments

Selection of probe, band intensity, band shape

- 3. Reactive probing: kinetics of a model reaction H_2 activation on Ag/SiO₂
- 4. In situ diffuse reflectance infrared spectroscopy (DRIFTS) Initiation of *n*-butane isomerization on sulfated zirconia catalysts





Goal: Identify nature of active surface sites and reaction mechanism



 structure of "ideal" surface may be analyzed under special circumstances (UHV conditions)



- structure of "real" catalyst difficult to analyze: inhomogeneous & unsuitable for many methods
- information on bulk insufficient to derive surface properties
- ✤ identify surface properties through adsorption



Surface Sites, Probe Molecules & Vibrational Spectroscopy





Select probe according to expected site properties

- ✤ acid site: basic probe (ammonia, pyridine, CO)
- ✤ basic site: acid probe (CO₂, pyrrole)

Many experimental possibilities: IR, DRIFTS, ATR, IRAS, SFG, EELS, Raman

- ✤ sample form: model system (single crystal), powder
- ✤ selection rules
- wide temperature and pressure range



Example: CO Adsorption on SiO₂ at 77 K





The ideal probe molecule...

- selective adsorption on particular site small, non-reactive molecule
- high extinction coefficients of vibrations of interest
- ✤ large variation of vibrational frequency upon adsorption
- ✤ induce large change in vibration frequency of functional group
- H. Knözinger, Handbook of Heterogeneous Catalysis, Wiley-VCh Weinheim 1997, p. 707-732.

Band positions / shifts are analyzed...

- there is more information in an IR spectrum!
 - analyze band position, intensity, shape, and background

Selection of the probe

- we may be wrong about the nature of the "active sites" example: sulfated zirconia is most likely not highly active in *n*-butane isomerization due to its acidic properties
- why use probe that has different chemistry than reactant?

"active site": reactant is the best probe

Selection of conditions

- ✤ non-reactive conditions will not inform us about mechanism
 - in situ spectroscopy

Information: Band Intensity

- ✤ adsorption of *n*-butane on H-Mordenite at 297 K
- simultaneous independent measurement of adsorbed amount

combine information to determine extinction coefficient

- ★ IMEC ≈ 43.5 cm⁻¹ (cm² µmol) for adsorbed *n*-butane IMEC ≈ 13.1 cm⁻¹ (cm² µmol) for gas phase *n*-butane
- Extinction coefficients can be determined for individual stretching or deformation bands

Information on polarization of adsorbed molecule (reaction begin!)

- rarely considered (sometimes width is discussed)
- Lorentzian / Gaussian shapes

zeolite data: V.B. Kazansky, N.A. Sokolova, M. Bülow, Microp. Mesop. Mater. 67 (2004) 283

Ag/SiO₂ Catalysts: Motivation

- no vibrations of adsorbed H_2 detectable in spectra
- ✤ shift of OH vibration through H_2 adsorption by ca. -35 cm⁻¹
- no difference between SiO₂ and Ag/SiO₂ (8.09 at% Ag)

Exchange of Si-OH with D₂

✤ activation as for catalysis : 598 K, H₂

- OH groups react in D_2 atmosphere to OD groups
- * increase OD bands = decrease OH bands (equal ε?)

- exchange rate increases with temperature
- reaction faster for Ag/SiO₂ than SiO₂
- ✤ rate initially constant, then decrease (consumption of OH groups)

Temperature Dependence of HD Exchange

 Apparent activation energy E_A for HD exchange reaction SiO₂: 90 kJ mol⁻¹ Ag/SiO₂: 68 kJ mol⁻¹

Activation of Hydrogen: DH Exchange

- E_A for DH exchange on Ag/SiO₂
 30 and 50 kJ mol⁻¹
- ★ $E_A(H \rightarrow D) < E_A(D \rightarrow H)$ H₂ more easily activated than D₂

Hydrogenation of Acrolein (TU Darmstadt, Prof. Claus) Ag/SiO₂ at 1013-2026 kPa: E_A ca. 40 kJ/mol

activation of H₂ on Ag rate-determining step

Promotion of Sulfated Zirconia

- sulfated zirconia
 Holm, Bailey 1962, US Patent 3,032,599
 Hino, Arata, JACS 1979 & Chem. Comm. 1980
- Fe or Mn: promoting effect Hollstein et al., 1990 US Patent 4,918,041; Hsu et al., Chem. Comm. 1992; Lange et al., Catal. Lett. 1996

n-Butane Isomerization over MnSZ: In Situ DRIFTS

- sulfate overtones, combination modes, fundamentals (2764-2049, 1400 cm⁻¹)
- butane gas phase CH-stretching and bending vibrations 2966, 2939, 2877, 1466 cm⁻¹

- ✤ bands at 1600 and 1630 cm⁻¹ increase
- Also range of C=C stretching vibrations, but corresponding CH vibrations not ob served
- water bending vibration

Correlation of Spectral and Catalytic Information

- Rate of isomerization proportional to the amount of water formed (induction period)
 X. Li, K. Nagaoka, L.J. Simon, J.A. Lercher, A. Hofmann, J. Sauer, submitted
- Role of Mn is not to improve initiation reaction, in presence of Mn actual isomerization reaction is promoted

- band positions for activated catalyst consistent with S₂O₇²⁻ according to DFT calculations
- Red shift of S=O vibration at 1400 cm⁻¹ with increasing H₂O content calculated Hofmann, J. Sauer, J. Phys. Chem. B 108 (2004) 14652

- IR is a versatile technique, complete spectral information should be exploited
- information on local structure on any surface under wide variety of conditions (materials and pressure gap)
- extinction coefficients of individual bands inform about polarization of molecule upon adsorption: initiation of chemical transformation
- ✤ reaction kinetics (of model reactions) can be studied, determine E_A
- reaction mechanism can be revealed through in situ studies
- comparison with calculated quantities easily possible

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9Ag/SiO₂: AgNO₃/NaOH aufgefällt; 8.09 at% Ag; d = 15 nm

SiO₂ (Alfa): analog behandeltes SiO₂

ICP-AES, TEM: Christian Mohr, Technische Chemie II, TU Darmstadt

Fläche OH-Banden (Si-OH + andere): \bigstar SiO2:22.5 cm⁻¹ g⁻¹ \bigstar Ag/SiO2:12.3 cm⁻¹ g⁻¹

Goal: identify type (B/L), number, strength of acidic sites

IR, NMR, calorimetry (various probes): not superacidic, rather like strongly acidic zeolite *Kustov 1995, Adeeva 1995, Fogash 1995*

no acidic sites that explain activity

Isomerisierungsmechanismen: Butan

Isomerisierungsmechanismen: Pentan

- Ausbildung von Banden im Verlauf der Reaktion bei 358-423 K Bande bei 310 nm, Allylkationen
- Deaktivierung eine Folge der bimolekularen Isomerisierung

Pentanisomerisierung: Reaktionsprofil und "Verkokung"

- ungesättigte Spezies sind keine Intermediate
- keine Folge der monomolekularen Isomerisierung
- Resultat des bimolekularen Mechanismus, Konkurrenzreaktion?

Reaction Profile during Pentane Isomerization

unsaturated species are not intermediates

not a result of monomolecular isomerization

result of bimolecular mechanism, competing reaction to formation of gas phase products

Activation & Catalytic Performance

He: average Mn valence after activation 2.48

O₂: average Mn valence after activation **2.69**

correlation between oxidation state and catalytic activity:

the higher the average Mn valence the higher the maximum isomerization rate

positive effect:
$$50\% O_2$$

Activation & Catalytic Performance

N₂: ca. 180 μ mol g⁻¹ h⁻¹ **O**₂: ca. 140 μ mol g⁻¹ h⁻¹

Zunahme von Bande bei 1597 cm⁻¹ bis max. Umsatz dann Wachstum Bande bei 1628 cm⁻¹ Verschiebung S=O-Bande

Verschiebung S=O Bande korreliert mit Fläche Banden bei 1600+1630 cm⁻¹ Wasserbildung?

Abnahme der Gesamtintensität starke Gasphasenbeiträge im CH-Bereich

Reaction (in situ XAS)

- no correlation of average Mn oxidation state with activity
- no evidence for oxidative dehydrogenation as non-catalytic initial reaction step

- same activity profile after regeneration in O₂
- more than one regeneration possible
- same activity after regeneration in O₂ for N₂-activated catalyst

- recovery of the original spectrum
 - \succ regeneration in O_2 possible
 - reproducible state of catalyst after O₂ treatment

"Regeneration" - N₂

Regenerierung von sulf. ZrO₂

500 mg SZ, 1 kPa *n*-C₄ Reaktion bei 338 K Reaktivierung bei 723 K

✤ "Konditionierung in O_2 "?

ein Modell für sulfatiertes und promotiertes sulfatiertes ZrO₂

Zentren für Alkanadsorption an sulf. ZrO₂

Isobutanadsorption, Anpassung mit Langmuirmodell Monolage \approx 80 µmol/g; Sulfatgehalt \approx 560 µmol/g

nur ca. 15% des Sulfat involviert in Adsorption / Reaktion

Activation of Sulfated Zirconia: In Situ DRIFTS

- ✤ adsorbed water (3700-3000, 1600 cm⁻¹) partly removed during activation at 773 K
- ✤ sulfate overtones, combination modes, fundamentals (2764-2049, 1400 cm⁻¹)
- ✤ band positions consistent with S₂O₇²⁻ according to DFT calculations A. Hofmann, J. Sauer, J. Phys. Chem. B 108 (2004) 14652