

NUMERICAL APPROXIMATION OF NON-LINEAR CHROMATOGRAPHIC MODELS CONSIDERING BI-LANGMUIR ISOTHERM

by

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In this research article, two standard models of liquid chromatography, namely the dispersive equilibrium model and the kinetic lumped model are approximated numerically. We studied the transport of multi components in a single column of chromatography considering non-linear adsorption thermodynamics. The models are analyzed for standard bi-Langmuir and generalized bi-Langmuir types adsorption equilibrium isotherms using Danckwert boundary conditions. Mathematically, the model equations form a non-linear system of PDE accounting for the phenomena of advection and diffusion, paired with an algebraic equation or a differential equation for adsorption isotherm. An extended semi-discrete high resolution finite volume scheme is employed to obtain the approximate solutions of the governing model equations. The method has second to third order accuracy. Several test case studies are conducted to examine the influence of various critical parameters on the process performance. The contemplated case studies incorporate the elution process of liquid chromatography with an increasing number of components. In particular, single component, two component, and three component mixtures are considered for the assessment of process performance. The formulated numerical algorithm provide an efficacious mechanism for investigating the retention behavior and the influence of mass transfer kinetics on the shapes of elution profiles.

Key words: chromatographic models, bi-Langumir adsorption isotherm, non-equilibrium transport, finite volume method, mass transfer

Introduction

Chromatography is an efficient and effective technique used in laboratories and industries to separate and analyze many kinds of complex chemical mixtures. This process of separation has been much revolutionized due to the progress in science and technology. Chromatography technique can be effectually employed to target sophisticated segregation tasks for producing high purity products at the economical production rates. Application areas of chromatography include fine chemical, petrochemical, biotechnical, pharmaceutical, forensic pathology, and Nucleic acids research, *etc.* It plays a pivotal part in the realms of forensic test-

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ing, finger printing, food and beverage industry, creating vaccinations, DNA testing, insulin purification, plasma fractionation and enzyme purification *etc.* [1-4].

Separation of mixture components through chromatographic methods is based on their selective distribution and various affinities between two non-miscible phases, a flowing liquid known as the mobile phase and a stationary solid phase which is fixed in the column. High performance liquid chromatography apparatus includes a high pressure pump, a column, an adsorbent (stationary phase), a solvent (mobile phase), a liquid mixture (sample), a computer, a detector, and storage tanks. In this process, the sample of mixture components is fed at the column inlet. The sample components, in contact with the stationary phase, are transported by the mobile phase throughout the column. They interact distinctly with the stationary phase and thus, migrate through the chromatographic system at different speeds and elute out from the column at different times [3, 4].

A number of dynamical models, taking into consideration diverse levels of complexities, were introduced within literary texts to simulate the over all performance of chromatographic procedures. The frequently considered mass balance chromatographic models are the general rate model, the non-equilibrium kinetic lump model (KLM) and the dispersive equilibrium model (DEM), [1-4]. The physiochemical transport process and the interactions that take place during chromatographic operation are mechanistically represented by a systems of PDE. This system is usually paired along some algebraic equations or differential equations for adsorption isotherm. The linearity and non-linearity of these models depend on the adsorption isotherms associated with them. This article deals with the non-linear DEM and KLM of chromatography considering bi-Langmuir sorption isotherms. The analytical solutions of these models are only possible for linear adsorption isotherms which generate decoupled system of equations. As a result, efficient and accurate numerical approximations are needed for predicting dynamical mechanism inside the column [3, 5-7]. Generally, three well known classes of numerical methods have been proposed and applied in the literature for the solution of chromatographic models. The non-oscillatory finite difference methods like TVB (total variation bounded), TVD (total variation diminishing), ENO (essentially non-oscillatory), and WENO (weighted essentially non-oscillatory), flux limiting finite volume method (FVM), and the discontinuous Galerkin finite element method (DG-FEM) are among the few numerical methods with the ability of resolving discontinuities in the solution profile [3, 5-12]. The FVM is an attractive and efficient method that has been widely used to approximate different chromatographic models [5, 6, 13, 14]. The main advantage of the FVM is that the spatial discretization is carried out directly in the physical space. The method is capable to compute weak solutions of the governing equations and narrow peaks of the elution profiles correctly. Moreover, it has the ability to accurately overcome numerical oscillations. The schemes accuracy can be upgraded by introducing high order interpolating polynomials in the solution elements [15-17].

This study extends and generalizes the previous studies of our research group for non-linear DEM and KLM to the case of bi-Langmuir isotherm [6, 8]. The high resolution finite volume method (HR-FVM) of Koren is extended and utilized for the solutions of governing model equations [12]. The scheme approximates the solution with an accuracy of second to third-order [6, 7]. The spurious oscillations in the solution profiles due to the presence of discontinuities and strong shock waves are resolved numerically by utilizing the flux-limiting functions [1, 12]. A second to third order accurate Runge-Kutta (RK) method is applied to solve the resulting system of ODE [18]. Various test problems of single and multi-components elution are examined with a broad range of thermodynamic and kinetic parameters to demonstrate influences of isotherms on the concentration profiles.

The non-linear kinetic lump model

In this section, a multi-components non-linear 1-D KLM, is considered to study the effects of band broadening on chromatographic separation process. The KLM is a simple model for the description of mass transfer kinetics inside the chromatographic column. It achieves the mass balances by introducing a kinetic equation that describes the rate of variation of the averaged solute concentration in the stationary phase by assuming a linear driving force. This driving force commenced from the deviation from equilibrium concentration. The model lumps the contributions of external and internal resistances of mass transport into coefficient of mass transfer. The model assumes that the bed is isothermal and homogeneously packed. It include two fundamental kinetic variables, the coefficient of mass transfer, k_m , and the coefficient of axial dispersion, $D_{z,j}$. With these presumptions, the 1-D balance equations of mass for the transport of N_c species in the mobile phase can be written:

$$\frac{\partial u_j}{\partial t} + v \frac{\partial u_j}{\partial z} = D_{z,j} \frac{\partial^2 u_j}{\partial z^2} - \frac{k_{m,j}(q_j^* - q_j)}{\epsilon}, \text{ for } j = 1, 2, \dots, N_c \quad (1)$$

where N_c is the number of species in the sample of mixture. For each component j , $u_j(z, t)$ symbolizes the solute concentration in the mobile phase, the symbol $q_j(z, t)$ is the solute concentration in the stationary phase, q_j^* – the stationary phase concentration in equilibrium, v – the interstitial velocity of mobile phase, $D_{z,j}$ – coefficient of axial dispersion, external porosity of column packing is represented by ϵ , $k_{m,j}$ – the rate coefficient of mass transfer, and while t and z are the time and axial co-ordinates, respectively.

The KLM, assumes slow mass transfer kinetics whereas the adsorption desorption kinetics is infinitely fast. Therefore, in addition the aforementioned equation, the associated balance equation for the concentrations of mixture component in the solid particles are also required to complete the model and can be written in the form of kinetic equation:

$$\frac{\partial q_j}{\partial t} = \frac{k_{m,j}(q_j^* - q_j)}{1 - \epsilon} \quad (2)$$

The equilibrium adsorption isotherm defines an equilibrium relation among the mixture components concentration in the mobile and stationary phases. For modelling and simulation of the chromatographic separation process, it is essential to represent experimentally determined adsorption equilibrium data by suitable mathematical equations. A number of different adsorption isotherm models have been developed in the literature which are classified as linear, Langmuir, BET, and Freundlich isotherms *etc.* [3, 4, 19]. Here, we consider the non-linear bi-Langmuir isotherm. This isotherm was derived theoretically by assuming that the surface of adsorbent is covered by two completely independent group of adsorption sites [20-22]. For a mixture of N_c components, the competitive bi-Langmuir isotherm is expressed:

$$q_j^*(u) = \frac{a_{j,I} u_j}{1 + \sum_{k=1}^{N_c} p_k b_{k,I} u_k} + \frac{a_{j,II} u_j}{1 + \sum_{k=1}^{N_c} p_k b_{k,II} u_k}, \quad k, j = 1, 2, 3, \dots, N_c \quad (3)$$

where j^{th} component Henry's coefficient is denoted by a_j , b_j quantizes the extent of non-linearity associated with the isotherm, and the symbol p_j could have negative or positive signs to indicate the anti-Langmuir behavior and the Langmuir behavior of adsorption isotherm in the components of a mixture. In applications, each mixture component behaves like a Langmuir isotherm if the term p_j has a positive sign, other wise it is an anti-Langmuir type [23, 24]. Moreover, the

subscripts I and II refer to the adsorption sites I and II, respectively. The following non-dimensional quantities are proposed to facilitate the study:

$$x = \frac{z}{L}, \quad \tau = \frac{vt}{L}, \quad \text{Pe}_{z,j} = \frac{Lv}{D_{z,j}}, \quad \kappa_j = \frac{k_{m,j}L}{v} \quad (4)$$

where L is the column length and $\text{Pe}_{z,j}$ – the dimensionless Peclet numbers. Substituting the aforementioned dimensionless quantities in the model eqs. (1) and (2), we get:

$$\frac{\partial u_j}{\partial \tau} = \frac{1}{\text{Pe}_{z,j}} \frac{\partial^2 u_j}{\partial x^2} - \frac{\partial u_j}{\partial x} - \frac{\kappa_j(q_j^* - q_j)}{\epsilon} \quad (5)$$

$$\frac{\partial q_j}{\partial \tau} = \frac{\kappa_j(q_j^* - q_j)}{(1-\epsilon)}, \quad 0 \leq x \leq 1 \quad (6)$$

In order to close the model equations eqs. (5) and (6), appropriate initial conditions as well as the boundary conditions at the left end and at the right end of the column, respectively, must be imposed. We consider an initially equilibrated column:

$$u_j(x, \tau = 0) = u_j^{\text{init}}, \quad q_j(x, \tau = 0) = q_j^{*,\text{init}}, \quad j = 1, 2, 3, \dots, N_c \quad (7)$$

In this study, we consider rectangular injections and the conventional Danckwerts boundary conditions at the left end of the column [25]. These boundary conditions are stated:

$$u_j(x = 0, \tau) - \frac{1}{\text{Pe}_{z,j}} \frac{\partial u_j(x = 0, \tau)}{\partial x} = \begin{cases} u_j^{\text{inj}}, & \text{if } 0 \leq \tau \leq \tau^{\text{inj}} \\ 0, & \text{if } \tau > \tau^{\text{inj}} \end{cases}, \quad j = 1, 2, 3, \dots, N_c \quad (8)$$

These inlet boundary conditions collaborate with Neumann condition at the right end of column:

$$\left. \frac{\partial u_j}{\partial x} \right|_{x=1} = 0 \quad (9)$$

where the j^{th} component injected concentration is denoted by the symbol u_j^{inj} , the dimensionless time of injection is denoted by τ^{inj} . Moreover, the injection becomes continuous when $\tau^{\text{inj}} \rightarrow \infty$ or when the simulation time is less than the injection time τ^{inj} .

The non-linear dispersive equilibrium model

The DEM, which is the most simple one among the chromatographic models, assumes that there is permanent equilibrium between the mobile and the stationary phases. Moreover, in DEM, the axial dispersion and all mass transfer resistances because of non-equilibrium isotherms are accumulated in an apparent dispersion coefficient. Under these assumptions, D_z in eq. (1) is replaced by a new variable $D^{\text{app},j} > D_z$. Thus, for instantaneous mass transfer rate *i.e.* $k \rightarrow \infty$, eqs. (1) and (2) can be combined together to obtain the DEM. In dimensionless form, the balance equations of mass, for DEM:

$$\frac{\partial u_j}{\partial \tau} + \mathcal{F} \frac{\partial q_j^*}{\partial \tau} + \frac{\partial u_j}{\partial x} = \frac{1}{\text{Pe}_{z,j}} \frac{\partial^2 u_j}{\partial x^2}, \quad \text{for } j = 1, 2, \dots, N_c \quad (10)$$

where $\mathcal{F} = (1 - \epsilon)/\epsilon$ symbolizes phase ratio. Equation (10) assumes the same initial and boundary conditions presented in eqs. (7)-(9).

Numerical method

A number of numerical techniques have been proposed and applied in the literary text for the estimation of the chromatographic models [3-6]. In this section, a semi-discrete HR-FVM [6, 17] is utilized for the solution the 1-D KLM. The method is easily implementable, compact and simple. It has an accuracy of second to third order in the space variable [8]. The resultant ODE system is approximated numerically by using a general ODE solver available in the text. The extensive analysis on the accuracy and efficacy of our proposed method has already been done analytically and numerically in the previous articles of our research group [6, 7]. In addition, the method is capable of resolving sharp peaks and discontinuous fronts in the solutions accurately. For the sake of simplicity, we consider a single solute 1-D KLM for the derivation of our proposed numerical method. The method could be easily extended to multi-component combinations in the sample mixture. In the considered single component case, *i.e.* for $u_1 := u$ and $N_c = 1$, eqs. (5) and (6) becomes:

$$\frac{\partial u}{\partial \tau} = \frac{1}{\text{Pe}_z} \frac{\partial^2 u}{\partial x^2} - \frac{\partial u}{\partial x} - \frac{\kappa_j(q^* - q)}{\epsilon} \quad (11)$$

$$\frac{\partial q}{\partial \tau} = \frac{\kappa(q^* - q)}{1 - \epsilon} \quad (12)$$

where the numerical solution of the PDE in eq. (11) utilizes the HR-FVM, whereas the ODE given in eq. (12) is approximated numerically by a standard ODE solver *i.e.* (ODE23).

Discretization of computational domain: For the implementation of proposed HR-FVM to eq. (11), the discretization of the computational domain is the initial step. Here, we considered a uniform discretization of the computational domain $[0, 1]$ to avoid intricacy. The mesh intervals width is constant and represented by Δx . Let \mathcal{N}_x be the large integer representing the number of grid point, the co-ordinate $x_{j-1/2}$ denotes the mid point for each $j \in 1, \dots, \mathcal{N}_x + 1$. The mesh point x_j in the interval $\Omega_j \equiv [x_{j-1/2}, x_{j+1/2}]$ are covered by the cell for $1 \leq j \leq \mathcal{N}_x$:

$$x_{1/2} = 0, \quad x_{j+1/2} = j\Delta x, \quad x_{\mathcal{N}_x+1/2} = 1 \quad (13)$$

and

$$x_j = \frac{x_{j-1/2} + x_{j+1/2}}{2}, \quad \Delta x_j = x_{j+1/2} - x_{j-1/2} = \frac{1}{\mathcal{N}_x + 1} \quad (14)$$

Cell averages: For each cell, the average values of the cell $v_j(\tau)$ are defined as:

$$v_j = v_j(\tau) = \frac{1}{\Delta x_j} \int_{\Omega_j} v(x, \tau) dx \quad (15)$$

where $v \in \{u, q, q^*\}$. Until now, we have discretized the computational domain and assigned the corresponding initial data set at $\tau = 0$ to each mesh interval.

Integral form of KLM: Assuming that the cell averages v_j^{n+1} are provided at the time level τ^n . Then, we can easily find cell averages v_j^{n+1} at the next level of time *i.e.* τ^{n+1} . Integrating eqs. (11) and (12) over Ω_j yields:

$$\frac{du_j}{d\tau} = -\frac{u_{j+1/2} - u_{j-1/2}}{\Delta x_j} + \frac{1}{\text{Pe}_z \Delta x_j} \left[\left(\frac{\partial u}{\partial x} \right)_{j+1/2} - \left(\frac{\partial u}{\partial x} \right)_{j-1/2} \right] - \frac{\kappa(q_j^* - q_j)}{\epsilon} \quad (16)$$

$$\frac{dq_j}{d\tau} = \frac{\kappa(q_j^* - q_j)}{1 - \epsilon} \quad (17)$$

The first order derivatives in eq. (16) can be estimated:

$$\left[\frac{\partial u}{\partial x} \right]_{j \pm 1/2} = \pm \left[\frac{u_{j \pm 1} - u_j}{\Delta x_j} \right] \quad (18)$$

Various numerical schemes can be used to calculate the convective fluxes $u_{j \pm 1/2}$ at the cell interface.

First order numerical method: In this method, the values of concentration are approximated at the cell interfaces in eq. (16) by utilizing back-ward difference equation. The approximation for concentration can be expressed:

$$u_j = u_{j+1/2}, \quad u_{j-1} = u_{j-1/2} \quad (19)$$

The aforementioned approximations generate a first order accurate method.

The HR-FVM of Koren: Here, the concentration values at the interface of a cell $u_{j+1/2}$ are approximated by the following flux-limiting equations [17]:

$$u_{j+1/2} = u_j + \frac{1}{2}(u_j - u_{j-1})\zeta(\xi_{j+1/2}) \quad (20)$$

where

$$\xi_{j+1/2} = \frac{\gamma + u_{j+1} - u_j}{\gamma + u_j - u_{j-1}} \quad (21)$$

represent the ratio between successive concentration gradients. Further, to avoid division by zero we consider $\gamma = 10^{-10}$. The limiting function ζ in eq. (20) can be defined as [17, 26]:

$$\zeta[\xi_{j+1/2}] = \max \left[0, \min \left[2\xi_{j+1/2}, \min \left[\frac{1}{3} + \frac{2}{3}\xi_{j+1/2}, 2 \right] \right] \right] \quad (22)$$

Analogously, the concentration $u_{j-1/2}$ could be computed by changing the index j with the index $j - 1$.

Other schemes for flux limiting: Different flux limiting methods are accessible from literary material that assume different flux-limiting function [16, 27, 28]. In these schemes, fluxes at the right cell boundary, Ω_j , are expressed:

$$u_{j+1/2} = u_j + \frac{1}{2}\mathcal{G}(\beta_{j+1/2})(u_{j+1} - u_j) \quad (23)$$

Likewise, we can evaluate the left cell boundary fluxes. Here, $\beta_{j+1/2}$ can be defined:

$$\beta_{j+1/2} = \frac{\gamma + u_j - u_{j-1}}{\gamma + u_{j+1} - u_j} \quad (24)$$

Some well-known flux limiting functions, used in our test problems, are presented in tab. 1. The concentration profiles for specific case studies will be analyzed using these flux limiters .

The Stratagem at boundaries of cells: The flux-limiting approximations given by eqs. (20)-(23) cannot be applied to the boundary element of the cells. Therefore, the first-order backward method is employed to compute cell-interface concentration in the boundary cells. The fluxes at the interfaces of interior cells can be computed by aforementioned second-order accurate HR-FVM.

Table 1. The Flux limiting function used in [23]

Flux-limiter	Formula
[16]	$\mathcal{G}(n) = \max \left\{ 0, \min \left[2n, \frac{1}{2}(1+n), 2 \right] \right\}$
[27]	$\mathcal{G}(n) = \max [0, \min(2n, 1), \min(n, 2)]$
[27]	$\mathcal{G}(n) = \max [0, \min(1, n)]$
[28]	$\mathcal{G}(n) = \frac{ n + n}{1 + n }$

The ODE-solver: A standard ODE solver is utilized for the solution of the ODE system in eqs. (16) and (17). Further, the mathematical software MATLAB is utilized to program the numerical scheme and the built-in MATLAB routine ODE (23) is utilized to obtain the solution for the resultant ODE system.

Discussion on numerical test problems

Here, the presented HR-FVM is applied to simulate different chromatographic elutions. In the numerical test cases, chromatographic elutions are considered for

- single component 1-D DEM and 1-D KLM,
- two components 1D KLM, and
- three components 1D LKM, respectively.

For the sake of simplicity, the axial dispersion coefficients $D_{z,j} = D_z$ and the mass transfer coefficients $k_{m,j} = k_m$, for $j = 1, 2, \dots, N_c$, are supposed to be identical in all components. However, for practical applications the current model equations allow different values for these kinetic parameters for each component.

The single component elution

At the current subsection, few test cases are discussed for non-linear single component elution. We analyze the single component 1-D DEM given by eq. (10) and 1-D KLM given by eqs. (11) and (12) for standard bi-Langmuir non-linear isotherm:

$$q^*(u) = \frac{a_{1,I}u}{1 + b_{1,I}u} + \frac{a_{1,II}u}{1 + b_{1,II}u}$$

with $p_j = 1$ in eq. (3). Both continuous (left plots) and pulse (right plots) injections are taken into account. The Dankwerts boundary conditions given in eqs. (8) and (9) are employed. Table 2 reflect the standard parameters utilized in this case study.

Table 2. Standard parameters utilized in single-component elution

Parameters	L [cm]	ϵ [-]	ν [cmmin ⁻¹]	D_z [cm ² min ⁻¹]	t_{inj} [min]	t_{max} [min]
Values	1	0.4	0.1	0.0001	2	60
Parameters	u^{init} [g l ⁻¹]	u^{inj} [g l ⁻¹]	$a_{1,I}$ [-]	$a_{1,II}$ [-]	$b_{1,I}$ [-]	$b_{1,II}$ [-]
Values	0	10	0.5	1.0	0.05	0.1

Effects of injected concentration: Figures 1 displays the effects of finite-width injected concentrations. Here, four distinct injected volumes, such as $u^{inj} = 1$ g/l, $u^{inj} = 4$ g/l, $u^{inj} = 7$ g/l, and $u^{inj} = 10$ g/l are taken into consideration in an initially empty column *i.e.* $u^{init} = 0$ g/l. The sample pulse is infused into the column for $t^{inj} = 12$ minutes. The plots reveals that the peak heights start improving by increasing the volume of feeded concentration. It depicted the well known fact that the band width is proportional to the volume of injected sample. The concentration profiles for DEM have sharp and narrow peaks representing equilibrium, where as the profiles have broader fronts for the KLM for the considered small value of dimension less rate coefficient of mass $k = 1$ per minute. It could be observed from these plots that the column with-holding time is decreased with the rising value of injected concentration. The self sharpening effects of adsorption fronts becomes discernible for both models.

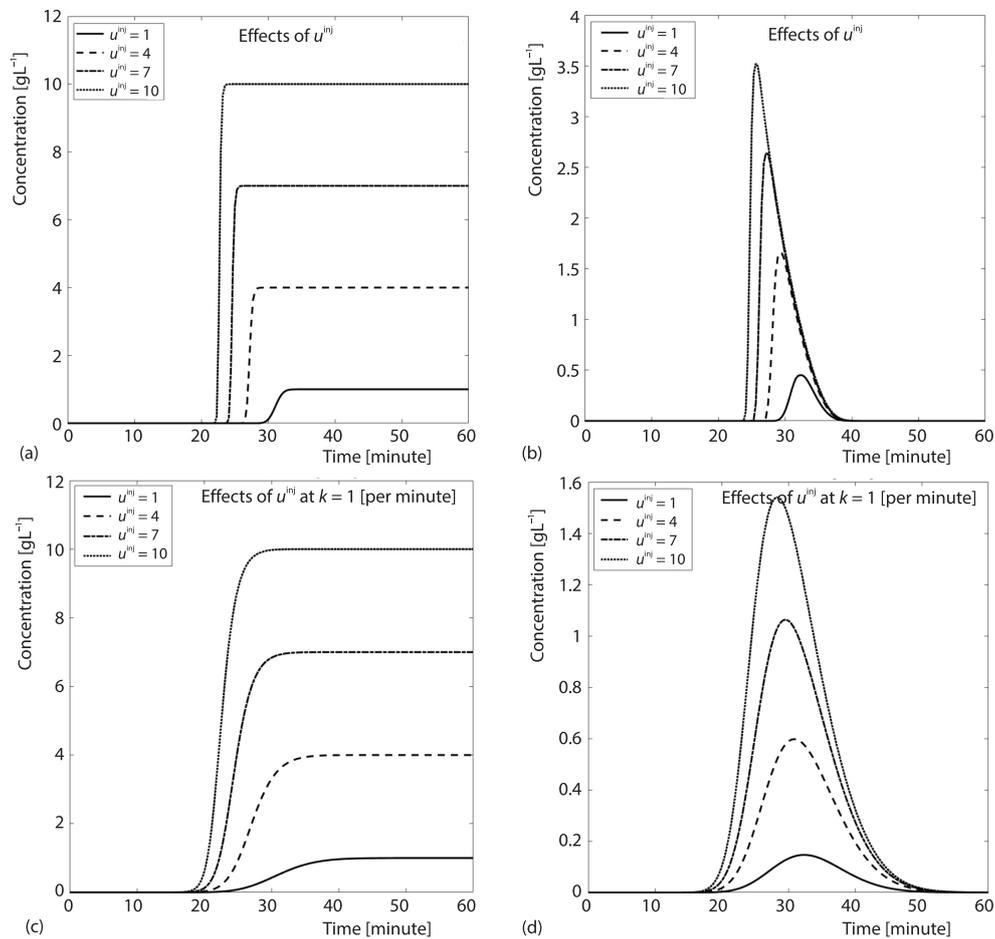


Figure 1. Effects of injected concentration u^{inj} for non-linear single component elution; (a) and (b) for DEM, and (c) and (d) for KLM with Danckwert boundary conditions

Effects of velocity: Figures 2(a) and 2(b) compares the concentration profiles for DEM and figs. 2(c) and 2(d) for KLM, to study the impact of flow-rate on retention time. Again the profiles are plotted for both continuous and pulse injections. Four different flow rates $v = 0.1$ cm

per minute, $v = 0.15$ cm per minute, $v = 0.2$ cm per minute, and $v = 0.25$ cm per minute are considered for the same value of $t^{inj} = 2$ minutes. Notably, the peak height with KLM is smaller than the DEM, because of delay in adsorption process incorporated in the model. It has also been observed that the column with holding time significantly reduces with the increase in the interstitial velocity. Moreover, the profiles become sharp with the dominant effects of considered adsorption for higher value of velocity and vice versa.

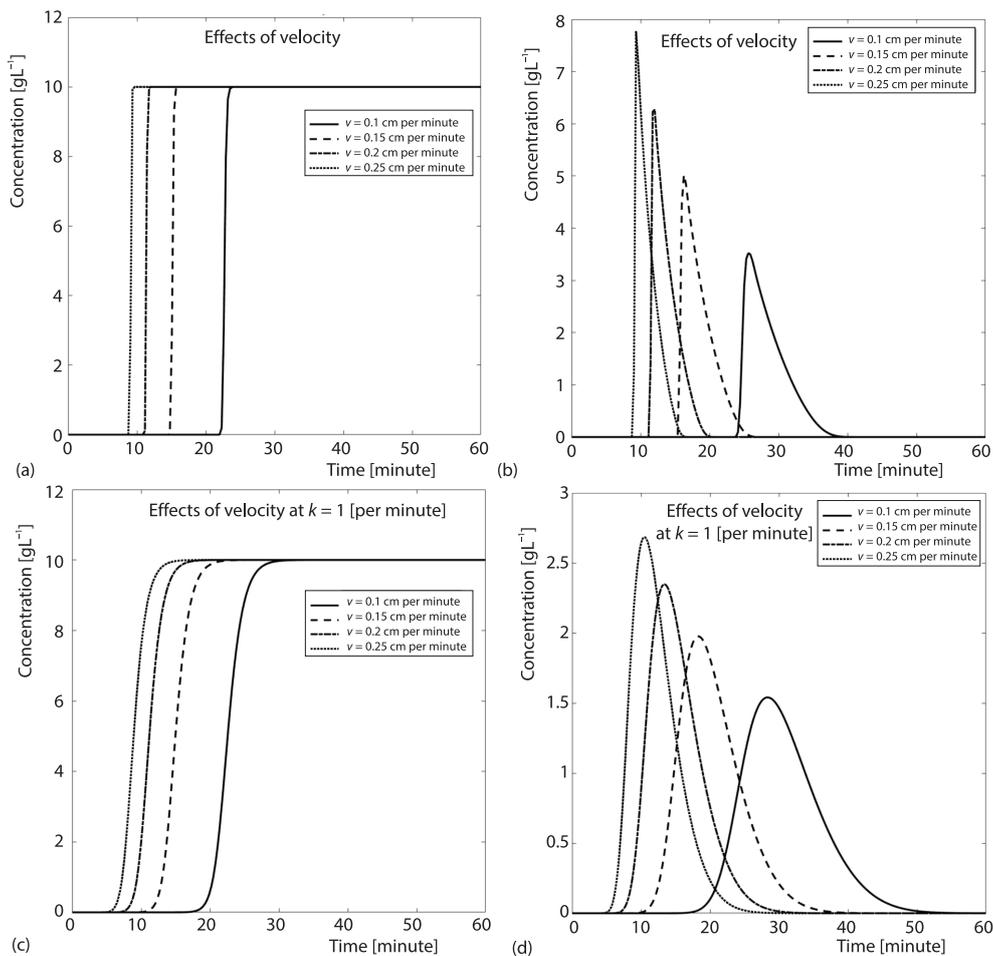


Figure 2. Effects of varying velocity for non-linear single component elution; (a) and (b) for EDM, and (c) and (d) for LKM with Danckwert boundary conditions

Effects of mass transfer coefficient: Figure 3 exhibits the influence of mass transfer coefficient k on 1-D KLM. The characteristic effects of non-linear isotherm (bi-Langmuir) are clearly evident from this figure. The profile is diffusive and broad for small value of and produces sharp corner for larger value of $k = 1$ per minute, $k = 100$ per minute. For $k = 100$ per minute the solution of KLM reduces to that of DEM as depicted in fig. 4. On the other hand, for small value of k per minute, the solution of KLM largely differs from the condition of equilibrium and hence, from the solution of DEM.

Relative error for KLM: Here, the single component KLM, *c.f.* eqs. (1) and (2), together with the bi-Langmuir non-linear isotherm:

$$q^*(u) = \frac{a_{1,I}u}{1+b_{1,I}u} + \frac{a_{1,II}u}{1+b_{1,II}u}$$

with $p_j = 1$ in eq. (3) is considered to compute relative errors. The standard parameters used in this problem are displayed in tab. 2. However, the experimental order of convergence and the accuracy of the method has already been computed in the previous articles by our research group [7, 8]. In the absence of analytical solution for the considered non-linear PDE, the solution of the flux-limiting Koren method at 3000 grid points is taken as the reference solution. The numerical solutions for 100 computational grid points at the column outlet are compared with the reference solution for $k = 1$ per minute and $k = 100$ per minute as shown in fig. 4.

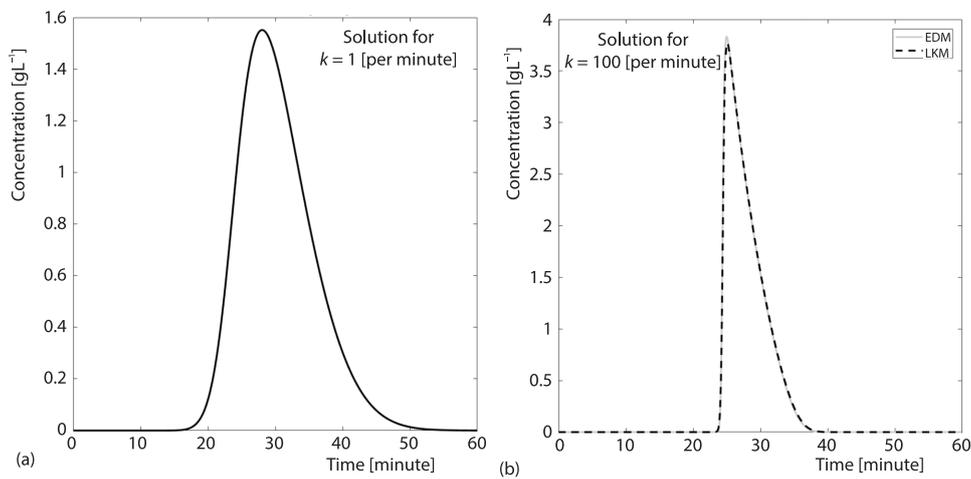


Figure 3. Effect of mass transfer coefficient k [per minute] on non-linear single component elution; (a) $k = 1$ and (b) $k = 100$

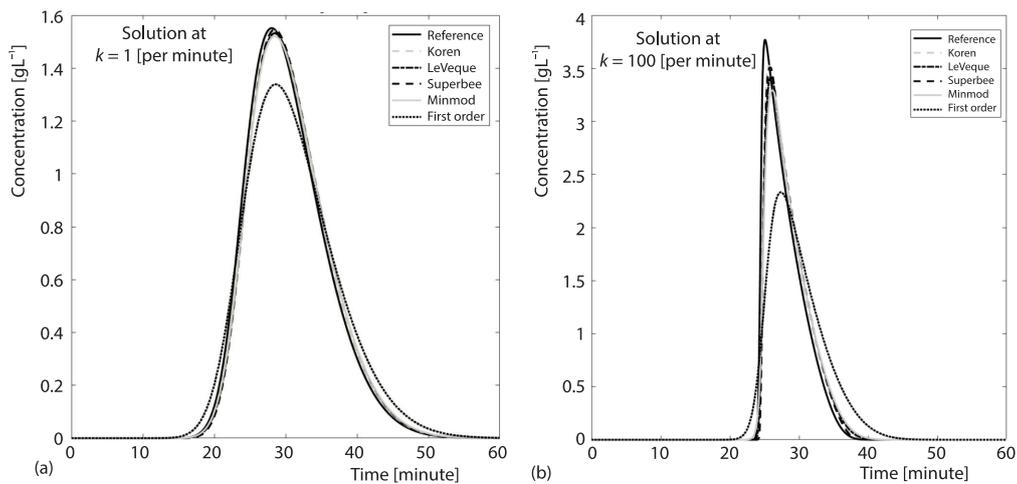


Figure 4. Comparison of scheme for non-linear single component elution; (a) $k = 1$ [per minute] and (b) $k = 100$ [per minute]

The relative error in time at the outlet of column, $x = 1$, can be calculated:

$$\text{Relative error} = \frac{\sum_{n=1}^{N_T} |U_R^n - U_N^n|}{\sum_{n=1}^{N_T} |U_R^n|} \quad (25)$$

where

$$U_R^n := U_R^n(x = 1, \tau)$$

represents the reference solution at time τ^n and $U_R^n(x = 1, \tau)$ is the corresponding numerical solution. The N_T is the total number of time steps and $\Delta\tau$ is the size of time step. Table 3 exhibits the relative error and experimental order of convergence (EOC) calculated by using Koren method for various grid points by assuming D_z as a variable. The results in tab. 3 depicts that the suggested flux limiting Koren scheme is second order accurate. The relative-errors and CPU run-times of different numerical schemes is computed in tab. 4, for two distinct values of $k = 1$ per minute and $k = 100$ per minute at 100 grid point. Notably, the Koren method generates smaller error in comparison the other schemes in terms of precision and efficacy. The solutions are smooth and have diffusive profile for $k = 1$ per minute. Thus, all the considered flux-limiting methods produces equivalent errors. Further, the first order method produced a diffusive profile, while the predicted concentration profiles of other schemes are in good agreement.

Table 3. Relative-error and EOC of the Koren scheme for single component elution

Grid points	$D_z = 0.001$		$D_z = 0.0001$		$D_z = 0.00001$	
	Relative-error	EOC	Relative-error	EOC	Relative-error	EOC
100	0.0437		0.0493		0.0507	
200	0.0226	0.9513	0.0237	1.0567	0.0240	1.0790
400	0.0111	1.0258	0.0112	1.0814	0.0110	1.1255
800	0.0048	1.2095	0.0050	1.1635	0.0046	1.2578
1600	0.0016	1.5850	0.0017	1.5564	0.0015	1.6167
3200	$1.1337 \cdot 10^{-4}$	3.8190	$1.2427 \cdot 10^{-4}$	4.0875	$1.0373 \cdot 10^{-4}$	3.9069

Table 4. Relative-errors and CPU run times for single component elution considering bi-Langmir isotherm at 100 grid points

Flux limiters	Relative-error		CPU
	$k = 1$ [per minute]	$k = 100$ [per minute]	
Superbee	0.0732	0.1805	11
Koren	0.0493	0.1296	10
van Leer	0.0705	0.1808	10
MC	0.0711	0.1833	10
Minmod	0.0686	0.1955	9
First order	0.1458	0.4526	6

The two-component elution

In this subsection, we have extended our analysis for the two component non-linear elution. In these case studies, the numerical results are generated by solving two component non-equilibrium 1-D KLM with the HR-FVS of Koren [1, 12]. Once again the analysis is done by using the Danckwert boundary conditions for infinite and finite feed volumes.

Case I [Generalized bi-Langmuir isotherm]: In this specific study, 1-D KLM given in eqs. (1) and (2) along with generalized bi-Langmuir isotherms with $p_1 = -1$ and $p_2 = 1$ in eq. (3) are used to simulate the propagation of a mixture carrying two components through a chromatographic column [18, 19]. All the standard parameters needed in the simulation are listed in tab. 5.

**Table 5. Case I: Generalized bi-Langmuir isotherm
(Parameters of non-linear two-component LKM)**

Parameters	L [cm]	ϵ [-]	ν [cmmin ⁻¹]	Dz [cm ² min ⁻¹]	$a_{1,I}$ [-]	$a_{1,II}$ [-]
Values	1	0.4	0.1	0.000001	0.5	0.75
Parameters	$a_{2,I}$ [-]	$a_{2,II}$ [-]	$b_{1,I}$ [-]	$b_{1,II}$ [-]	$b_{2,I}$ [-]	$b_{2,II}$ [-]
Values	0.25	2.0	0.05	0.015	0.0001	0.1

The column is set at a constant initial state in accordance with a certain initial composition. A specific feed composition is continuously injected in the column at time $\tau = 0$ for producing an inlet state. For small axial dispersion coefficient, this set-up coincides to a specific Riemann-problem.

In non-linear chromatographic theory, solutions of Riemann-problem are classified into three different elution fronts. These elution fronts are characterized as a semi-shock wave, a shock wave (discontinuous) and simple rarefaction wave (continuous). Shock is defined as a mathematical discontinuity in the equilibrium theory of non-linear chromatography. Shock waves arise when upstream state of composition fronts propagate faster than the downstream state. As a consequence of this compression, shock waves has sharp front and the components concentration improves across the shock. Contrary to the shock waves, rarefaction waves are the waves of expansion through which concentration decreases. They typically occur when the mobile phase eluted a strongly retained component, as the composition fronts travel along the column.

The numerical solutions comprises of three constant states, for instance the inlet state, \mathcal{A} , is defined on the left, the initial state, \mathcal{B} , is defined on the right, parted by two waves of transition which might be either the shock waves or the simple waves and the intermediate state, Int, is at the intercept of the characteristics of different index arising from states, \mathcal{A} and \mathcal{B} , respectively. In addition, we used the following abbreviations in the plot: $S_R :=$ shock wave on the right, and $Ref_c :=$ rarefaction wave on the left.

Result for the simulation of Case I: The following set of parameter values is used to perform the considered simulation by our suggested numerical method. The inlet concentrations for the Component I is taken as $u_1^{inj} = 0.0451$ g/l and for the Component II is $u_2^{inj} = 0.0476$ g/l. The initial concentrations for Component I is taken as $u_1^{inj} = 0.1818$ g/l and for the Component II is $u_2^{inj} = 0.1142$ g/l. The injection time for the problem is $t^{inj} = 2.0$ minutes and the total time of simulation is $t^{max} = 80$ minutes. The numerical predictions in time for two different values of k at the column out let *i.e.* $x = 1$ are displayed in fig. 5. The plots in fig. 5 leads to the classical solution. The

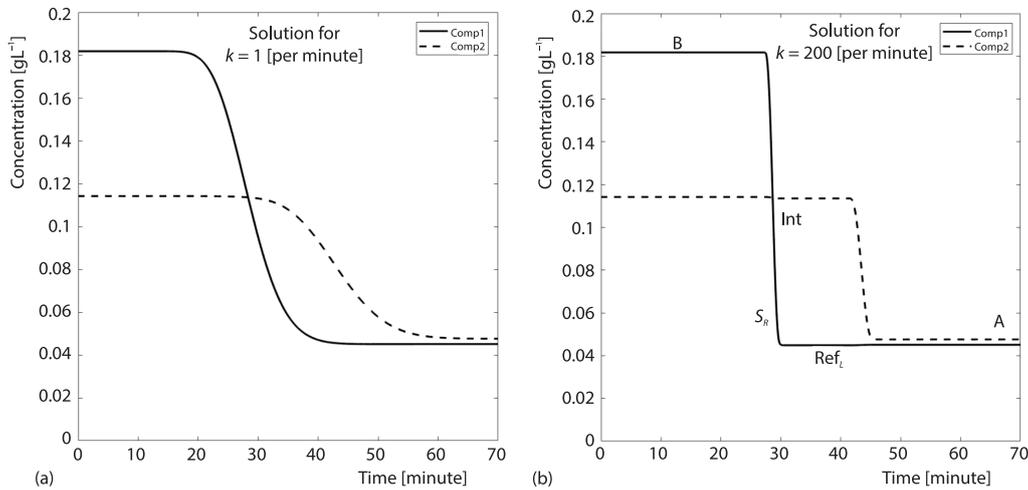


Figure 5. Plots of Case I (Riemann problem) at the column outlet;
 (a) $k = 1$ per minute and (b) $k = 200$ per minute

solution has two constant states namely the initial state, \mathcal{B} , on right and the inlet state, \mathcal{A} , on left, respectively, a shock wave on the right S_R , an Intermediate state, Int, in the center, and a rarefaction wave on the right Ref_L . It was observed that for the considered smaller value of $k = 1$ per minute the solution fronts are more diffusive in comparison of the solution front for the large value of $k = 200$ per minute. Moreover, when $D_z \rightarrow 0$ the solutions fronts would become more steep and sharper.

Case II [Standard bi-Langmuir isotherm]: In this test case, 1-D KLM given in eqs. (1) and (2) is applied to the two component chromatographic model *i.e.* $N_c = 2$. The standard non-linear bi-langmuir isotherm with $p_1 = p_2 = 1$ in eq. (3) is taken into consideration for specific injected volumes. The optimal parameters needed for the solution of the problem are $L = 1$ cm, $\nu = 0.1$ cm per minute, $\epsilon = 0.4$, $a_{1,I} = 0.5$, $a_{1,II} = 0.75$, $a_{2,I} = 0.25$, $a_{2,II} = 2.0$, $b_{1,I} = 0.05$, $b_{1,II} = 0.015$, $b_{2,I} = 0.0001$, $b_{2,II} = 0.1$, $t^{\max} = 80$ minutes, and $D_{z,i} = 0.0001$ cm² per minute. A rectangular pulse

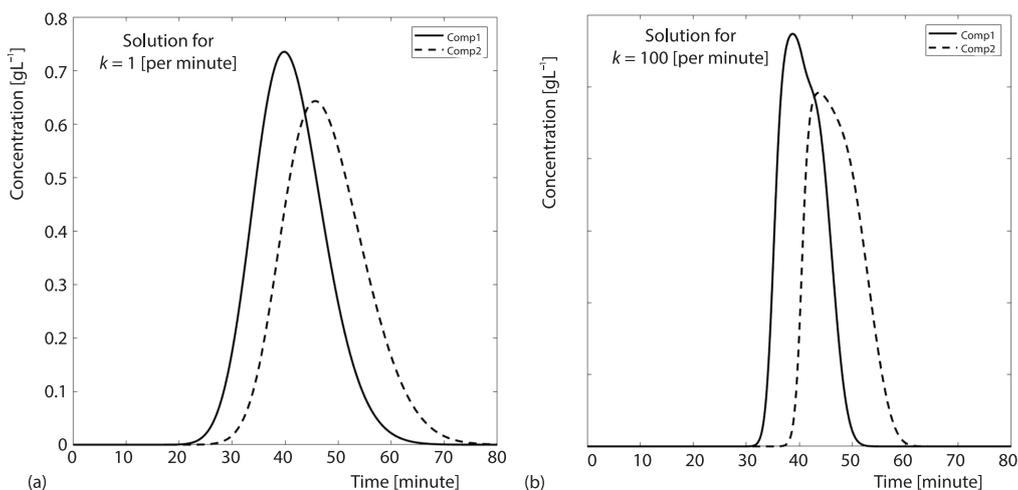


Figure 6. Two component non-linear elution profile at the column outlet;
 (a) $k = 1$ per minute and (b) $k = 100$ per minute

of the liquid mixture containing the two components $u_i^{\text{inj}} = 1 \text{ g/l}$ is infused in the flowing stream of solvent for $t^{\text{inj}} = 12 \text{ minutes}$. The Dankwerts boundary conditions given by eqs. (8) and (9) for $N_c = 2$ are utilized to generate the numerical result. In fig. 6, numerical predictions for two distinct values of rate coefficient of mass transfer, k , are shown. It is depicted from the fig. 6 that the concentration profiles become broaden along with elongated tails for $k = 1 \text{ per minute}$. Whereas, for $k = 100 \text{ per minute}$ the concentration profiles of both components show improvement in separation and have narrow rectangular shapes. Moreover, for $k = 100 \text{ per minute}$, the results of KLM are exactly equivalent to those obtained for DEM.

The effects of non-equimolar injection are demonstrated in fig. 7. Three different injection volumes:

- $u_1^{\text{inj}} = 6 \text{ g/l}$ and $u_2^{\text{inj}} = 3 \text{ g/l}$,
- $u_1^{\text{inj}} = 4 \text{ g/l}$ and $u_2^{\text{inj}} = 2 \text{ g/l}$, and
- $u_1^{\text{inj}} = 1 \text{ g/l}$ and $u_2^{\text{inj}} = 0.5 \text{ g/l}$,

are investigated. Once again the numerical results are generated for two different values of the rate coefficient of mass k . The elution profiles are diffusive for $k = 1 \text{ per minute}$, the diffusion process dominates the convection process and due to the considered small value of mass transfer coefficient the equilibrium is not achieved. Whereas for $k = 100 \text{ per minute}$, the profiles are sharp and peaked, the results depict equilibrium in the phase system. Moreover, for $k = 100 \text{ per minute}$, it can be observed that, an increase in the volume of injected feed produces an overshoot in the concentration profiles. Moreover, the prominent impact of self-sharpening fronts of adsorption can be observed.

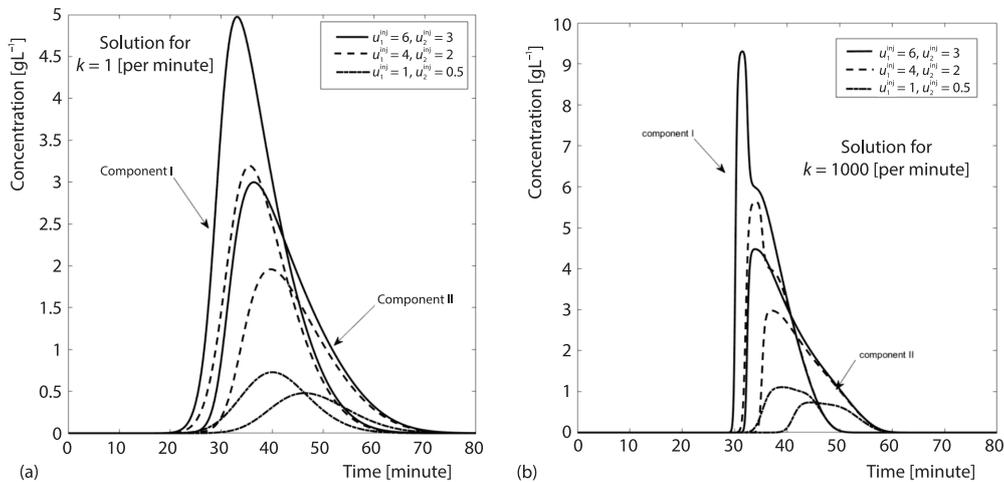


Figure 7. Effects of non-equimolar injection on two component non-linear elution profiles; (a) $k = 1 \text{ per minute}$ and (b) $k = 1000 \text{ per minute}$

The three component elution

Figure 8 presents the elution profiles for a three component segregation process. The parameters for the solution of this case study are $L = 1 \text{ cm}$, $\epsilon = 0.4$, $v = 0.1 \text{ cm per minute}$, $a_{1,\text{I}} = 1.0$, $a_{1,\text{II}} = 0.75$, $a_{2,\text{I}} = 0.5$, $a_{2,\text{II}} = 2.0$, $a_{3,\text{I}} = 0.25$, $a_{3,\text{II}} = 3.5$, $b_{1,\text{I}} = 0.05$, $b_{1,\text{II}} = 0.015$, $b_{2,\text{I}} = 0.0001$, $b_{2,\text{II}} = 0.1$, $b_{3,\text{I}} = 0.02$, $b_{3,\text{II}} = 1.0$, $t^{\text{max}} = 100 \text{ minutes}$, and $D_{z,i} = 0.0001 \text{ cm}^2 \text{ per minute}$. Numerical simulation are computed for standard bi-Langmuir isotherm given in eq. (3), for $j = 1, 2, 3$. The inlet concentration of height $u_j^{\text{inj}} = 1 \text{ g/l}$ for $j = 1, 2, 3$ is infused into column with

initial concentration $u_j^{\text{init}} = 0$ g/l for $t^{\text{inj}} = 2$ minutes. The numerical results generated for two distinct values of rate coefficient k of the mass transfer are displayed in fig. 8. The numerical predictions depicts asymmetrical, sharp fronts which is a typical behavior of bi-Langmuir adsorption isotherm. Further, components with greater value of equilibrium constant of adsorption elute later from the column and the components having smaller values of equilibrium constant of adsorption elute early. The generated elution profiles are dispersed and tailed for $k = 1$ per minute. Moreover, a better separation is accomplished as a result of the establishment of equilibrium for sufficiently large value of k (*i.e.* for $k = 100$ per minute).

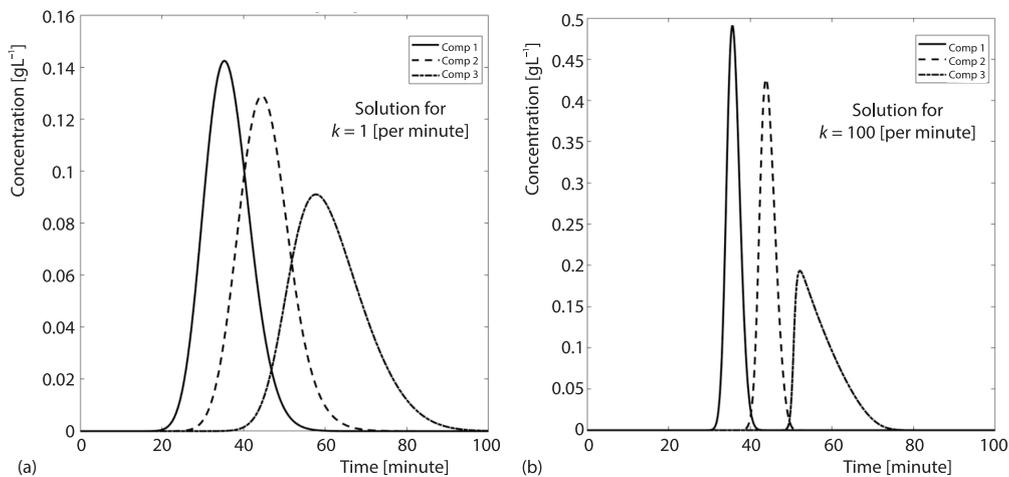


Figure 8. Three component non-linear elution profiles; (a) $k = 1$ per minute and (b) $k = 100$ per minute

Conclusions

In this article, two dynamic models known as dispersive equilibrium and the KLM of liquid chromatography are simulated numerically. The considered chromatographic models were examined for the bi-Langmuir adsorption isotherm by using Danckwert boundary conditions. The resulting systems consists of advection-diffusion PDE paired with an algebraic or the differential equation. A high resolution flux-limiting finite volume method was extended for the numerical solutions of the considered models. Numerous case studies of increasing difficulty, includes

- single component,
- two components, and
- three components elution were considered to scrutinize the models.

The effects of various kinetic parameter, in particular the rate coefficient of mass transfer and the effects of injected feed volumes, were studied on the performance of process. Further, the concentration profiles were investigated over non-linear chromatographic conditions for a broad variety of flux limiting functions. The presented finite volume gives second order accuracy. The scheme avoids over predictions and numerical oscillations in the solutions. The performance of the scheme in terms of stability, accuracy and computational time was validated against other flux limiting finite volume schemes. The suggested scheme was found more suitable on the basis of simulation results. Although this article deals with 1-D dispersive equilibrium and the KLM under isothermal conditions, the analysis can be expanded to the

models with enhanced resistance of mass transfer and reaction operating under non-isothermal conditions. Moreover, the analysis could also be extended to 2-D models in various situations. Such simulations are advantageous for better understanding of underlying transport mechanisms, up-grading physiochemical parameters and optimizing the experimental conditions.

Nomenclature

$a_{i,I}$ – adsorption constant of component i for site I, [–]	\mathcal{F} – phase ratio, [–]
$a_{i,II}$ – adsorption constant of component i for site II, [–]	k_m – mass transfer coefficient, [min ⁻¹]
$b_{i,I}$ – bi-Langmuir isotherm coefficient of component i for site I, [–]	L – column length, [cm]
$b_{i,II}$ – bi-Langmuir isotherm coefficient of component i for site II, [–]	t – time co-ordinate, [min]
$D_{z,j}$ – axial dispersion coefficient, [cm ² min ⁻¹]	t^{inj} – time of injection, [–]
ϵ – external porosity, [–]	t_{max} – total simulation time, [min]
	u_j^{init} – initial concentrations, [gl ⁻¹]
	u_j^{inj} – inlet concentration, [gl ⁻¹]
	v – interstitial phase velocity, [cmmin ⁻¹]
	z – axial co-ordinate, [–]

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